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1 **Bioavailability of hydrophobic organic chemicals on an in vitro metabolic**
2 **degradation using rat liver S9 fraction**

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20 **ABSTRACT**

21 Metabolic transformation of highly hydrophobic organic chemicals (HOCs) is one of the most
22 important factors modulating their persistence, bioaccumulation and toxicity. Although sorption of HOCs
23 to cellular matrices affects their bioavailability, it is still not clear how the cellular binding or sorption of
24 HOCs in in vitro metabolism assays influences their enzymatic transformation kinetics. To elucidate
25 effects of non-specific binding to enzymes, we measured apparent enzyme kinetics in an in vitro assay
26 using four polycyclic aromatic hydrocarbons (phenanthrene, anthracene, pyrene and benzo[a]pyrene) as
27 model HOCs and S9 mixture isolated from rat liver as a model enzyme mixture. Bovine serum albumin
28 (BSA) was also selected as non-metabolically active protein to investigate effects of protein binding. The
29 observed transformation rates were much higher than those predicted assuming that only freely dissolved
30 HOCs are available for metabolism. A new model including kinetic exchanges between non-specifically
31 bound HOCs and those bound to active enzyme binding sites explained the apparent degradation kinetics
32 at various experimental conditions better. The results are relevant for in vitro-in vivo extrapolation because
33 the metabolic transformation rate in vivo may depend strongly on the local enzyme density and the micro-
34 cellular environment. While non-specific protein binding reduces the unbound fraction of chemicals, this
35 effect could be partially compensated by the facilitated transport to the active sites of the enzymes.

36

37 **Keywords** – enzyme kinetics; facilitated transport; non-specific sorption; equilibrium binding constants;
38 in vitro-in vivo extrapolation (IVIVE)

40 **Introduction**

41 Enzymatic transformation of hydrophobic organic chemicals (HOCs) has been of significant
42 interest because their environmental persistence, bioaccumulation potential, and toxicity strongly depend
43 on their metabolic transformation rate (Cowan-Ellsberry et al. 2008; Lee et al. 2019; Lo et al. 2016;
44 Nichols et al. 2006). The increasing need to evaluate how fast HOCs undergo metabolic transformation
45 cannot be met by in vivo studies because of long experimental time, high experimental cost and ethical
46 concerns. High-throughput in vitro assays are accepted as alternatives to in vivo testing and they come at
47 various levels of complexity to evaluate potential for enzymatic degradation (Austin et al. 2002; Connors
48 et al. 2013; Cowan-Ellsberry et al. 2008; Han et al. 2007; Jones and Houston 2004; Kleinow et al. 1998;
49 Lee et al. 2019; Lo et al. 2015). The simplest method among them is to measure the depletion of a parent
50 chemical in the presence of microsomes or S9 mixture isolated from liver homogenate (Austin et al 2002;
51 Cowan-Ellsberry et al. 2008; Lee et al. 2019).

52 In an enzymatic assay, the assay medium contains high density of proteins and other cellular
53 materials. It is well-known that hydrophobic chemicals are strongly bound to cellular matrices and this
54 sorption may affect their bioavailability (Austin et al. 2002; Fischer et al. 2019; Glden and Seibert 2005;
55 Heringa et al. 2004; Hestermann et al 2000; Kwon et al. 2007). Reduced bioavailability of HOCs in such
56 systems is often explained by the equilibrium sorption to medium and non-target sites, which makes them
57 unavailable for the receptors in the test system. For example, Heringa et al. (2004) showed that serum
58 protein concentration strongly influences dose-response relationship in an estrogenicity reporter gene
59 assay and the effect concentrations should be normalized to free concentrations of hydrophobic estrogenic
60 chemicals. Recent studies have confirmed this observation for a wide range of chemicals using a combined
61 modeling and measurement approach (Escher et al. 2019; Fischer et al. 2017; Henneberger et al. 2019).
62 Similarly, Austin and co-workers have shown that metabolic transformation rate is approximately constant

63 if corrected for the extent of non-specific binding although the apparent transformation rate normalized to
64 protein concentration decreases with increasing enzyme concentration (Austin et al. 2002, 2005). However,
65 their work was limited to mostly ionizable pharmaceuticals of which the logarithms of ionization-
66 corrected distribution ratios between 1-octanol and water at pH 7.4 ($\log D_{7.4}$) were lower than 3.0.

67 On the contrary to the interpretation of decreased transformation rates caused by decrease in freely
68 dissolved concentration, several studies noted that non-specific sorption might accelerate the transport of
69 HOCs to the active target sites (Bittner et al. 2011; Blanchard et al. 2005; Bowman and Benet 2018; Escher
70 et al. 2011; Fujino et al. 2018; Kim et al. 2019; Matsunaga et al. 2019; Miyauchi et al. 2018; Poulin et al.
71 2016). Non-reactive proteins such as albumin are able to form substrate-albumin complexes and these
72 complexes could deliver the substrate to the active target site. In vitro hepatic clearance rate was measured
73 greater than expected with the decreased freely dissolved concentration in the extracellular medium
74 especially for chemicals that strongly bind to albumin (Blanchard et al. 2005; Bowman and Benet 2018;
75 Kim et al. 2019; Poulin et al. 2016). Escher et al. (2011) compared bioconcentration factor (BCF) of HOCs
76 in fish by extrapolating in vitro metabolic degradation rate obtained using S9 fraction isolated from
77 rainbow trout (*Oncorhynchus mykiss*) with in vivo experimental values. The extrapolated BCF value for
78 hydrophobic nonylphenol assuming that only freely dissolved fraction is available for metabolic
79 degradation was much greater than the experimental BCF-values, suggesting a possibility of delivering
80 nonylphenol non-specifically bound to proteins and other cellular matrices. However, the role of non-
81 specific sorption of HOCs to the bioavailability in metabolic degradation is still not very clear although
82 this is crucial for extrapolating in vitro biodegradation studies to in vivo bioconcentration of highly HOCs.

83 In this study, we evaluated the effects of non-specific sorption on the apparent enzymatic kinetics
84 in an in vitro metabolic degradation assay using four highly hydrophobic polycyclic aromatic
85 hydrocarbons (PAHs), phenanthrene, anthracene, pyrene and benzo[a]pyrene, as model HOCs.

