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## Highlights

### **The impact of porous medium heterogeneity on the thermal feedback of open-loop shallow geothermal systems**

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- Heterogeneity has a relevant impact on geothermal system efficiency.
- Heterogeneity of hydraulic conductivity affects the transient of thermal feedback.
- Heterogeneity and dispersivity do not affect long-term behaviour of well doublets.
- Uncertainty increases with medium heterogeneity in non-ergodic conditions.

# The impact of porous medium heterogeneity on the thermal feedback of open-loop shallow geothermal systems

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## Abstract

Groundwater has been increasingly used to provide low-carbon heating and cooling of buildings with open-loop shallow geothermal systems. Water is generally reinjected into the same aquifer after the heat exchange in order to avoid the aquifer depletion. However, this can result in the return of part of the injected water to the production well(s), causing a gradual thermal alteration known as thermal feedback. Thermal feedback is a major design issue of open-loop shallow systems but, so far, it has been mainly addressed neglecting the heterogeneity of the aquifer properties. This study investigates the impact of aquifer heterogeneity on two main metrics that characterize thermal feedback: thermal breakthrough time (i.e., the first arrival time of the thermal plume) and recirculating ratio (i.e., the fraction of water coming back to production well). A stochastic approach was adopted performing a large number of numerical simulations that cover a wide range of possible scenarios. Results highlight that conductivity heterogeneity plays a major influence on the temperature evolution at the production well. The breakthrough time alone might lead to misleading evaluations of the system efficiency, given that a few particles can reach the production well by traveling in the highly-conductive layers. Conversely, both the heterogeneity and the thermal dispersivity have a negligible impact on the recirculating ratio, which quantifies the long-term evolution of thermal feedback. As a consequence, the available approaches based on advection-only and homogeneous medium are a robust tool to predict the long-term behaviour of shallow open-loop geothermal systems.

*Keywords:* Geothermal systems, Thermal feedback, Thermal breakthrough time, Stochastic

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1 **1. Introduction**

2 The use of shallow geothermal energy for heating and cooling of buildings has become popular  
 3 thanks to the low operational costs and the low carbon intensity (Casasso and Sethi, 2019; Bayer  
 4 et al., 2019; Lund and Toth, 2020; Tissen et al., 2021; Bartolini et al., 2020). The heat in the  
 5 subsurface can be exploited by shallow geothermal systems in two ways: through the circulation  
 6 of a heat carrier fluid into a closed pipe loop (closed-loop systems) or by exchanging heat  
 7 with groundwater (open-loop systems). Generally speaking, closed-loop systems are installed in  
 8 the absence of an exploitable aquifer or, for small-power installations (e.g., below 100 kW),  
 9 to avoid the maintenance issues typical of wells. Open-loop systems are more popular for  
 10 large-scale installations up to a few MW thanks to their higher efficiency and the economies  
 11 of scale (Tsagarakis et al., 2020). Large flow rates in the order of tens or even hundreds of L/s  
 12 are abstracted to provide such a large thermal power and, for this reason, water is generally  
 13 reinjected into the same aquifer to avoid its depletion and depressurization (Horne, 1985; Banks,  
 14 2012).

15 However, reinjection raises a few possible issues, among which the return to the production  
 16 well(s) of a share of the reinjected water (Milnes and Perrochet, 2013). Since the temperature of  
 17 reinjected water is different from the background value of the aquifer (i.e., colder when the plant  
 18 operates in heating mode, and hotter when it operates in cooling mode), the abstracted water  
 19 progressively decreases or increases its temperature. Such a process occurs at the production  
 20 well only under certain hydraulic conditions, which are seldomly avoidable in densely-populated  
 21 urban areas (Clyde and Madabhushi, 1983; Kong et al., 2017). The gradual thermal alteration  
 22 of abstracted water is defined *thermal feedback* or *thermal recycling* according to the operat-  
 23 ing parameter imposed, that is, respectively, the reinjection temperature or the temperature  
 24 difference between reinjected and abstracted water (Milnes and Perrochet, 2013). This study  
 25 adopts constant reinjection temperatures and therefore focuses on the issues related to thermal  
 26 feedback, which might gradually compromise the efficiency of the geothermal plant even to its  
 27 failure (Banks, 2009). In order to prevent this, the temperature of reinjected water has a min-  
 28 imum and a maximum limit. The minimum temperature allowed is, theoretically, the water  
 29 icing ( $0^{\circ}\text{C}$ ); however, a safety margin must be imposed on this value. The maximum tempera-

30 ture allowed depends on technical constraints, such as the operating limits imposed by the heat  
31 pump manufacturer or the HVAC (Heating, Ventilation, and Air Conditioning) designer and  
32 on legislative constraints. Indeed, reinjection of warm water has several potentially negative  
33 impacts on groundwater ecosystems and on groundwater quality (Casasso and Sethi, 2019), as  
34 well as on neighbouring and downstream shallow geothermal installations (Epting et al., 2017;  
35 Barla et al., 2018; Pophillat et al., 2020).

36 Thermal feedback is therefore a major design issue for open-loop shallow geothermal systems.  
37 So far, the literature addressed this issue mainly considering a homogeneous porous medium.  
38 Early publications (Gringarten and Sauty, 1975; Lippmann and Tsang, 1980) and more recent  
39 works (Luo and Kitanidis, 2004; Milnes and Perrochet, 2013; Kong et al., 2017) provided the  
40 mathematical framework to address thermal feedback under the following assumptions: i) homo-  
41 geneous porous medium, ii) constant operating conditions (flow rate, temperature difference),  
42 and iii) a well doublet aligned with groundwater flow. Recently, Casasso and Sethi (2015) de-  
43 veloped a MATLAB code to assess thermal feedback with arbitrary well doublet alignments and  
44 derived an empirical formula to estimate the time trend of well temperatures for wells aligned  
45 with groundwater flow.

46 However, solutions based on homogeneous conductivity and effective macrodispersion coef-  
47 ficients are not able to grasp the effect of aquifer heterogeneity on thermal plume dynamics.  
48 Since the traditional procedures assuming homogeneous conductivity might lead to an incorrect  
49 design or an erroneous interpretation of the plant performance, we shall consider a stochas-  
50 tic approach (Dagan, 1989; Rubin, 2003; Fiori et al., 2015a; Kitanidis, 2015) to evaluate the  
51 effect of heterogeneity on shallow geothermal systems. By increasing the conductivity hetero-  
52 geneity, preferential flow paths emerge, thereby altering the temperature distribution at the  
53 production well (Pandey et al., 2018). Moreover, data scarcity does not allow a highly detailed  
54 description of the spatial variability of conductivity (Nowak et al., 2010; Maya et al., 2018).  
55 Consequently, such a lack of knowledge leads to high uncertainty in the predicted values. More  
56 precisely, heterogeneity in hydraulic conductivity could significantly affect the metrics used to  
57 evaluate the efficiency of geothermal systems. One of the most considered metrics is the *thermal*  
58 *breakthrough time* (Clyde and Madabhushi, 1983), which is defined as the first arrival time of a  
59 thermal plume travelling back to the production well and is ruled by the flow patterns in the well  
60 doublet. Another metric is the *recirculating ratio*, which quantifies the fraction of the injected

61 water returning to the production well and it is an indicator of the long-term sustainability of  
62 the system (Milnes and Perrochet, 2013).

63 So far, a small number of studies have investigated the impact of heterogeneity on the  
64 geothermal systems. Liu et al. (2019) examined the response of a well pair system in a heteroge-  
65 neous geothermal reservoir during continuous time operation. They studied how the variability  
66 of hydraulic conductivity, heat capacity and correlation length affect the well pair performances.  
67 They showed that breakthrough time decreases with increasing heterogeneity degree and cor-  
68 relation length values. Babaei and Nick (2019) addressed low-enthalpy well doublets with an  
69 initial temperature of 75°C and a reinjection at 30°C. In particular, they hypothesized a hetero-  
70 geneous and spatially correlated porosity field (assessing the effect of different values of variance  
71 and correlation length) and a permeability field that varies accordingly. They found that an  
72 increase of variance and/or correlation length of the porosity (and, hence, permeability) results  
73 in a decrease of the well doublet lifetime, defined as the time it takes for the abstracted water  
74 temperature to be reduced by 1°C. The same lifetime definition was previously used by Crooi-  
75 jmans et al. (2016) and by Willems et al. (2017) for a sedimentary fluvial reservoir considering  
76 different facies realizations. Watanabe et al. (2010), on the other hand, modelled a Hot Dry  
77 Rock reservoir with an equivalent porous medium approach, focusing on the propagation of the  
78 thermal plume downstream the reinjection well. They found that this phenomenon is mostly  
79 influenced by permeability and, to a lesser extent, by the thermal capacity, whereas the thermal  
80 conductivity has a negligible influence. The aforementioned studies focused on deep geothermal  
81 systems, which are generally characterized by low intrinsic permeabilities ( $10^{-18}$ - $10^{-12}$  m<sup>2</sup> accord-  
82 ing to Moeck (2014)) and large temperature differences between abstraction and reinjection, i.e.,  
83 in the order of tens of centigrade degrees. Shallow open-loop geothermal systems are installed in  
84 more permeable formations ( $10^{-11}$ - $10^{-9}$  m<sup>2</sup> according to Sethi and Di Molfetta (2019)) and adopt  
85 temperature differences within a few degrees (e.g.,  $\pm 4$ K according to Casasso et al. (2020)).  
86 To the authors' knowledge, so far no study has addressed the impact of the heterogeneity of  
87 subsurface properties on the operation of shallow open-loop geothermal systems.

88 The aim of this work is to test the impact of hydraulic conductivity heterogeneity on heat  
89 transport in open-loop shallow systems through a stochastic modelling framework. Our objec-  
90 tives are the following:

- 91 • Focusing on the interplay between heterogeneity and several thermo-hydro-geological pa-

92 parameters (e.g. thermal diffusion or pore-scale dispersivity) and engineering parameters  
93 (e.g., wells arrangement or operational pumping rates).

- 94 • Analyzing the behavior of the breakthrough time, i.e. the shortest time a water particle  
95 employs to move from the injection to the extraction well, and the recirculating ratio as a  
96 function of the main design parameters.
- 97 • Comparing the numerical results with the analytical solutions available in literature, in  
98 order to test the potentialities and limitations of more simplified approaches.
- 99 • Assessing the uncertainty due to the limited knowledge of the subsurface characterization  
100 and its effect on the system performance.