86 Commercially available S9 mixture isolated from rat liver homogenate was chosen as the model enzyme
87 mixture to provide a proof of principle. Apparent first-order transformation rate constants were measured
88 at various S9 enzyme concentrations, alone and in the presence of various concentrations of bovine serum
89 albumin (BSA). BSA was chosen as non-metabolically active protein in order to investigate effects of
90 non-specific sorption to proteins. In parallel, non-specific binding was measured in form of partition
91 constants between S9 mixture and buffer and between BSA and buffer. A new enzyme kinetics model was
92 proposed to explain the experimental data in this study.

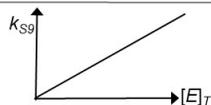
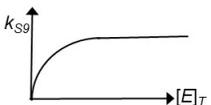
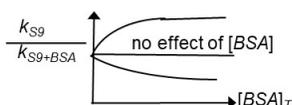
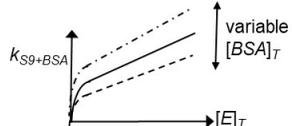
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94 **Enzyme kinetic models**

95 Enzymatic degradation of a substrate, S , can be described simply by model 1 in Figure 1, where E
96 is the enzyme, $E-S$ is the enzyme-substrate complex after substrate binding to active enzyme sites, P is
97 the product, and k_1 , k_{-1} , k_2 are kinetic rate constants. Assuming irreversibility of metabolic transformation
98 and pseudo-steady state of the formation of $E-S$, a simple rate expression well-known as Michaelis-Menten
99 kinetics is obtained. Equation 1 describes the rate of the total substrate depletion.

$$100 \text{ rate} = -\frac{d[S]_T}{dt} = \frac{k_2[E]_T[S]_T}{\frac{k_{-1}+k_2}{k_1} + [S]_T} = \frac{V_{max}[E]_T[S]_T}{K_m + [S]_T} \quad (1)$$

101 where $[E]_T$ is the total concentration of the enzyme (mg L^{-1}), $[S]_T$ is the total substrate concentration (nmol
102 L^{-1}), V_{max} is the maximum velocity ($\text{nmol mg}^{-1} \text{min}^{-1}$) and K_m is the half-saturation constant (nmol L^{-1}).

Reactions	rate of substrate depletion $-\frac{d[S]_T}{dt}$	relationship between the pseudo-first order depletion rate constant of substrate k_{S9} and $[E]_T$
Model 1: Michaelis-Menten $S_T + E \xrightleftharpoons[k_{-1}]{k_1} E-S \xrightarrow{k_2} P$	$-\frac{d[S]_T}{dt} = \frac{k_2[E]_T[S]_T}{\frac{k_{-1} + k_2}{k_1} + [S]_T} \approx \frac{k_2[E]_T[S]_T}{\frac{k_{-1} + k_2}{k_1}}$	$k_{S9} = \frac{k_1 k_2}{k_{-1} + k_2} [E]_T$ 
Model 2: only free substrate is available $S_{free} + E \xrightleftharpoons[k_{-1}]{k_1} E-S \xrightarrow{k_2} P$ $S_{ns, S9} \xrightleftharpoons[K_{ns}]{S_{free}}$	$-\frac{d[S]_T}{dt} = \frac{k_1 k_2}{k_{-1} + k_2} \cdot \frac{[E]_T [S]_T}{1 + K_{ns} [E]_T}$	$k_{S9} = \frac{k_1 k_2}{k_{-1} + k_2} \cdot \frac{[E]_T}{1 + K_{ns} [E]_T}$ 
Model 3: non-specifically sorbed substrate may be delivered to the active enzymatic binding site $S_{free} + E \xrightleftharpoons[k_{-1}]{k_1} E-S \xrightarrow{k_2} P$ $S_{ns} \xrightleftharpoons[K_{ns, S9}]{S_{free}} \xrightleftharpoons[K'_{-1}]{K'_1} E-S$	$-\frac{d[S]_T}{dt} = \frac{k_1 k_2}{k_{-1} + k'_{-1} + k_2} \cdot \frac{\left(1 + \frac{k'_1}{k_1} K_{ns} [E]_T\right) [E]_T [S]_T}{1 + K_{ns} [E]_T}$	$k_{S9} = \frac{k_1 k_2}{k_{-1} + k'_{-1} + k_2} \cdot \frac{\left(1 + \frac{k'_1}{k_1} K_{ns} [E]_T\right) [E]_T}{1 + K_{ns} [E]_T}$ 
Model 4: substrate sorbed non-specifically to enzyme or to other protein may be delivered to the active enzymatic binding site $S_{free} + E \xrightleftharpoons[k_{-1}]{k_1} E-S \xrightarrow{k_2} P$ $S_{ns, BSA} \xrightleftharpoons[K_{ns, BSA}]{S_{free}} \xrightleftharpoons[K'_{-1}]{K'_{-1}} E-S$ $S_{ns, S9} \xrightleftharpoons[K_{ns, S9}]{S_{free}} \xrightleftharpoons[K'_{-1}]{K'_1} E-S$		

103

104 **Figure 1.** Models describing enzymatic degradation kinetics: model 1, classical Michaelis-Menten model,
 105 applicable if the nominal concentration of substrate $[S]$ is available; model 2 applicable if only free
 106 substrate $[S]_{free}$ are available; model 3, applicable if non-specifically sorbed substrate $[S]_{ns}$ may be
 107 delivered to the active enzymatic binding site; and model 4 applicable if there are other proteins (e.g.,
 108 BSA) that can sorb substrate and the sorbed substrates may be delivered to the active binding site on S9
 109 protein.

110

111 However, for HOCs, a large fraction of the substrate may be bound non-specifically to other
 112 protein sites than the active site (Austin et al. 2002; Heringa et al. 2004; Hestermann et al. 2000). Thus,
 113 the rate of formation of product is more likely to depend on freely dissolved substrate concentration $[S]_{free}$

114 than on the total concentration of substrate $[S]_T$ that is spiked in the assay medium due to non-specific
 115 binding to experimental matrices. Therefore, we may include non-specific binding in the kinetic model 2
 116 as shown in Figure 1. In general, non-specific sorption of hydrophobic chemicals between water and nano-
 117 sized cellular materials are known to be much faster than enzymatic degradation half-life (Cócera et al.
 118 2001; Kraus et al. 2018; Schlautman and Morgan 1993). If we assume that equilibrium is obtained
 119 instantaneously, we can model the effects of non-specific sorption using the distribution constant between
 120 proteins and the solution. Free substrate concentration, $[S]_{free}$, can be estimated by assuming that $[E-S]$ is
 121 negligible (i.e., $[S]_T \cong [S]_{ns} + [S]_{free}$) compared to free and non-specifically sorbed substrates as:

$$122 \quad [S]_{free} = \frac{[S]_T}{1 + K_{ns}[E]_T} \quad (2)$$

123 where K_{ns} is the distribution constant between protein and the buffer solution ($L \text{ kg}^{-1}$) via non-specific
 124 sorption defined by equation 3.

$$125 \quad K_{ns} = \frac{[S]_{ns}}{[E]_T[S]_{free}} \quad (3)$$

126 If total substrate concentration is sufficiently low (eq. 4),

$$127 \quad \frac{k_{-1} + k_2}{k_1} \gg [S]_T \quad (4)$$

128 and only free substrates are available for metabolic transformation, equation 1 can be written as:

$$129 \quad -\frac{d[S]_T}{dt} = \frac{k_1 k_2}{k_{-1} + k_2} \cdot \frac{[E]_T}{1 + K_{ns}[E]_T} [S]_T \quad (5)$$

130 Thus, the apparent first-order rate constant would be expected to increase linearly with increasing enzyme
 131 concentration at sufficiently low $[E]_T$, then approach a constant value as $[E]_T$ increases (eq. 6).

$$132 \quad k_{S9} = \frac{k_1 k_2}{k_{-1} + k_2} \frac{[E]_T}{1 + K_{ns}[E]_T} \quad (6)$$

133 If we additionally assume that the non-specifically sorbed substrate can be delivered to the active
 134 site on the enzyme (Model 3 in Figure 1), and describe this process with the rate constants, k'_1 and k'_{-1} ,

135 we obtain a modified rate expression as follows (see Section A, Electronic Supplementary Material for
 136 mathematical derivation):

$$137 \quad -\frac{d[S]}{dt} = \frac{k_1 k_2}{k_{-1} + k_{-1}' + k_2} \cdot \frac{\left(1 + \frac{k_1'}{k_1} K_{ns}[E]_T / 10^6\right) [E]_T}{1 + K_{ns}[E]_T} [S]_T \quad (7)$$

138 There are two limiting cases of model 3. If the free fraction of substrate dominates (i.e., $K_{ns}[E]_T$
 139 $\ll 1$ and $k_1' K_{ns}[E]_T \ll k_1$) and the substrate concentration is much below the saturation level, equation 7
 140 is simplified to:

$$141 \quad -\frac{d[S]_T}{dt} = \frac{k_1 k_2 [E]_T}{k_{-1} + k_{-1}' + k_2} [S]_T \quad (8)$$

142 in which the pseudo-first order rate constant is proportional to the total enzyme concentration. On the
 143 other hand, if the bound forms dominate (i.e., $K_{ns}[E]_T \gg 10^6$ and $k_1' K_{ns}[E]_T \gg 10^6 k_1$) and the substrate
 144 concentration is low enough, equation 5 is simplified to:

$$145 \quad -\frac{d[S]_T}{dt} = \frac{k_1' k_2 [E]_T}{k_{-1} + k_{-1}' + k_2} [S]_T \quad (9)$$

146 Equation 9 is similar to equation 6 except for the slope. The ratio of the slope in equation 8 to that in
 147 equation 9 is equal to the ratio of association rate constants (i.e., k_1 to k_1').

148 To test if the concept of non-specific sorption is applicable, we can add a second, enzymatically
 149 inactive protein, bovine serum albumin (BSA). The reaction model implementing this additional process
 150 is depicted in Figure 1 (model 4) but the kinetic equations are not solved.

151 We measured the transformation rate as a function of substrate concentration for a small number
 152 of controls to assure that $[S]_T \ll K_m$ (See Figure 1, Supplementary Data). Under this condition it is possible
 153 to determine a pseudo-first order rate constant of substrate depletion (k_{S9}) which is equivalent to
 154 $V_{max}[E]_T/K_m$. Thus plotting k_{S9} versus $[E]_T$ will indicate which kinetic model describes the experimental
 155 data best (Figure 1).

156

157 **Materials and methods**

158 **Materials**

159 Four polycyclic aromatic hydrocarbons (PAHs), phenanthrene (CAS RN 85-01-8, 98%, Aldrich,
160 Buchs, Switzerland), anthracene (CAS RN 120-12-7, 99%, Fluka, Buchs, Switzerland), pyrene (CAS RN
161 129-00-0, 99%, Fluka), and benzo[*a*]pyrene (CAS RN 50-32-8, 99.9%, Supelco, Bellefonte, PA), were
162 chosen as model hydrophobic compounds to evaluate their transformation kinetics in the presence of the
163 enzyme mixture at various non-reactive protein concentrations. Hexachlorobenzene (CAS RN 118-74-1,
164 >99%, Fluka) was used as reference chemical in the sorption experiments because it is hardly degradable.
165 Uninduced rat S9 mixture (Catalog no. RTS9-PL) was purchased from CellzDirect, Inc. (Austin, TX). The
166 protein content of the S9 mixture from the supplier was used. Bovine serum albumin (BSA),
167 dimethylsulfoxide (DMSO), NADP-sodium salts, glucose-6-phosphate, magnesium sulfate, and
168 tris(hydroxymethyl)aminomethyl-chloride (Tris-HCl) were of high purity and purchased from Sigma-
169 Aldrich, Inc. (St. Louis, MO).

170

171 **Chemical analyses**

172 Concentration of selected PAHs was analyzed using high-performance liquid chromatography
173 system equipped with a P680 HPLC pump and an ASI-100 autosampler (Dionex Softron GmbH,
174 Germering, Germany). They were separated on a C18 Supelcosil LC-PAH column (150 mm × 4.6 mm, 5
175 μm, Supelco, Bellefonte, PA) at 40°C and detected using an RF-2000 fluorescence detector (Dionex). The
176 excitation wavelength was 275 nm for phenanthrene, 260 nm for anthracene and pyrene, and 290 nm for
177 benzo[*a*]pyrene and the emission wavelengths were 350 for phenanthrene, 420 nm for anthracene and

178 pyrene, and 430 nm for benzo[a]pyrene. De-ionized water and acetonitrile were used as the mobile phase
179 in isocratic mode with the flow rate of 1 mL min⁻¹.