101 The paper is structured as follows. Section 2 presents the methodology by describing the  
102 thermal feedback problem, the theoretical framework of heat transport in heterogeneous porous  
103 media, and the numerical modelling setup. Section 3 presents the results divided into the analysis  
104 of the thermal breakthrough time, the recirculating ratio, the temperature at the pumping  
105 well and the ergodicity issue, discussing the main findings and the relationship with existing  
106 literature. Conclusions are reported in Section 4.

## 107 **2. Methodology**

### 108 *2.1. Problem statement*

109 In this work we consider an open-loop shallow geothermal system for the heating of buildings  
110 (though the same approach can also be applied to a cooling plant). The geothermal system  
111 consists of a well doublet placed into a confined aquifer of constant thickness  $B$ . A uniform-in-  
112 the-mean regional flow crosses the aquifer. Assuming a system of reference  $\mathbf{x} = \{x_1, x_2, x_3\}$ , the  
113 regional flow is aligned to  $x_1$ . Groundwater is abstracted upstream and, after the heat exchange,  
114 it is reinjected downstream with a constant lower temperature. The angle between the regional  
115 flow and the well doublet is defined as  $\theta$  and it is measured as shown in Figure 1. The wells in  
116 the doublet are placed at a distance  $L$ . The two wells are working at a constant rate  $Q_w$ , so  
117 that the model is steady-state for flow and transient for heat transport.

118 The pumping activity modifies the natural flow field and determines a local inversion of  
119 groundwater flow in the zone between the two wells. If the injected water reaches the extrac-  
120 tion well, we have the so called *thermal feedback*, which determines a progressive alteration of

121 the water temperature at the production well  $T_{prod}$  with a consequent decrease of the system  
 122 efficiency. The occurrence of the thermal feedback depends on hydrogeological characteristics,  
 123 such as the hydraulic conductivity  $K$ , the regional-flow gradient  $\mathbf{J} = \{J, 0, 0\}$  and the aquifer  
 124 depth  $B$ , as well as engineering parameters, such as the pumping rate  $Q_w$  and the wells spatial  
 125 arrangement (i.e. the well distance  $L$  and the angle  $\theta$ ).

126 This problem can be studied by interpreting heat as a tracer moving in a porous medium.  
 127 Such an assumption is valid under Local Thermal Equilibrium (LTE) between the rock and  
 128 the fluid (Shook, 2001; Hoehn and Cirpka, 2006; Markle and Schincariol, 2007; Hecht-Méndez  
 129 et al., 2010; Stauffer et al., 2019; Irvine et al., 2015; Sarris et al., 2018; Gossler et al., 2019).  
 130 As a consequence, the thermal plume moves through both pores and soil matrix and thus it  
 131 is slower than the fluid velocity. The thermal retardation factor  $R_{th}$  can be quantified as the  
 132 ratio between the thermal capacity of the porous medium and the thermal capacity of water, as  
 133 follows (Shook, 2001):

$$R_{th} = \frac{\rho_s c_s}{n \rho_w c_w} \quad (1)$$

134 where  $\rho_w$  and  $\rho_s$  are the water and the solid matrix densities, respectively,  $c_w$  and  $c_s$  the specific  
 135 heat capacities of water and solid matrix, respectively, and  $n$  is the porosity.

136 The thermal breakthrough time  $\tau_0$ , namely the shortest time a water particle spends travel-  
 137 ling from the injection well to the production well, is the metric commonly adopted to evaluate  
 138 the thermal feedback. So far, most of practical studies (Gringarten and Sauty, 1975; Lippmann  
 139 and Tsang, 1980; Clyde and Madabhushi, 1983; Milnes and Perrochet, 2013; Casasso and Sethi,  
 140 2015) have evaluated  $\tau_0$  by means of a closed analytical solution that assumes a homogeneous  
 141 domain, a mean regional flow aligned with the pumping wells (i.e.  $\theta = 0$ ) and advective-  
 142 only transport. Under such hypotheses the analytical breakthrough time  $\tau_0^{an}$  can be calculated  
 143 through the complex potential theory as follows (see, e.g., Strack, 2017; Luo and Kitanidis,  
 144 2004):

$$\tau_0^{an} = R_{th} \frac{nL}{KJ} \left[ \frac{\chi}{\sqrt{\chi-1}} \tan^{-1} \left( \frac{1}{\sqrt{\chi-1}} \right) - 1 \right] \quad (2)$$

145 where  $\chi$  is the dimensionless pumping rate

$$\chi = \frac{2Q_w}{\pi BKJL} \quad (3)$$



146 Providing that the aforementioned assumptions are satisfied, the thermal feedback occurs only  
 147 when  $\chi > 1$  (Luo and Kitanidis, 2004).

148 In order to evaluate the sustainability of an open-loop system, designers also need to quantify  
 149 the long-term effect. A typical metric is the fraction of injected water returning to the production  
 150 well  $RR$ , which provides the indication of the efficiency decay of the plant. As well as for  $\tau_0^{an}$ ,  
 151 a closed form analytical solution can be introduced to assess  $RR^{an}$  under the assumption of  
 152 advective transport and well doublet aligned with the mean flow (Milnes and Perrochet, 2013):

$$RR^{an} = \frac{2}{\pi} \left[ \tan^{-1} \left( \sqrt{\chi - 1} \right) - \frac{\sqrt{\chi - 1}}{\chi} \right] \quad (4)$$

153 We emphasize that these analytical formulae (e.g. eqs. (2) and (4)) are obtained assuming  
 154 only convective heat transport, neglecting conduction, medium heterogeneity and other pore-  
 155 scale dispersive/diffusive phenomena. Introducing these more realistic phenomena or angle  $\theta$   
 156 different from zero requires the use of numerical solution schemes. Moreover, these solutions  
 157 neglect the spreading of the flow trajectories operated by the natural heterogeneity of real  
 158 aquifers. Heterogeneity determines the emergence of fast flow paths and stagnation zones in the  
 159 medium, thereby exerting a significant impact on  $\tau_0$  (Wen and Gómez-Hernández, 1996; Zinn  
 160 and Harvey, 2003; Knudby and Carrera, 2006; Fiori and Jankovic, 2012). Given that in the  
 161 ergodic case  $\tau_0$  assumes values in the range  $(0, +\infty)$ , a significant deviation from the equivalent  
 162 homogeneous solution is expected in heterogeneous media. In the next sections, we present  
 163 the mathematical framework and the numerical setup to study open-loop shallow systems in  
 164 heterogeneous porous media.

## 165 2.2. Theoretical framework

166 Figure 1 depicts a sketch of the conceptual model considered here. We assumed that the  
 167 flow field occurs in a 3-D confined and stratified aquifer, which is made of  $N$  layers, each one  
 168 characterized by a random homogeneous hydraulic conductivity  $K_i$ , for  $i = 1, N$ . The log-  
 169 conductivity field  $Y = \ln K$  is modeled as a stationary random variable normally distributed  
 170 with mean  $\ln(K_G)$ , with  $K_G$  the geometric mean of  $K$ , and variance  $\sigma_Y^2$  (Freeze, 1975; Fiori  
 171 et al., 2015b). The thickness of each layer is  $2I_v$ , with  $I_v$  the vertical integral scale of  $Y$ , such  
 172 that the number of layers is  $N = B/(2I_v)$ . Water is injected over the total thickness of the  
 173 aquifer, in such a way that each layer conveys a flux proportional to the local  $K_i$  (see, e.g.,

174 Kreft and Zuber, 1978; Demmy et al., 1999; Frampton and Cvetkovic, 2009). This stratified-  
 175 formation conceptual scheme is quite common in groundwater studies dealing with contaminant  
 176 migration in groundwater (e.g. Zavala-Sanchez et al., 2009; Pedretti and Fiori, 2013; Zech et al.,  
 177 2018) and can be considered suitable for systems with  $L < I_h$ , with  $I_h$  the  $Y$  horizontal integral  
 178 scale.

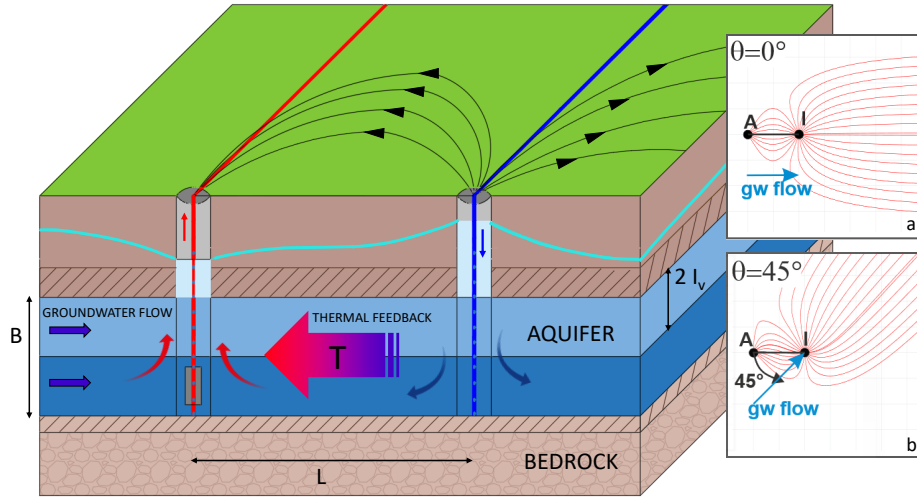


Figure 1: A sketch of the conceptual model. The porous formation is a 3-D confined and stratified aquifer. It is composed of a series of  $N$  layers of conductivity  $K_i$ , with  $i = 1, N$ . The conductivity is a stationary random variable lognormally distributed. A well doublet operating as a geothermal system is placed at the center of the domain. Insets a and b show two configurations of the angle  $\theta$  between the wells and the regional flow.

179 At the beginning of the simulation, groundwater is at a constant temperature  $T_{ref}$ . After  
 180 being extracted from the production well, water is reinjected in the injection well at a different  
 181 temperature  $T_{well}$ . As a consequence, a heat plume develops from the injection well, and part of  
 182 this flow can reach the production well located upstream. Heat transport in geothermal system  
 183 results from the interplay of different physical phenomena such as conduction, thermal advec-  
 184 tion and thermal dispersion (Carlslaw and Jaeger, 1959). Conduction is the direct microscopic  
 185 transfer of kinetic energy between atoms and molecules. It results in heat moving in the opposite  
 186 direction of temperature gradient. Thermal advection is the transport of heat due to the motion  
 187 of a fluid moving from one place to another. Thermal dispersion is the heat exchange occur-  
 188 ring in porous media due to the nonuniformity in temperature and velocity at the pore-scale

189 (Özgümüş et al., 2013).