180

181 **Determination of partition constants and sorption constants**

182 Partition constants between polydimethylsiloxane (PDMS) and 50 mM Tris buffer solution at pH
183 7.8 ($K_{PDMSbuffer}$) were determined using a dynamic permeation method (Kwon et al. 2007). In short,
184 $K_{PDMSbuffer}$ values were calculated from the apparent permeation rate constant from a PDMS disk loaded
185 with chemicals to a clean PDMS disk separated by the buffer solution, k_d (s⁻¹), using the following
186 relationship:

$$187 \quad K_{PDMSbuffer} = \frac{D_{buffer} \cdot A \cdot 1}{\delta_{buffer} \cdot V_{PDMS} \cdot k_d} \quad (10)$$

188 where D_{buffer} is the diffusion coefficient of a chemical in the buffer solution (m² s⁻¹), δ_{buffer} is the aqueous
189 boundary layer thickness in the buffer solution (estimated to be 12.5 μm in a previous study; Kwon et al.
190 2007), A is the surface area of the PDMS disk (m²), V_{PDMS} is the volume of the PDMS disk (m³), and k_d is
191 the experimentally measured rate constant (s⁻¹). D_{buffer} was assumed to be equal to the aqueous diffusion
192 coefficient estimated using a correlation with solute's molecular weight (Kwon et al. 2007).

193 The sorption constants between buffer solution and denatured S9, native BSA or denatured BSA
194 were measured using a PDMS depletion method (Escher et al. 2011; Kwon et al. 2009; Ter Laak et al.
195 2005). Rat S9 protein and BSA were denatured by increasing the pH of the solution using the equivalent
196 volume of NaOH (yields pH of 14), then immersing the vials for 5 minutes in boiling water, followed by
197 adjusting pH to 9.0 using concentrated HCl. In this way the precipitation of the denatured protein could
198 be avoided.

199 The detailed procedures of measuring partition constants and sorption constants were described
200 previously (Kwon et al. 2007, 2009). PDMS disks loaded with chemical species were depleted in the

201 presence of various volumes of deactivated S9 or BSA solution. Partition constants $K_{PDM/Ssus}$ were
 202 obtained using a non-linear regression between the fraction lost to the suspension ($C_{PDMS}/C_{PDMS,0}$) and the
 203 volume ratio V_{sus}/V_{PDMS} ($m^3_{suspension} m^{-3}_{PDMS}$):

$$204 \frac{C_{PDMS}}{C_{PDMS,0}} = \frac{1}{1 + \frac{V_{sus}/V_{PDMS}}{K_{PDMS/sus}}} \quad (11)$$

205 where C_{PDMS} is the concentration of a chemical in PDMS after equilibrium ($mol m^{-3}$), $C_{PDMS,0}$ is the initial
 206 concentration in PDMS ($mol m^{-3}$), $K_{PDM/Ssus}$ is the partition constant between PDMS and the suspension
 207 containing S9 or BSA ($m^3_{suspension} m^{-3}_{PDMS}$). Then, the partition constant between protein and buffer
 208 ($K_{protein/buffer}$, $L kg^{-1}$) was calculated by

$$209 K_{protein/buffer} = \frac{\frac{K_{PDMS/buffer}}{K_{PDMS/sus}} - 1}{m_{protein}} \quad (12)$$

210 where $K_{PDMS/buffer}$ is the partition constant between PDMS and buffer and $m_{protein}$ is protein concentration
 211 in the suspension ($kg L^{-1}$). These partition constants were used to quantitatively describe non-specific
 212 binding (or sorption) in the metabolic transformation assay.

213

214 **In vitro metabolic transformation assay**

215 Apparent degradation rate constants were measured at various S9 enzyme concentrations. 8 μL of
 216 dimethylsulfoxide containing the test chemical was spiked into an amber vial containing 10 mM NaNADP,
 217 10 mM $MgCl_2$, 40 mM glucose-6-phosphate, and desired concentration of S9 and BSA in 50 mM Tris
 218 buffer (pH 7.8) to make a total volume of 1600 μL . The initial concentration of selected PAHs was
 219 approximately 100 nM, which is low enough to fall into the linear range of Michaelis-Menten kinetics
 220 based on published half-saturation constants of PAHs (Fitzsimmons et al. 2001) and confirmed by the
 221 screening experiments in the presented set-up (Figure S1, Electronic Supplementary Material). The

222 solution was shaken gently (90 rpm) at 25°C in the dark. After pre-determined incubation time (up to 2
223 h), 200 µL of the solution was taken and immediately mixed with 1800 µL ice-cold acetonitrile to quench
224 the enzymatic transformation. The mixture was then centrifuged at 3,000 g for 10 min to precipitate
225 proteins and the supernatant was taken for chemical analysis. The pseudo-first order degradation rate
226 constant k_{S9} was obtained using linear regression (eq. 11) using concentration measured at six different
227 time points.

$$228 \ln \frac{[S]}{[S_0]} = -k_{S9}t \quad (13)$$

229 For a control experiment, changes in concentration of PAHs were also measured in the presence of
230 denatured S9.

231

232 **Results**

233 **Partition constants between S9 and buffer and between BSA and buffer**

234 Table 1 shows all partition and sorption constants obtained in this study and a comparison of the
235 data with octanol-water partition constants (K_{ow}), PDMS-water partition constants (K_{PDMSw}), and
236 liposome-water partition constants (K_{lipw}) using palmitoyl-oleoyl-phosphatidylcholine from literature
237 (Jonker and van der Heijden 2007).

238 Values of $K_{PDMSbuffer}$ were $10^{3.69}$, $10^{3.82}$, $10^{4.13}$, and $10^{5.01}$ for phenanthrene, anthracene, pyrene, and
239 benzo[*a*]pyrene, respectively, as shown in Table 1 (see Figure S2, Electronic Supplementary Material for
240 experimental determination of the mass transfer kinetics). The values of $K_{PDMS/buffer}$ resulting from a fit of
241 the experimentally measured rate constants were slightly but not statistically significantly smaller than
242 K_{PDMSw} obtained using de-ionized water (Kwon et al. 2007).

243 Table 1 also shows $K_{S9/buffer}$, $K_{BSA(native)/buffer}$ and $K_{BSA(denatured)/buffer}$ values obtained using equation
244 12 after determining $K_{PDMSsus}$ using non-linear regression (eq 11) of the fraction remaining in PDMS

245 ($C_{PDMS}/C_{PDMS,0}$) versus volume ratio (see Figure S3, Electronic Supplementary Material). $K_{BSA(native)/buffer}$
246 and $K_{BSA(denatured)/buffer}$ agreed well, indicating that the assumption is justified that non-specific binding of
247 HOCs to proteins can be regarded as a partitioning process. Control experiments with hexachlorobenzene,
248 which is not metabolizable, also indicated that sorption is not only independent of the tertiary structure of
249 BSA but also independent of the tertiary structure of the S9, because there was no difference between
250 $K_{S9(native)/buffer}$ and $K_{S9(denatured)/buffer}$ (see Figure S4, Electronic Supplementary Material) and pH changes
251 prior and after the denaturation affected the results only slightly. $K_{BSA(native)/buffer}$ values were lower than
252 K_{ow} values by a factor of 14 (pyrene) to 72 (benzo[*a*]pyrene). This difference is in a good agreement with
253 a compilation of data showing that protein-water partition constants are lower than K_{ow} by approximately
254 a factor of 20 (de Bruyn and Gobas 2007).

255 **Table 1.** Summary of partition constants between PDMS and Tris-buffer ($K_{PDMS/buffer}$), between S9 and buffer ($K_{S9/buffer}$) and between BSA and buffer
 256 ($K_{BSA/buffer}$) with literature $\log K_{ow}$, $\log K_{PDMSw}$, and $\log K_{lipw}$.

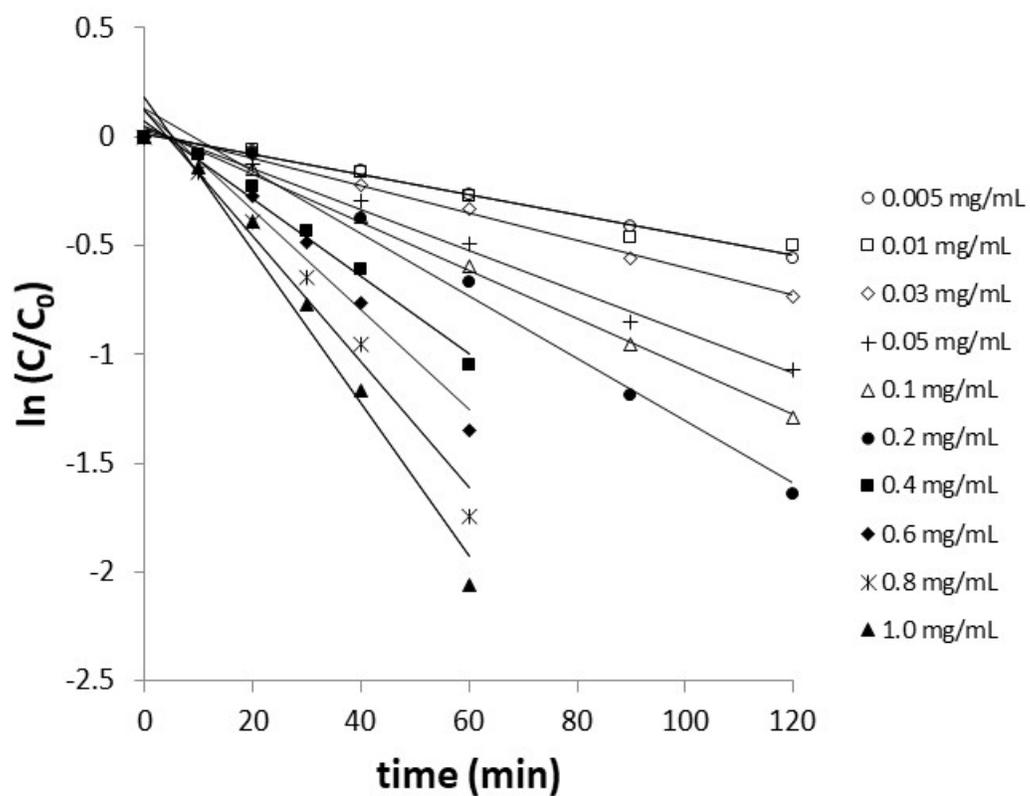
Partition constants							
Chemical	$\log K_{ow}$	$\log K_{PDMSw}$	$\log K_{lipw}$	$\log K_{PDMS/buffer}$	$\log K_{S9/buffer}$	$\log K_{BSA(native)/buffer}$	$\log K_{BSA(denatured)/buffer}$
Phenanthrene	4.52 ^a	3.87 (3.77, 3.96) ^b	4.86 ^c , 5.07 ^d	3.69 (3.57, 3.78)	4.38 (4.23, 4.49)	3.20 (3.00, 3.33)	3.09 (2.80, 3.33)
Anthracene	4.50 ^a	3.98 (3.88, 4.06) ^b	5.15 ^d	3.82 (3.72, 3.91)	4.57 (4.43, 4.68)	3.33 (3.21, 3.43)	3.30 (2.98, 3.27)
Pyrene	5.00 ^a	4.36 (4.26, 4.45) ^b	5.78 ^d	4.13 (3.97, 4.25)	4.87 (4.61, 5.03)	3.85 (3.66, 3.98)	3.59 (3.31, 3.37)
Benzo[<i>a</i>]pyrene	6.35 ^a	5.09 (4.98, 5.18) ^b	6.98 ^c , 7.41 ^d	5.01 (4.90, 5.09)	5.88 (5.63, 6.04)	4.49 (4.32, 4.61)	4.50 (4.26, 4.65)

257 Values in parenthesis are the lower and the upper 95% confidence limits calculated using error propagation. ^aValues of $\log K_{ow}$ are recommended
 258 values in Sangster (1989). ^bValues are from Kwon et al. (2007). ^cValues are from Kwon et al. (2009). ^dValues are from Jonker and van der Heijden
 259 (2007) using SPME method.

260 **Effects of enzyme concentration on the metabolic rate**

261 Concentration of PAHs remained unchanged in the presence of denatured S9. The degradation in
262 presence of native S9 followed first-order reaction kinetics with r^2 values mostly higher than 0.9. Figure
263 2 shows an example of pseudo-first order kinetic decay for benzo[*a*]pyrene at various S9 concentrations.
264 Figure 3 shows the pseudo-first order substrate depletion rate constants k_{S9} (min^{-1}) at various S9 enzyme
265 concentrations for the selected PAHs compiled from at least three different independent experiments.
266 There were detectable rate constants even at very low S9 concentration ($0.025 - 0.05 \text{ mg}_{\text{protein}} \text{ mL}^{-1}$). There
267 was a steep increase in the rate constant followed by a gradual linear increase with increasing enzyme
268 concentration. Dashed and solid lines in Figure 3 denote best-fit lines for model 2 and 3 (eq 5 and 7),
269 respectively, using the experimentally measured $K_{S9/\text{buffer}}$ values as K_{ns} values.