190 Under LTE, heat transport in porous media can be modelled in a similar way to the transport  
191 of solutes. Thus at the Darcy-scale, heat transport can be described by the advection-dispersion  
192 equation for solute transport (De Marsily, 1986):

$$-\nabla \left( \frac{\mathbf{q}}{n} T \right) + \nabla (D \nabla T) + \frac{q_H}{n \rho_w c_w} = R_{th} \frac{\partial T}{\partial t} \quad (5)$$

193 where  $T$  is the local temperature,  $q_H$  the heat source,  $\mathbf{q}$  the water flux at the Darcy-scale, related  
194 to advection, and  $D$  is the thermal dispersion which accounts for the heat transfer at pore scale.  
195 The thermal dispersion  $D$  is given by the sum of two different components, the thermal diffusion  
196  $D_{th}$  and the pore-scale dispersion  $D_\alpha$ :

$$D = D_{th} + D_\alpha = \frac{\lambda}{n \rho_w c_w} + \alpha_d \frac{|\mathbf{q}|}{n} \quad (6)$$

197 where  $\lambda$  is the effective thermal conductivity of the medium,  $\alpha_d$  the pore-scale dispersivity, here  
198 assumed as isotropic, and  $|\mathbf{q}|$  is the magnitude of the local velocity. The water flux can be  
199 described by the well known Darcy equation:

$$\mathbf{q} = -K \nabla \phi = -K \mathbf{J} \quad (7)$$

200 where  $\phi$  is the hydraulic head.

201 Eq. (5) assumes constant water density and viscosity, thus neglecting the temperature  
202 dependence on these properties. The limited temperature ranges at which shallow geothermal  
203 systems operate (i.e., up to  $\pm 6^\circ\text{C}$  compared to background temperature) induce a slight variation  
204 of water properties that makes this assumption plausible, as reported in Hecht-Méndez et al.  
205 (2010). Under such hypotheses, eq. (5) is formally identical to the *advection dispersion equation*,  
206 which describes the solute migration of a sorbing solute in groundwater (Shook, 2001; Hidalgo  
207 et al., 2009). By taking advantage of such a mathematical and conceptual equivalence, transport  
208 is simulated with a particle tracking procedure developed along a Lagrangian framework. This  
209 approach has been extensively used and tested in studies dealing with the solute transport in  
210 heterogeneous aquifers with several levels of complexity (Cortis and Berkowitz, 2005; Salamon  
211 et al., 2006; Rizzo et al., 2019).

212 The procedure adopted here is the equivalent random walk formulation of eq. (5), which  
 213 aims to mimic the water and heat transport in the domain (Kinzelbach, 1988; Uffink, 1988). We  
 214 consider a water parcel which, once released in the injection well with temperature  $T_{well}$ , moves  
 215 in the flow domain following a flow path. The “total” trajectory  $\mathbf{X}(t)$  of the water parcel can be  
 216 written as the sum of two independent components: i) the advective one related to the Darcy-  
 217 scale advective velocity, and ii) the fluctuation component  $\mathbf{X}'(t)$  which represents phenomena  
 218 acting at the pore or microscopic scale. The fluctuation, which summarizes the effects of pore-  
 219 scale dispersion and conduction, is described here by a Wiener process characterized by the local  
 220 dispersion coefficient  $D = D_{th} + D_\alpha$  (see eq. (6)). In the following, we shall adopt for simplicity  
 221 an isotropic pore-scale tensor. The total trajectory  $\mathbf{X}(t)$  can be written as:

$$\mathbf{X}(t) = \mathbf{X}_0 + \int_0^t \mathbf{v}(\mathbf{x}, t - \tau) d\tau + \mathbf{X}' \quad (8)$$

222 with  $\mathbf{X}_0$  the initial position of the particle and

$$\mathbf{X}' \in N[0, 2Dt/R_{th}] \quad (9)$$

223 where  $\mathbf{v}(\mathbf{x}, t) = \mathbf{q}(\mathbf{x}, t)/(n R_{th})$  is the local Darcy-scale advective velocity in the position  $\mathbf{x}$  at  
 224 time  $t$ . The dispersion term plays a key role: it determines the deviation of the water particles  
 225 from the advective streamlines, thereby triggering mixing, macrodispersion and heat dispersion  
 226 phenomena (Rubin et al., 1999; Shook, 2001; Villiermaux, 2012; Le Borgne et al., 2013; Dentz and  
 227 de Barros, 2015; Di Dato et al., 2018). Given that the heat transport occurs along the flow paths,  
 228 their ensemble constitutes the heat plume, namely the portion of the domain with temperature  
 229 affected by the heat injection. Since the temperature is regarded as a tracer associated to the  
 230 water particles, its assessment in a given position of the flow field would require an ensemble  
 231 average over different realizations. However  $T_{prod}$  at the extraction well can be obtained by  
 232 taking the average over the flow paths entering in the well and invoking the ergodicity (Dagan,  
 233 1991).

234 In this work we adopt a numerical scheme for the Lagrangian particle tracking procedure.  
 235 Beside the two lumped parameters  $\tau_0$  and  $RR$ , we analyze the temperature evolution at the  
 236 production well. In fact, although the two metrics  $\tau_0$  and  $RR$  can be used for a fast assessment  
 237 of the geothermic plant efficiency, they do not give any information on the temperature evolution  
 238 at the production well, which in turn assesses the plant efficiency evolution in time.

239 *2.3. Numerical setup*

240 On the line of the theoretical framework discussed in the previous section, we developed  
 241 a numerical code to investigate how spatial heterogeneity, thermal dispersion and engineering  
 242 parameters affect the thermal feedback metrics, i.e.  $\tau_0$  and  $RR$ , and the temperature evolution at  
 243 the production well. The flow field is solved by means of the finite volume scheme of MODFLOW-  
 244 2005 (Harbaugh, 2005), which is managed through the FloPy python script (Bakker et al., 2016).  
 245 The thermal propagation is modelled by following the Lagrangian approach through the particle  
 246 tracking procedure outlined in Di Dato et al. (2019). The injected mass is modelled with a cloud  
 247 of particles and transport is simulated by tracking them according to the Itô–Taylor integration  
 248 scheme (Itô, 1951):

$$\mathbf{X}_p(t + \Delta t) = \mathbf{X}_p(t) + \mathbf{A}(\mathbf{X}_p, t)\Delta t + \mathbf{B}(\mathbf{X}_p, t) \epsilon \sqrt{\Delta t} \quad (10)$$

249 where  $\mathbf{X}_p$  is the particle position at the initial time  $t$ ,  $\Delta t$  is the numerical time step,  $\epsilon$  is a vector  
 250 of independent normally distributed random numbers with zero mean and unit variance and the  
 251 tensors  $\mathbf{A}$  and  $\mathbf{B}$  are defined, respectively, as (Kinzelbach, 1988; Uffink, 1988):

$$\mathbf{A} = \mathbf{v} + \nabla \cdot \left( \frac{D}{R_{th}} \right) \mathbf{I} \quad (11)$$

$$\mathbf{B} \cdot \mathbf{B}^T = \left( 2 \frac{D}{R_{th}} \right) \mathbf{I} \quad (12)$$

252 where  $\mathbf{I}$  is the identity tensor. The time step  $\Delta t$  is chosen by following the particle tracking  
 253 procedure outlined in Di Dato et al. (2019, see Appendix A). The authors proposed a modified  
 254 version of the algorithm of Pollock (1988) to model diffusion and pore-scale dispersion. Di Dato  
 255 et al. (2019) verified the accuracy of their algorithm by comparing the numerical results with a  
 256 3<sup>rd</sup> order Runge-Kutta scheme (Drummond et al., 1984) and the analytical solution of Moench  
 257 (1989) obtaining a very good match.

258 As the focus of this paper is on the production of shallow geothermal energy for heating  
 259 and cooling of buildings, the system domain is chosen to model the typical size of a small  
 260 installation, e.g. for a detached house, in which the available space for well distancing is not  
 261 large. The numerical domain depicts a perfectly stratified porous medium with a constant  
 262 depth  $B = 10$  m divided in 10 layers of thickness equal to  $2I_v = 1$  m. Such a value of  $I_v$

263 is consistent with the values encountered in natural porous formations (Rubin, 2003). Each  
 264 layer is homogeneous and characterized by a random log-conductivity  $Y = \ln K$  drawn from a  
 265 normal distribution with mean  $\ln(K_G)$  and variance  $\sigma_Y^2$ . In stratified media the geometric mean  
 266 is given by  $K_G = K_{eff}/\exp(\sigma_Y^2/2)$ , where the effective conductivity  $K_{eff}$  is equivalent to the  
 267 arithmetic mean of  $K$ . We stress that here the definition of  $K_{eff}$  refers to a system subject only  
 268 to regional flow and it is not a property of strongly nonuniform well flow (Bellin et al., 2020).  
 269 The dimensionless pumping rate  $\chi$  in heterogeneous media is therefore defined as:

$$\chi = \frac{2Q_w}{\pi BK_{eff}JL} \quad (13)$$

270 We explore three heterogeneous scenarios ranging from homogeneous ( $\sigma_Y^2 = 0$ ) to mild hetero-  
 271 geneity degree, i.e.  $\sigma_Y^2 = 1$  and 2.

272 Two fixed heads are assigned to the left and the right boundaries, such that a regional  
 273 flux develops from left to right. In order to model a confined aquifer, the hydraulic heads  
 274 are set higher than the aquifer top. Two wells are located at the center of the computational  
 275 domain at a distance of  $L = 10$  m and the line joining the wells forms an angle of  $\theta$  with  
 276 the regional flux. As stated in Casasso and Sethi (2015), the convention adopted is that  $\theta$   
 277 is measured counterclockwise from the line joining the wells. The upstream well is extracting  
 278 and the downstream one is injecting water at equal constant rate  $Q_w$ , in such a way to create  
 279 an open loop. Three setups are considered here:  $\theta = 0, \pi/4$  and  $\pi/2$ . The pumping rate is  
 280 chosen in such a way to investigate  $\chi$  ranging from 2 to 12. The 3-D computational grid is  
 281  $7L \times 7L = 70 \text{ m} \times 70 \text{ m}$  in the horizontal direction, which suffices to avoid the well influence at  
 282 the boundaries. The dimensions of the computational cell are  $L/50 = 0.2$  m on the horizontal  
 283 direction and  $I_v/4 = 0.125$  m on the vertical direction.