270 A linear relationship between the apparent rate constant and the total enzyme concentration would
271 be expected according to the classical Michaelis-Menten kinetics (model 1) and the saturation of the
272 apparent rate constant would be expected with increase of the total enzyme concentration according to model
273 2 but neither model can explain the experimental data. The experimental bi-phasic increase in the apparent
274 rate constant is best explained by model 3 that assumes that non-specifically bound HOCs are also
275 available for enzymatic degradation. The initial steep increase followed by a steady increase in the
276 apparent rate constant indicates that freely dissolved PAHs are more readily available for enzymatic
277 degradation but PAHs non-specifically bound to S9 and cellular matrices are also bioavailable and cannot
278 be neglected although their contribution is slower, so they are not fully available. This means for equation
279 5 that k_1 is much higher than k'_1 but k'_1 is sufficiently greater than zero to affect the apparent degradation
280 kinetics.

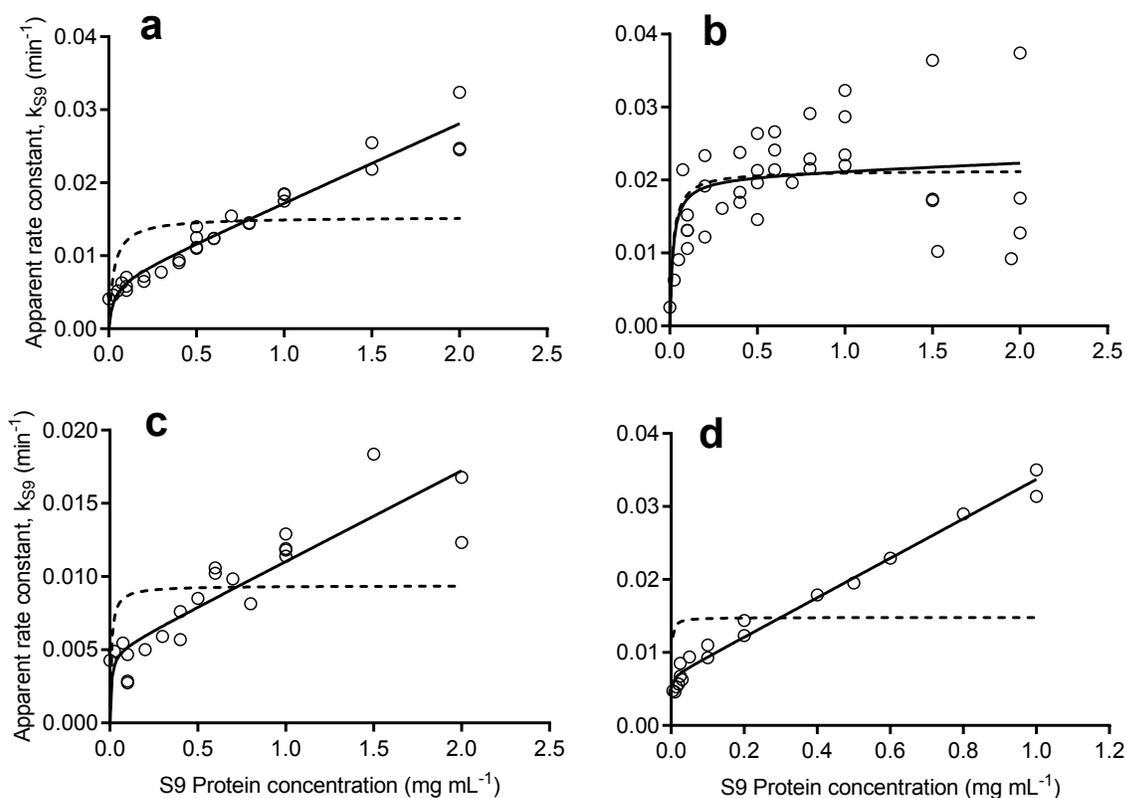


281

282 **Figure 2.** Determination of pseudo-first order rate constant at various S9 concentration for
 283 benzo[*a*]pyrene as an example. C and C_0 stand for the total substrate concentration at time t and $t=0$.

284

285



286

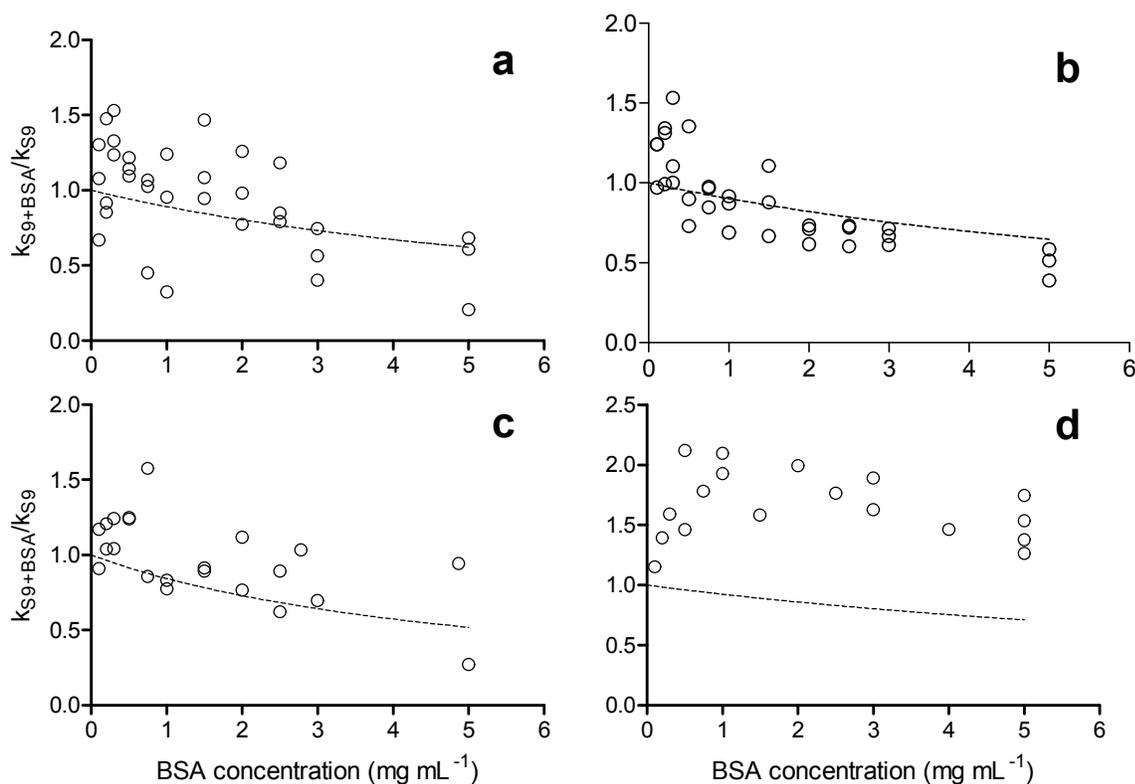
287 **Figure 3.** Apparent first-order rate constant k_{S9} at various enzyme concentrations for (a) phenanthrene,
 288 (b) anthracene, (c) pyrene, and (d) benzo[a]pyrene. The solid lines illustrate the best-fit curves using the
 289 new model (equation 7) with the best-fit parameters given in the Electronic Supplementary Material
 290 (Table S1). For comparison, the dashed lines show the model that assumed that only free substrates are
 291 available (equation 6).

292

293 Effects of variable BSA concentrations

294 We also tested if additional non-specific binding has the same effect as S9 by running experiments
 295 with mixtures of 0.5 mg mL⁻¹ S9 with different BSA concentrations (0 to 5 mg mL⁻¹). Figure 4 shows
 296 apparent first-order rate constants k_{S9+BSA} normalized by the rate constant without BSA, k_{S9} . These ratios
 297 k_{S9+BSA}/k_{S9} decreased with increasing BSA for phenanthrene, anthracene, and pyrene (Figure 4a, b, and
 298 c). However, the opposite trend was observed for benzo[a]pyrene (Figure 4d). Dashed lines refer to
 299 predicted ratios k_{S9+BSA}/k_{S9} with using $K_{BSA/buffer}$ and $K_{S9/buffer}$ under the assumption that non-specific

300 sorption to BSA makes the substrate unavailable for enzymatic degradation and distribution of species in
301 the assay medium is near equilibrium (model 2). The decrease in the freely dissolved concentration by
302 adding BSA to the system satisfactorily explained the decreased apparent rate constants for phenanthrene,
303 anthracene and pyrene although data scattered, whereas this hypothesis fails to explain the experimental
304 data of benzo[*a*]pyrene.
305



306
307 **Figure 4.** Apparent relative first-order rate constant in the presence of bovine serum albumin k_{S9+BSA}/k_{S9}
308 for (a) phenanthrene, (b) anthracene, (c) pyrene, and (d) benzo[*a*]pyrene. The concentration of S9 mixture
309 was 0.5 mg mL^{-1} . Dashed lines illustrate expected curves if only free substrate $[S]_{\text{free}}$ is available for
310 enzymatic degradation (model 2 in Figure 1).

311

312 Discussion

313 **Non-specific sorption of PAHs to S9 and BSA**

314 As summarized in Table 1, $K_{BSA(native)/buffer}$ and $K_{BSA(denatured)/buffer}$ agreed well, indicating that
315 sorption of HOCs to proteins could be regarded as non-specific partitioning. Losing the tertiary structure
316 of the protein through denaturation does not seem to affect the partitioning. Negligible differences
317 between $K_{S9(native)/buffer}$ and $K_{S9(denatured)/buffer}$ for the positive control using non-degradable
318 hexachlorobenzene also supports that this non-specific sorption is independent on the tertiary structure of
319 BSA or S9 and the solution pH (Figure S4). This finding is important because it confirms that the $K_{S9/buffer}$
320 values, which need to be determined with denatured S9 to differentiate binding from degradation, are
321 representative for native S9. In addition, $\log K_{BSA/buffer}$ increased with increasing $\log K_{ow}$ (Table 1),
322 suggesting that the affinity of PAHs to albumin is rather unchanged, but the decrease in their aqueous
323 solubility increases $\log K_{BSA/buffer}$.

324 It is also interesting that the experimentally determined $K_{S9/buffer}$ values were higher than $K_{BSA/buffer}$
325 by approximately one order of magnitude (Table 1). Although protein content of the commercial S9
326 mixture used in this study was quantified and all results were expressed in relation to protein content of
327 the S9, there was no information on the amount of residual lipids. Liposome-water partition constants
328 (K_{lipw}) of the selected PAHs using palmitoyl-oleoyl-phosphatidylcholine were slightly higher than their
329 K_{ow} values (Jonker and van der Heijden 2007; Kwon et al. 2009) as shown in Table 1. Thus, only 5-10%
330 of residual lipid (w/w) may result in the extraordinarily high sorption constant due to dominating
331 contribution of residual lipids. For comparison, fetal bovine serum contains 2.9 % lipids ($m_{lip}/(m_{lip}+m_{protein})$)
332 (Fischer et al. 2017) and it is conceivable that S9 has a similar lipid content. In contrast the commercially
333 available BSA is purified and fatty acid-free. Although further validation is needed to rationalize the
334 unusually high non-specific sorption to S9 proteins, these sorption constants can be used for the purpose
335 of evaluation of bioavailability of highly HOCs in S9 enzymatic degradation assay.

336

337 **Comparison of enzyme kinetic models**

338 As shown in Figure 3, the apparent enzymatic degradation rate constants for the four PAHs
339 followed model 3, indicating that HOCs non-specifically sorbed to non-active site of S9 proteins and other
340 organic matter such as proteins and lipids in the medium are still available for enzymatic degradation
341 although they are not as promptly available as freely dissolved forms.

342 The extension of the proposed kinetic model (model 4 in Figure 1) provides a useful insight for
343 the availability of HOCs to the enzymatic degradation in more complex and thus closer to in vivo
344 conditions. If we assume that substrates non-specifically bound to non-reactive proteins such as BSA are
345 still available for enzymatic activation (i.e., forming $[E-S]$ complex), we may introduce another
346 association rate constant (k_1'') from sorbed to BSA to the active reaction site and dissociation rate constant
347 (k_{-1}'') from the active site to sorbed to BSA. If k_1'' is negligibly small compared to k_1 or k_1' , normalized
348 rate constants would be close to that predicted by the model shown in Figure 4. On the other hand, we
349 may not neglect the effects of k_1'' in the overall enzymatic kinetics if k_1'' is not negligibly small. The
350 experimental results of benzo[*a*]pyrene can be predicted if k_1'' is higher than k_1' . Thus, the observed
351 enzymatic degradation kinetics may or may not decrease depending on the chemical investigated and its
352 sorption behavior. Krauss and Goss (2018a, b) proposed in vitro-in vivo extrapolation models including
353 desorption rate constants of HOCs from protein to explain how binding to proteins affect the overall
354 hepatic clearance. Because hepatic metabolism depends on desorption rate constant, fraction bound to
355 proteins, and the intrinsic metabolic rate constant by enzymes (Krause and Goss, 2018b), further
356 investigation on enzymatic kinetics in the presence of various cellular matrices is required.