284 The thermal dispersion is given by the sum of the thermal diffusion  $D_{th}$  and pore-scale  
 285 dispersion  $D_\alpha$ , as defined by eq. (6). We consider here four scenarios, given by the combination  
 286 of  $\alpha_d = 0$  and 0.001 m (Fiori and Dagan, 1999) and  $D_{th} = 0$  and  $10^{-6} \text{ m}^2/\text{s}$  (Holman, 2008,  
 287 Appendix A, Table A-3), which grasp the range of values typically observed in natural aquifers.  
 288 We highlight that this study focuses on the heterogeneity of the hydraulic conductivity, thereby  
 289 neglecting the variability of other parameters, such as thermal conductivity and capacity. This  
 290 choice is justified by the fact that the hydraulic conductivity varies in much wider ranges and  
 291 has a much stronger influence than both thermal conductivity and capacity. Piga et al. (2017)

292 highlighted that only the long-term (but not the short-term) propagation of thermal plumes is  
 293 somehow affected by the thermal conductivity, whereas heat capacity has a negligible effect both  
 294 in the short and the long term. When it comes to thermal feedback, much shorter time and space  
 295 scales (i.e. the nearbies of the well doublet) are involved, compared to the propagation of thermal  
 296 plumes (which develop over larger spatial scales compared to the well doublet distance). For  
 297 this reason, even thermal conductivity has a secondary effect. Similar conclusions were achieved  
 298 by Lo Russo et al. (2012).

299 We modelled the thermal plume by releasing  $N_p = 5880$  particles from the injecting well.  
 300 The injected mass is distributed around the injecting well at every  $\pi/60$  radiant and placed  
 301 uniformly along the depth with an offset of  $2I_v$ , which is needed in order to avoid boundary  
 302 effect, from the top and the bottom of the domain. Figure 2 collects a few snapshots of the  
 303 trajectories resulting from the application of the random walk particle tracking to our numerical  
 304 system. The plane  $x_1 - x_3$  is aligned with the regional flow and  $\theta = 0$ . The hydraulic conductivity  
 305 field is generated with variance  $\sigma_Y^2 = 2$ . The figure shows as the particles placed in the highly-  
 306 conductive layers travel faster (see dark orange layer in Figure 2). On the contrary, the particles  
 307 in the low-conductive layers move very slowly (see light yellow layers in Figure 2).

308 Finally, flow and transport are performed on  $MC = 500$  Monte Carlo realizations, which  
 309 allow to obtain reliable estimates of the ensemble Breakthrough Curve (BTC). For each real-  
 310 ization  $i$ , we collected the breakthrough time  $\tau_{0,i}$  as the time needed for the fastest particle to  
 311 reach the pumping well, and the recirculating ratio  $RR_i$  as the ratio between the number of  
 312 particles at the pumping well to the total particles. The ensemble breakthrough time  $\langle \tau_0 \rangle$  and  
 313 recirculating ratio  $\langle RR \rangle$  are then calculated as

$$\langle \tau_0 \rangle = MC^{-1} \sum_{i=1}^{MC} \tau_{0,i} \quad (14)$$

$$\langle RR \rangle = MC^{-1} \sum_{i=1}^{MC} RR_i \quad (15)$$

314 Assuming ergodic transport, the breakthrough curve at the pumping well is calculated as  
 315 the Cumulative Distribution Function (CDF) of the travel times to the well considering all  
 316 simulations together. The BTC is subsequently scaled with the initial local velocity in order  
 317 to consider flux-proportional injection (see, e.g., Janković and Fiori, 2010; Pedretti and Fiori,  
 318 2013; Fiori et al., 2017; Di Dato et al., 2017). The temperature at the production well is finally

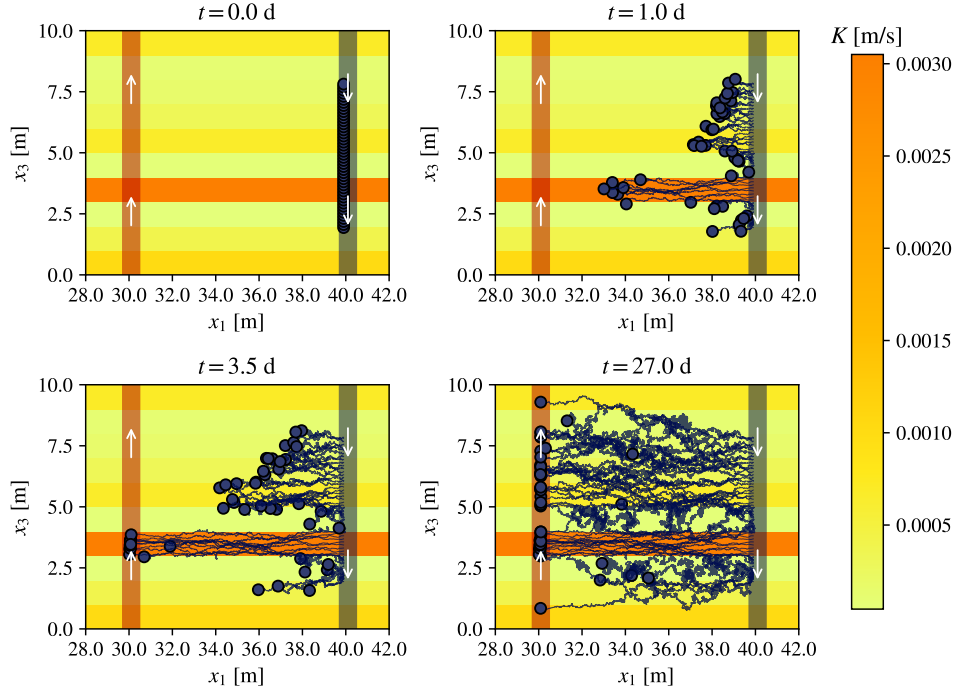


Figure 2: Four snapshots depicting the particle trajectories as a function of time. The plane  $x_1 - x_3$  is placed at  $x_2 = 0$ . The two wells are aligned with the regional flow (i.e.  $\theta = 0$ ). The thermal plume travels in a stratified medium with variance  $\sigma_Y^2 = 2$ , thermal diffusion  $D_{th} = 10^{-6} \text{m/s}^2$  and thermal dispersivity  $\alpha_d = 0.001 \text{ m}$ .

319 calculated by counting the number of particles converging at the production well, as follows  
 320 (Ferguson, 2006):

$$T_{prod}(t) = \frac{n(t)T_{well} + [N_p - n(t)]T_{ref}}{N_p} \quad (16)$$

321 where  $n(t)$  is the number of particles that have been collected at the time  $t$ . The numerical code  
 322 has been tested in order to verify that the number of Monte Carlo simulations and the number  
 323 of injected particles are enough to reach statistical convergence.

324 The parameters used for the simulations and listed in Table 1 were chosen as representative of  
 325 the geothermal systems typically designed (Galgaro and Cultrera, 2013; Piga et al., 2017). The  
 326 scenarios comprise two values of hydraulic gradient  $J$ , two values for the effective conductivity  
 327  $K_{eff}$ , three values of angle  $\theta$ , three values of heterogeneity degree  $\sigma_Y^2$ , two values of  $\alpha_d$  and  $D_{th}$   
 328 and thirteen pumping rates  $Q_w$ , for a total of 936 different combinations. In order to keep this  
 329 number small, we fixed those parameters that impact only the temporal scale at which thermal



330 feedback occurs, such as the porosity  $n$ , the aquifer depth  $B$ , the distance between the wells  
331  $L$ , the thermal retardation factor  $R_{th}$  and the temperature difference between the two wells.  
332 Generally the introduction of additional variability in the parameters involves an increase of  
333 heterogeneity in the results. The findings obtained here could be enhanced by considering, for  
334 instance, an heterogeneous porosity or a heterogeneous thermal dispersivity.

Parameter	Description	Value
Fixed parameters		
$n$	Porosity	0.1
$B$	Aquifer depth	10 m
$L$	Distance between the wells	10 m
$R_{th}$	Thermal retardation factor	3.4 <sup>a</sup>
$I_v$	Vertical integral scale	0.5 m <sup>b</sup>
$T_{well}$	Temperature at the injecting well	5°C
$T_{ref}$	Temperature in groundwater	15°C
Scenarios parameters		
$\theta$	Angle between wells and regional flow	0, $\pi/4$ , $\pi/2$
$\alpha_d$	Pore-scale dispersivity	0, 0.001 m <sup>c</sup>
$D_{th}$	Thermal diffusion	0, 1e-6 m/s <sup>2</sup> <sup>d</sup>
$K_{eff}$	Effective conductivity	0.001, 1e-5 m/s <sup>b</sup>
$\sigma_Y^2$	Variance of the log-conductivity field	Homog., 1, 2 <sup>b</sup>
$J$	Hydraulic gradient	0.01, 0.001
$Q_w$	Pumping rate	$X = [2 - 12]$ <sup>e</sup>

<sup>a</sup> See Casasso and Sethi (2015); <sup>b</sup> See Rubin (2003, Table 2.2); <sup>c</sup> See Fiori and Dagan (1999); <sup>d</sup>  
See Holman (2008, Appendix A, Table A-3); <sup>e</sup> The pumping rate is set up in order to obtain a  
 $\chi$  varying between 2 and 12

Table 1: Model parameters for the numerical experiments.

### 335 3. Results and Discussion

336 Results are shown in terms of breakthrough time  $\tau_0$ , recirculating ratio  $RR$  and temperature  
337 at the pumping well  $T_{prod}$  for different scenarios. We will analyze separately the impact of  
338 pore-scale processes and the angle between the wells and the regional flow. In the first case,  
339 the geothermal system is aligned with the groundwater flow (i.e.  $\theta = 0$ ). In the latter case the  
340 analysis is carried under pure advection (i.e.  $\alpha_d = 0$  and  $D_{th} = 0$ ).

#### 341 3.1. Breakthrough time

342 The first analysis we introduce deals with the homogeneous domain. Figure 3 shows the  
343 ratio  $\tau_0/\tau_{reg}$  as a function of  $\chi$ , which represents the dimensionless pumping rate. Results are  
344 normalized by  $\tau_{reg} = KJ/(R_{th}nL)$ , i.e. the time needed to travel the distance  $L$  when only  
345 regional flow is considered.

346 In Figure 3a different markers pertain to different couples of  $(K, J)$ , which determine different  
347 flow velocities in the system, whereas different colors are associated to different values of the pore-  
348 scale processes  $\alpha_d$  and  $D_{th}$ . Results show that generally  $\tau_0/\tau_{reg}$  decreases with an exponential  
349 behaviour with  $\chi$ , namely the higher the pumping rate, the shorter the first travel time. Such a  
350 result is consistent with previous studies (Milnes and Perrochet, 2013; Casasso and Sethi, 2015).  
351 Despite the general behaviour is similar, significant deviations from the purely advective solution  
352 can be noticed in the cases with lower velocities. In fact, when advective velocity decreases, the  
353 relative importance of diffusion increases. In such a case, the impact of thermal diffusion is  
354 not negligible, while the effect of pore-scale dispersivity appears to be always irrelevant in any  
355 simulated scenario. The previous analysis is supported by Figure 3b, which depicts a snapshot  
356 of the particle trajectories for the considered scenarios with  $D_{th} = 10^{-6}$  m/s<sup>2</sup>. We highlight  
357 that  $D_{th} = 10^{-6}$  m/s<sup>2</sup> is the typical thermal diffusion among the values encountered in natural  
358 aquifers (Holman, 2008). Inspection of figure shows that when the flow velocity is smaller  
359 (scenarios 3 and 4), the dispersion processes prevail and the trajectories assume a more chaotic  
360 pattern with respect to the scenarios where the advection prevails (1 and 2). As a consequence,  
361 analytical solutions for the geothermal system design should be carefully taken into account even  
362 for homogeneous media. In fact, by considering only advection, the analytical eq. (2) might  
363 lead to a significant overestimation of the breakthrough time.

364 The application range of solution  $\tau_0^{an}$  is explored in Figure 4, where the relative difference in

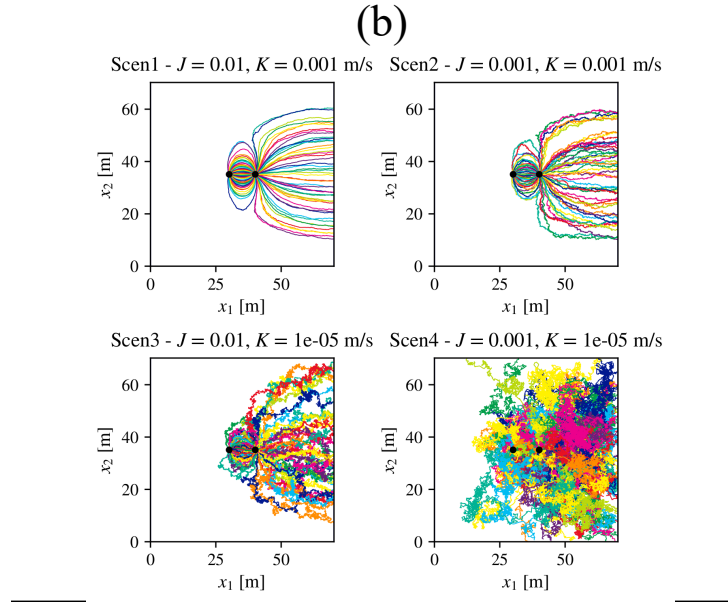
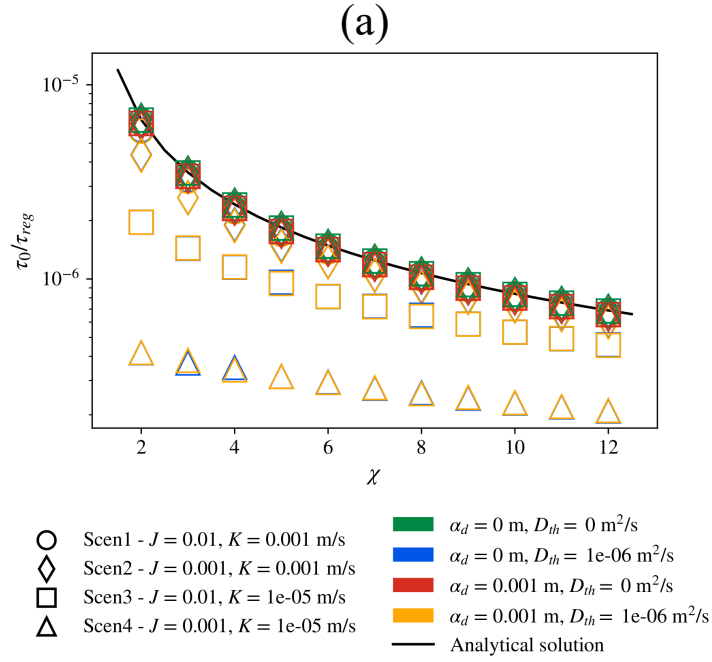


Figure 3: a) Normalized thermal breakthrough times  $\tau_0/\tau_{reg}$  as a function of the dimensionless pumping rate  $\chi$  for several scenarios depicting different regional flow, i.e. combinations of  $K$  and  $J$  in a homogeneous medium. Results are normalized by the time a particle needs to cover the distance  $L$  under uniform flow and advective transport. b) Pathlines in homogeneous porous media as a result of different combinations of average gradient ( $J$ ) and hydraulic conductivity values ( $K$ ) of the porous medium when thermal diffusion is  $D_{th} = 10^{-6}$  m/s<sup>2</sup>.

365 predicted breakthrough time  $|\tau_0 - \tau_0^{an}|/\tau_0^{an}$  is represented as function of  $D_{th}$  and  $\chi$ . This ratio,  
 366 namely the normalized absolute error of the analytical solution, approaches the zero value when  
 367 advection is dominant, while on the opposite case, i.e. when it approaches the value of one,  
 368 pore-scale heat transport mechanisms play the key role. Scenarios 1 and 2 are characterized by  
 369 higher flow velocities and are associated with small errors, therefore the analytical solution can  
 370 be used and the effect of dispersion is negligible. Focusing on the fourth scenario, it is possible  
 371 to observe how the accuracy of the travel time assessed with eq. (2) decreases with decreasing  $\chi$ ,  
 372 when the pumping rate is lower. In short, figure 4 confirms that the impact of heat conduction  
 373 on the breakthrough time is relevant only for low velocity systems, while advective transport  
 374 prevails in most cases.

375 We discuss now the effect of the heterogeneity of the hydraulic conductivity  $K$  on the break-  
 376 through time  $\tau_0$ . The medium heterogeneity, defined by the variance of the log-conductivity  $\sigma_Y^2$ ,  
 377 has been recognized as a key parameter in transport problem in natural aquifers, since velocity  
 378 gradients due to  $K$  variability triggers macrodispersion phenomena (Matheron and De Marsily,  
 379 1980; Dagan, 1986; De Barros and Rubin, 2011; Zech et al., 2015; Di Dato et al., 2016). In this  
 380 study we consider two heterogeneity scenarios, depicted by formation with mild heterogeneity  
 381 degrees, i.e.  $\sigma_Y^2 = 1$  and 2. Results are shown as a function of the dimensionless pumping rate  
 382  $\chi$ , which is defined by eq. (13) for the heterogeneous medium. The other parameters governing  
 383 the regional flow are kept constant and pertain to the second scenario in the previous paragraph,  
 384 i.e.  $J = 0.001$  and  $K_{eff} = 0.001$  m/s. It is worth noticing that in stratified media the effective  
 385 hydraulic conductivity corresponds to the arithmetic mean of  $K$ .

386 As in the previous paragraph, we analyze the mean breakthrough time  $\langle\tau_0\rangle$ , defined as the  
 387 expected value of the sample of the breakthrough times. The sample is composed of a number  
 388 of Monte Carlo simulations, i.e.  $MC = 500$ . The mean breakthrough time  $\langle\tau_0\rangle$  is depicted as  
 389 a function of  $\chi$  for four combinations of pore-scale dispersivity  $\alpha_d$  and thermal diffusion  $D_{th}$ ,  
 390 as shown in Figure 5. The homogeneous solutions and the analytical function (see eq. (14))  
 391 are depicted too as reference. Generally the behaviour appears to be similar to the previous  
 392 analysis, with  $\langle\tau_0\rangle$  that decreases for increasing  $\chi$  values. As expected, the effect of the medium  
 393 heterogeneity is to reduce the  $\langle\tau_0\rangle$ , which decreases moving from the homogeneous case to the  
 394  $\sigma_Y^2 = 1$  and  $\sigma_Y^2 = 2$  cases. Such behavior is a consequence of the larger sampling of the higher  
 395 values of the hydraulic conductivity involved by the higher  $\sigma_Y^2$ . The higher values of  $K$  are

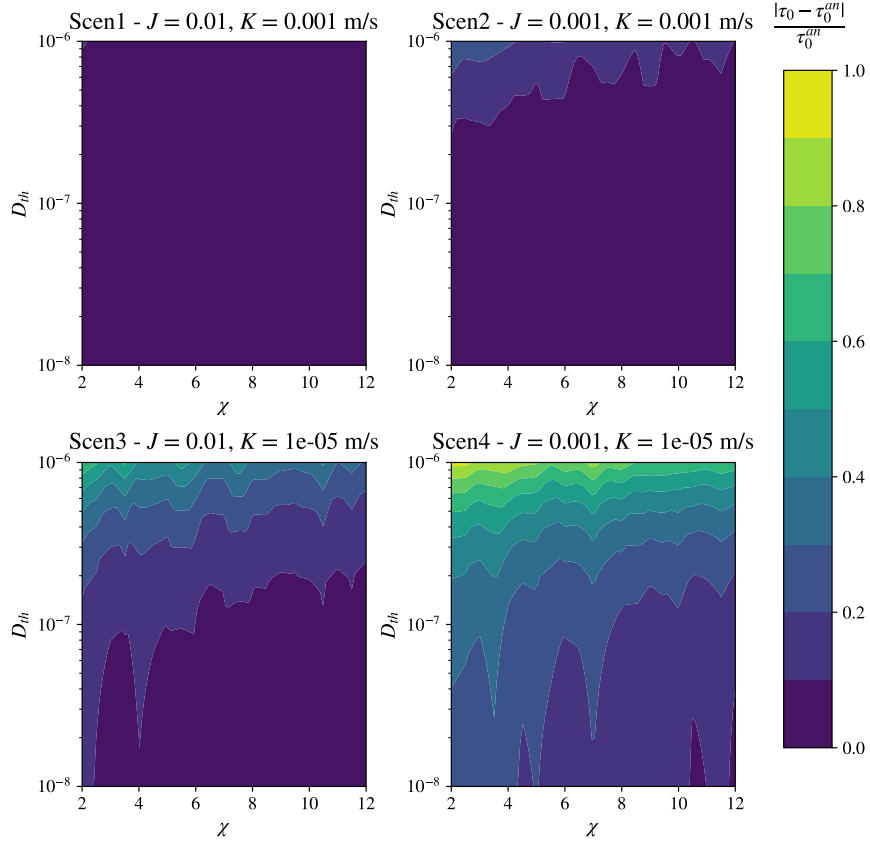


Figure 4: Contour plot of the difference between the numerical  $\tau_0$  and the analytical  $\tau_0^{an}$  (eq. (2)) for  $\chi$  and  $D_m$  and several regional flow scenarios. The plot provides also an indication of the governing transport mechanism, which is advective when  $|\tau_0 - \tau_0^{an}|/\tau_0^{an}$  tends to zero and dispersive when  $|\tau_0 - \tau_0^{an}|/\tau_0^{an}$  increases.

396 representative of the fast flow channels which develop in heterogeneous natural formations. As  
 397 showed in Figure 2, the particles placed in the higher-conductivity layer travel much faster than  
 398 the other ones. The inset of Figure 5 depicts also the coefficient of variation  $CV$  of  $\tau_0$  with  
 399 respect to the  $MC$  realizations as a function of  $\chi$  for several heterogeneity values. For the case  
 400  $\sigma_Y^2 = 2$ ,  $CV$  shows values higher than 2. This result is of paramount importance because it  
 401 indicates that  $\tau_0$  cannot be considered as a comprehensive index without the assessment of its  
 402 variability.

403 When analyzing different geometrical configurations obtained by varying the angle  $\theta$  between

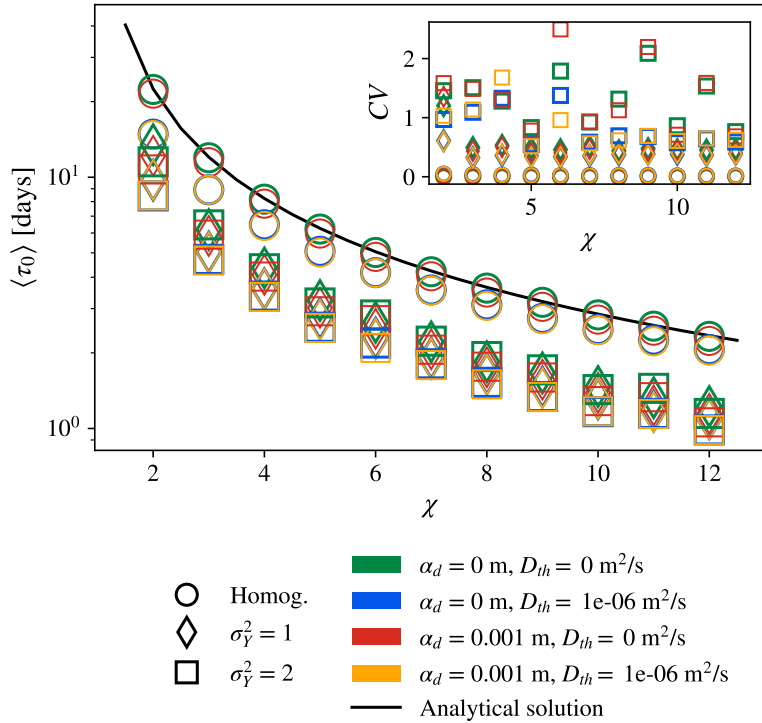


Figure 5: Mean breakthrough time  $\langle \tau_0 \rangle$  [d] as a function of  $\chi$  for several values of hydrodynamic dispersion  $\alpha_d$  and thermal diffusion  $D_{th}$ . The inset depicts the coefficient of variation  $CV$ . The mean value and the  $CV$  are calculated over a sample of  $MC = 500$  Monte Carlo simulations. Results are calculated for a well doublet aligned to the regional flow (i.e.  $\theta = 0$ ).

404 the wells and the regional flow, the most efficient setup is for  $\theta$  equal to zero. Otherwise, by  
 405 increasing the angle between the wells and the regional flow, the breakthrough time decreases,  
 406 as shown in Figure 6. This result is consistent with previous studies (Milnes and Perrochet,  
 407 2013; Casasso and Sethi, 2015). Such an aspect should be taken into consideration in practical  
 408 application, given that groundwater direction might be affected by seasonal variation (Bellin  
 409 et al., 1996).

410 It should be highlighted that in both cases, the results show slight differences in the mean  
 411  $\langle \tau_0 \rangle$  when  $\sigma_Y^2$  changes from 1 to 2. Liu et al. (2019) performed a similar analysis by studying the  
 412 relationship between thermal breakthrough time and conductivity heterogeneity with a variance  
 413 ranging between 0 and 6. As in the present work, they observed that the breakthrough time  
 414 decreases non-linearly with  $\sigma_Y^2$ , with smaller differences in the higher heterogeneity cases. In  
 415 contrast, the uncertainty associated to  $\tau_0$  in a single realization increases dramatically with

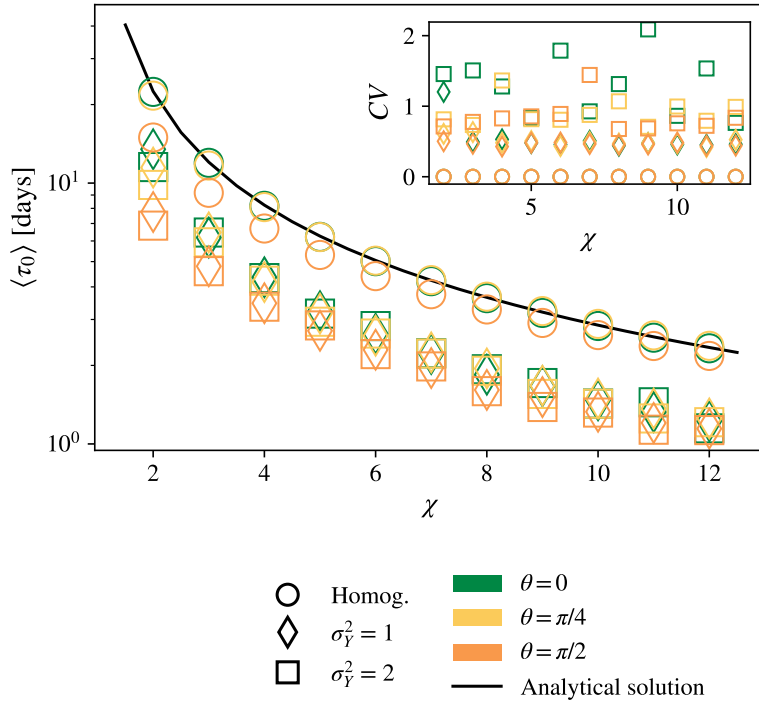


Figure 6: Mean breakthrough time  $\langle \tau_0 \rangle$  [d] as a function of  $\chi$  for several values of the angle between regional flow and wells  $\theta$ . The inset depicts the coefficient of variation  $CV$ . The mean value and the  $CV$  are calculated over a sample of  $MC = 500$  Monte Carlo simulations. Results are calculated under advection-only transport (i.e.  $\alpha_d = D_{th} = 0$ ).

416 heterogeneity, as shown by the coefficient of variation  $CV$  in the insets of both Figures 5 and 6.  
 417 However, such an uncertainty decreases with the number of layers when ergodicity is reached.  
 418 Such an issue will be discussed later in a dedicated paragraph.

### 419 3.2. Recirculating ratio $RR$

420 Along with the breakthrough time, which is an indicator of the early arrivals, the other  
 421 main operational metric of open-loop geothermal well doublets is the recirculating ratio  $RR$ ,  
 422 i.e. the fraction of the flow returning from the injection well to the production well, which is  
 423 instead an indicator of the long-term effects of returning flow. Figure 7 depicts the effect of  
 424 pore-scale dispersivity and thermal dispersion for both homogeneous and heterogeneous media  
 425 on the mean recirculating flow  $\langle RR \rangle$ . The results show that conductivity heterogeneity as well  
 426 as thermal dispersion processes generally have a small impact on  $\langle RR \rangle$ , significant differences  
 427 can be noticed only for the lower normalized pumping rate  $\chi < 6$ . Low pumping rate magnifies

428 the effect of preferential paths, thereby increasing the probability of particles to come back to  
 429 the production well. The coefficient of variation of  $\langle RR \rangle$ , shown in the inset, increases with  $\sigma_Y^2$   
 430 and decreases with  $\chi$  pointing at an higher uncertainty in domains characterized by an high  
 431 heterogeneity degree and a lower pumping rate.

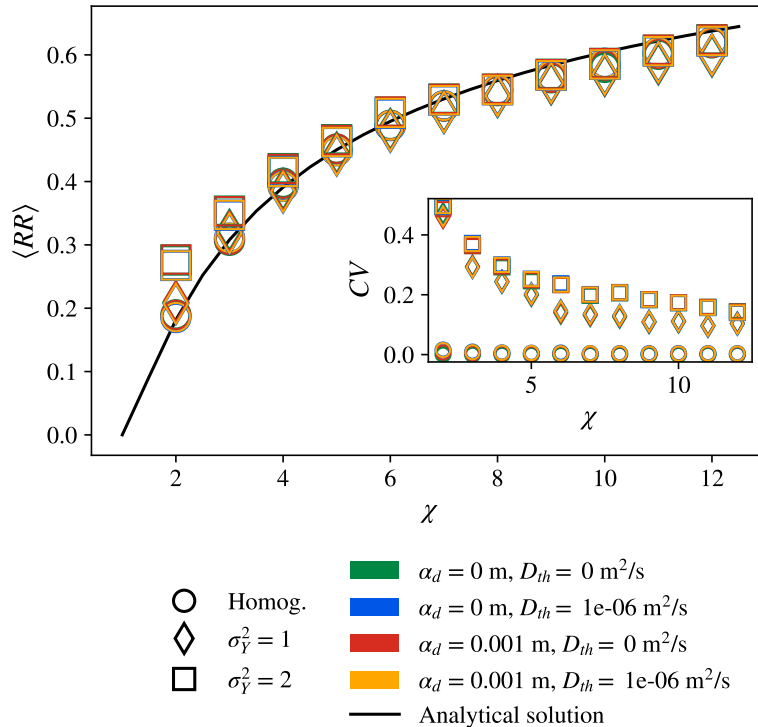


Figure 7: Mean recirculating ratio  $\langle RR \rangle$  as a function of  $\chi$  for several values of hydrodynamic dispersion  $\alpha_d$  and thermal diffusion  $D_{th}$ . The inset depicts the coefficient of variation  $CV$ . The mean value and the  $CV$  are calculated over a sample of  $MC = 500$  Monte Carlo simulations. Results are calculated for a well doublet aligned to the regional flow (i.e.  $\theta = 0$ ).

432 Figure 8 shows the mean recirculating ratio  $\langle RR \rangle$  as a function of  $\chi$  for several values of  
 433  $\theta$ , for both homogeneous and heterogeneous media under only advection (i.e.  $\alpha_d = D_{th} = 0$ ).  
 434 The most efficient configuration is when the wells and the regional flow are aligned, following  
 435 the breakthrough time behaviour. As in the previous analysis, when  $\chi$  is large the effect of the  
 436 heterogeneity is negligible on both the average value of  $\langle RR \rangle$  and its variation coefficient.

437 Furthermore we notice that while the  $CV$  for the  $\tau_0$  was around one, the  $CV$  for  $RR$  is smaller  
 438 than 0.2 for large  $\chi$ . Such a result indicates that the uncertainty related to the recirculating  
 439 volume is less affected by heterogeneity than breakthrough time. From a practical point of



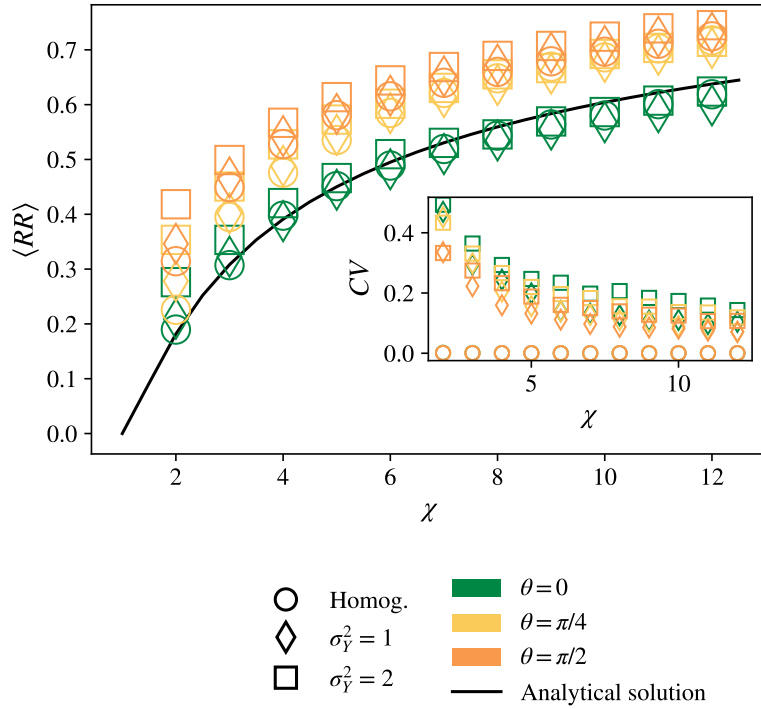


Figure 8: Mean recirculating ratio  $\langle RR \rangle$  as a function of  $\chi$  for several values of the angle between regional flow and wells  $\theta$ . The inset depicts the coefficient of variation  $CV$ . The mean value and the  $CV$  are calculated over a sample of  $MC = 500$  Monte Carlo simulations. Results are calculated under advection-only transport (i.e.  $\alpha_d = D_{th} = 0$ ).

440 view, this implies that the recirculating flow rate can be determined by considering the effective  
 441 conductivity instead of homogeneous conductivity. Consequently, the results from the analytical  
 442 solution can be a robust evaluation tool.

### 443 3.3. Temperature at the pumping well

444 Evaluating breakthrough times is key to assess whether thermal feedback will occur. Indeed,  
 445 even if  $\chi > 1$ , the breakthrough time is often larger than the duration of the heating/cooling  
 446 season and, hence, the water temperature at the production well remains unaltered. However,  
 447 the efficiency of the system does not depend on whether thermal breakthrough time occurs or not,  
 448 but on the time trend of operating temperatures. This holds true *a fortiori* for heterogeneous  
 449 aquifers, where thermal breakthrough time may occur within a very short time. As depicted by  
 450 the snapshots in Figure 2, the heterogeneous field is composed of alternating layers of high and  
 451 low conductivity. Consequently, particles in the high-conductive layers reach the production

452 well earlier than particles in the other zones. In contrast, the particles trapped in the low-  
 453 conductivity zones extend the arrival time of the last part of the plume. Therefore considering  
 454  $\tau_0$  only would mislead the evaluation of the operational sustainability of the system. For this  
 455 reason, we also analyzed the long-term evolution of water temperatures at the production well.  
 456 Figure 9 shows the temperature time trends for several typical values of  $\chi$  and for four  
 457 combinations of hydrodynamic dispersion  $\alpha_d$  and thermal diffusion  $D_{th}$ . Figure 10 depicts the  
 458 temperature evolution as a function of heterogeneity for several values of  $\theta$ .

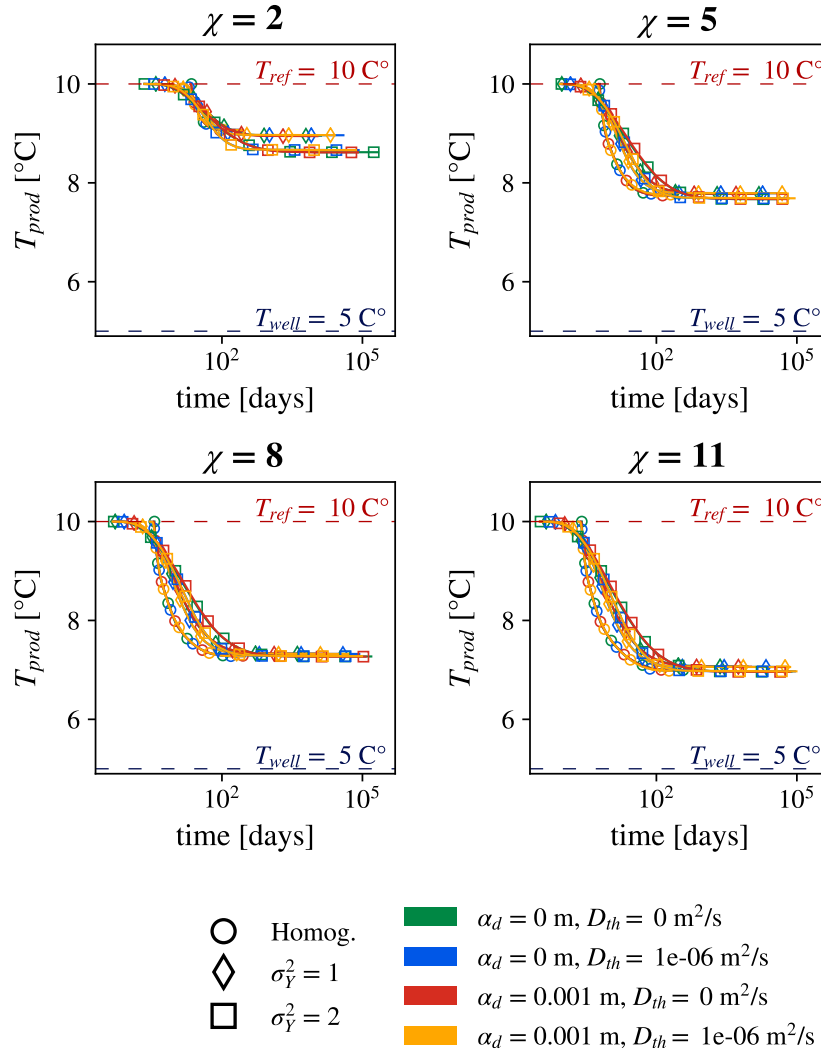


Figure 9: Temperature at the pumping well for several  $\chi$  values and for four combinations of hydrodynamic dispersion  $\alpha_d$  and thermal diffusion  $D_{th}$ . Results are calculated for a well doublet aligned to the regional flow (i.e.  $\theta = 0$ ).

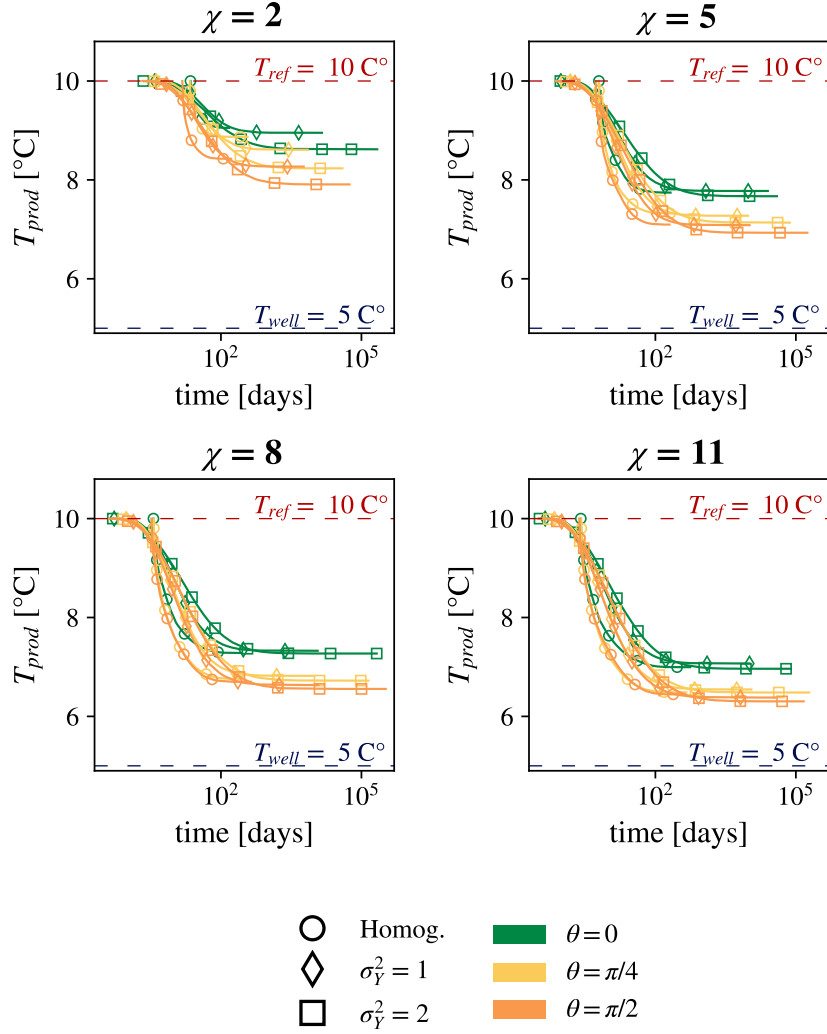


Figure 10: Temperature at the pumping well for several  $\chi$  values and for several values of  $\theta$ . Results are calculated under advection-only transport (i.e.  $\alpha_d = D_{th} = 0$ ).

459 Both figures confirm that the plume dispersion at the production well increases with heterogene-  
 460 ity, in line with experimental evidences (Sauty et al., 1982; Park et al., 2018). Heterogeneity  
 461 has a strong influence on the breakthrough time and on the shape of thermal breakthrough  
 462 curve. Also Babaei and Nick (2019) observed a similar behavior. Their study shows that con-  
 463 ductivity heterogeneity reduces the time needed to drop the temperature by 1°C when the initial  
 464 temperature is of 75°C and the reinjection is at 30°C.

465 In contrast, conductivity heterogeneity is negligible for the long-term development of ther-  
 466 mal feedback, as already observed for the recirculating ratio  $RR$ . Such behavior becomes more

467 evident by increasing  $\chi$ , when advection dominates over heat conduction. Although the break-  
468 through time decreases with heterogeneity, the overall efficiency of the system benefits from it.  
469 In fact, the temperature decreases faster when the medium is homogeneous, as shown by the  
470 lines with circle markers in Figures 9 and 10. The effect of thermal dispersion on BTC shape  
471 increases with medium heterogeneity: while the four BTCs overlap for homogeneous medium,  
472 heterogeneity causes a departure in BTCs depending on the  $D_{th}$  value. Thermal diffusion ac-  
473 celerates the development of thermal feedback as well, as shown in Figure 9.

474 The angle  $\theta$  has a small impact on the thermal breakthrough time, for which the effect of  
475 heterogeneity predominates. In contrast, the BTC long-term behavior is controlled mainly by  
476 the well doublet angle  $\theta$  and heterogeneity plays a negligible effect.

### 477 3.4. The ergodicity issue

478 As stated previously, the *CV* in the insets of Figures 5-8 shows the uncertainty associated  
479 to heterogeneity. In the present study, the coefficient of variation indicates the dispersion of the  
480 single realizations around their ensemble mean. Here we have considered a sample of  $MC =$   
481 500 Monte Carlo realizations. However, the coefficient of variation decreases by increasing the  
482 aquifer depth. When the wells are deep enough to totally grasp the variability of conductivity  
483 heterogeneity, the single realization approaches the ensemble mean. Only under such a case, it  
484 is possible to assume the ergodic condition, which allows to consider the single realization as  
485 representative of the ensemble mean (Kitanidis, 1988; Dagan, 1991; Fiori, 1998; Dentz et al.,  
486 2000). Given that well screens usually cross a short depth (typically from a few meters to a  
487 few tens of meters), ergodicity could not always be assumed, thereby increasing the uncertainty  
488 associated with the predicted ergodic BTC. Figure 11 shows the BTCs for each realization and  
489 the ensemble BTCs averaged over an increasing number of Monte Carlo simulations ( $MC$ ).

490 For the case considered here, i.e. aquifer depth is composed of ten layers, the single BTC  
491 realization can significantly differ from its ergodic counterpart. As a practical consequence,  
492 a thermal feedback occurring in a heterogeneous medium could significantly differ from the  
493 expected theoretical one, which typically assumes ergodicity. Moreover, the uncertainty of the  
494 single realization increases with medium heterogeneity. Figure 11 shows that ergodic conditions  
495 are reached averaging over 10 to 20 realizations, which correspond to 100-200 layers according to  
496 the heterogeneity degree. As a consequence, the analysis associated to this kind of uncertainty  
497 should be carefully considered while designing geothermal systems in heterogeneous media.

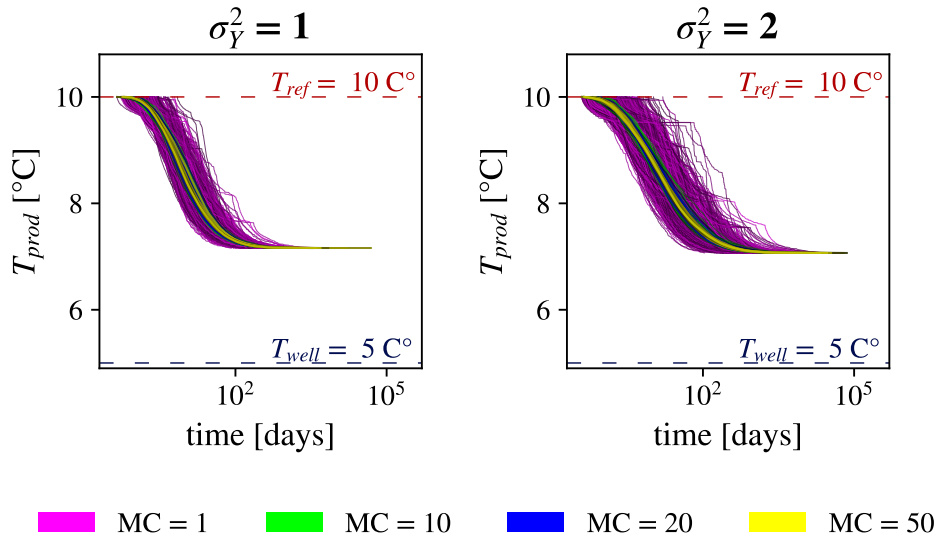


Figure 11: Sample of BTCs used ( $MC = 500$  realizations) and the ensemble BTC as function of the MC simulations (layers).

498 This last issue is of paramount importance in studies dealing with the efficiency of geothermal  
 499 systems. When the exploitation plant is made of wells crossing a small number of geological  
 500 formations, the temperature evolution in time can significantly differ with the expected one,  
 501 based on model results, whose parameters are usually defined by a limited number of tests. In  
 502 contrast, modeling results are more reliable when the wells cross a large number of geological  
 503 formations. Finally we highlight that additional sources of uncertainty on results could arise  
 504 considering variability in other parameters, such as the porosity or the thermal dispersion, which  
 505 are kept constant within this extensive analysis. Despite this we believe that our results can be  
 506 considered as general and can provide a suitable basis for a more reliable efficiency assessment  
 507 of shallow geothermal energy systems.

#### 508 4. Conclusions

509 The present study analyzed the interplay of thermal dispersion and macrodispersion in heat  
 510 transport, thereby focusing on the role of heterogeneity and thermal dispersivity in the design  
 511 of open-loop shallow geothermal systems. We analyzed the following metrics: the breakthrough  
 512 time, corresponding to the time the reinjected water needs to reach the production well; the  
 513 recirculating rate, i.e. the fraction of injecting water returning to the production well; and the

514 temperature curve at the production well.

515 The main findings are:

- 516 • The effects of thermal dispersion parameters are strictly related to the pumping rates and,  
517 in general, to the groundwater velocity values. In general, thermal dispersion becomes  
518 appreciable in systems characterized by low pumping rates.
  
- 519 • The heterogeneity has a strong impact on the early operational time of geothermal well  
520 doublets. Due to channeling, the thermal plume travels faster in the highly conductive  
521 layers. As a result, the breakthrough time decreases with heterogeneity. Moreover, the  
522 uncertainty associated with early arrivals increases with heterogeneity. Such behavior  
523 confirms evidences already observed by Liu et al. (2019) and Babaei and Nick (2019).
  
- 524 • The heterogeneity, as well as dispersion and convection, has a negligible effect on the  
525 long-term period. The recirculating ratio depends strongly on the parameter  $\chi$  and the  
526 angle  $\theta$ , namely it can be modelled by assuming advection only. Therefore the analytical  
527 solution for the recirculating ratio  $RR^{an}$  gives a robust assessment of the long-term system  
528 sustainability.
  
- 529 • The thermal plume spreads more when increasing the variance of medium conductivity.  
530 The breakthrough time can therefore be misleading as an indicator of the system efficiency  
531 and the whole thermal BTC should be considered. Heterogeneity should be carefully con-  
532 sidered, because trajectory dispersion magnifies the variance of arrival times. In highly  
533 heterogeneous aquifers, the time span between thermal breakthrough time and a substan-  
534 tial development of thermal feedback can be long enough for the heating/cooling season  
535 to end. Consequently the system could benefit from the medium heterogeneity. On the  
536 other hand, the uncertainty due to non-ergodic conditions should be taken into serious  
537 consideration as well.

538 The present work can be considered as a first step towards a better understanding of the cou-  
539 pled effect of aquifer heterogeneity and engineering design on the efficiency of shallow geothermal  
540 systems. Despite significant assumptions were adopted (i.e. stratified formation, steady state  
541 flow, constant injection temperature), the study highlighted and explained noteworthy mod-  
542 elling issues. For instance, we found that heterogeneity has a minor impact on the long-term

543 behavior, but it has a tremendous impact on the short-term counterpart. As a consequence, the  
544 assessment of the system efficiency should rely not only on the breakthrough time, but also on  
545 the complete temperature evolution at the production well. In contrast, simplified analytical  
546 solutions assuming only advection work well to assess the long-term sustainability of the system.

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