357

358 **Implications for environmental bioconcentration of HOCs**

359 Many highly HOCs are suspected to bioconcentrate in aquatic and terrestrial organisms and the
360 key parameter that determines the BCF is in vivo clearance rate (Cowan-Ellsberry et al. 2008; Lee et al.
361 2019; Nichols et al. 2006). Experimental data in this study clearly showed that not only freely dissolved
362 HOCs are available for metabolic degradation but also HOCs non-specifically bound to serum proteins

363 or residual lipids are available, providing a clue why experimental BCF values for HOCs are often found
364 to be greater than extrapolated using in vitro enzymatic degradation rate (Escher et al. 2011).

365

366 **Implications for human quantitative in vitro to in vivo extrapolation models (QIVIVE)**

367 The mechanistic model presented here for in vitro metabolism has also implications for the in vivo
368 situation in human pharmacokinetic models, where it is difficult to estimate the quantitative contribution
369 of non-specifically bound HOCs to be delivered to the active enzymatic sites. Recent studies provided
370 evidence of the facilitated transport of drugs by albumin-mediated uptake mechanisms for the protein
371 bound fraction in hepatocytes and cardiac myocytes (Fujino et al. 2018; Kim et al. 2019; Matsunaga et al.
372 2019; Poulin et al. 2016). These findings obtained in a cellular environment are consistent with our study
373 in a cell-free environment. Facilitated transport mechanisms warrant further investigations. Since in vitro
374 studies aim at an extrapolation to in vivo, results from in vitro study should be applied for prediction of
375 fate in vivo with great care because the actual metabolic rate in vivo may also depend on local enzyme
376 density and micro-cellular environment. The changes in the apparent degradation rate or the clearance
377 rate should be assessed for more HOCs in the presence of diverse matrices in the microenvironment where
378 the metabolic transformation takes place.

379

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385

386 **Electronic Supplementary Material**

387 Derivation of rate expressions of enzymatic degradation in the presence of non-specific binding is
388 presented in the Supporting Information. In addition, supplementary raw data is presented (determination
389 of partition constants between PDMS and buffer, BSA and S9, additional partitioning data on
390 hexachlorobenzene, experimental derivation of rate constants).

391

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521

Declaration of interests

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

The authors declare the following financial interests/personal relationships which may be considered as potential competing interests:

Bioavailability of hydrophobic organic chemicals on an in vitro metabolic degradation using rat liver S9 fraction

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Contents:

A. Mathematical derivations of rate expressions in equation 7.

Figure S1. Relationship between transformation rate ($\Delta C/\Delta t$) and initial concentration of substrate for benzo[*a*]pyrene as an example.

Figure S2. Determination of partition coefficients between PDMS and Tris buffer solution, pH 7.8, $K_{PDMSbuffer}$.

Figure S3. Determination of partition coefficients (a) phenanthrene, (b) anthracene, (c) pyrene, and (d) benzo[*a*]pyrene between PDMS and deactivated S9 protein suspension $K_{S9buffer}$ and (e) phenanthrene, (f) anthracene, (g) pyrene, and (h) benzo[*a*]pyrene between PDMS and BSA suspension $K_{BSA(native)buffer}$.

Figure S4. Determination of partition coefficients of hexachlorobenzene between PDMS and S9 protein or BSA suspension, in native state or denatured with using various methods, including pH change, pH adjusted to 14 and then boiling for 5 min, and adjustment to various pH-values.

Table S1.

A. Mathematical derivations of rate expressions in equation 7

As described in Figure 1 of the main text, non-specific binding of substrate may affect enzymatic degradation kinetics. If we assume that (1) formation of degradation product is irreversible, (2) non-specific binding is very fast and can be considered to be in equilibrium, and (3) concentration of active enzyme-substrate complex is at pseudo-steady state, we can write the differential equations describing the reactions as follows:

$$\frac{d[P]}{dt} = -\frac{d[S]}{dt} = k_2[E-S] \quad (\text{A1})$$

$$\frac{d[E-S]}{dt} = 0 = k_1[S]_{free}[E] + k_1'[S]_{ns}[E] - k_{-1}[E-S] - k_{-1}'[E-S] - k_2[E-S] \quad (\text{A2})$$

Mass balance equations on both enzyme and substrate give

$$[E]_T = [E] + [E-S] \quad (\text{A3})$$

$$[S] = [S]_{free} + [S]_{ns} + [E-S] \cong [S]_{free} + [S]_{ns} \quad (\text{A4})$$

The ratio of non-specifically bound substrate to free substrate can be given by the equilibrium distribution ratio as:

$$K_{ns} = \frac{[S]_{ns}/[E]_T}{[S]_{free}} = \frac{[S] - [S]_{free}}{[E]_T[S]_{free}} \quad (\text{A5})$$

where $[E]_T$ has units of kg L^{-1} and K_{ns} has units of L kg^{-1} . Plugging A3-A5 into A2 and rearranging gives

$$[E-S] = \frac{[E]_T[S]_{free}}{\frac{k_{-1} + k_{-1}' + k_2}{k_1 + k_1'K_{ns}[E]_T} + [S]_{free}} \quad (\text{A6})$$

Thus, apparent enzymatic degradation rate becomes

$$-\frac{d[S]}{dt} = \frac{k_2[E]_T[S]_{free}}{\frac{k_{-1} + k_{-1}' + k_2}{k_1 + k_1'K_{ns}[E]_T} + [S]_{free}} \quad (\text{A7})$$

Plugging equation 2 of the main text into equation (A7) gives

$$-\frac{d[S]}{dt} = \frac{k_2[E]_T[S]}{\frac{(k_{-1} + k_{-1}' + k_2)(1 + K_{ns}[E]_T)}{k_1 + k_1'K_{ns}[E]_T} + [S]} \quad (\text{A8})$$

If the substrate concentration is sufficiently low (eq 7 in main text), one obtains equation 5 in the main text:

$$-\frac{d[S]}{dt} = \frac{k_1 k_2}{k_{-1} + k_{-1}' + k_2} \cdot \frac{\left(1 + \frac{k_1'}{k_1} K_{ns}[E]_T\right) [E]_T}{1 + K_{ns}[E]_T} [S] \quad (7)$$

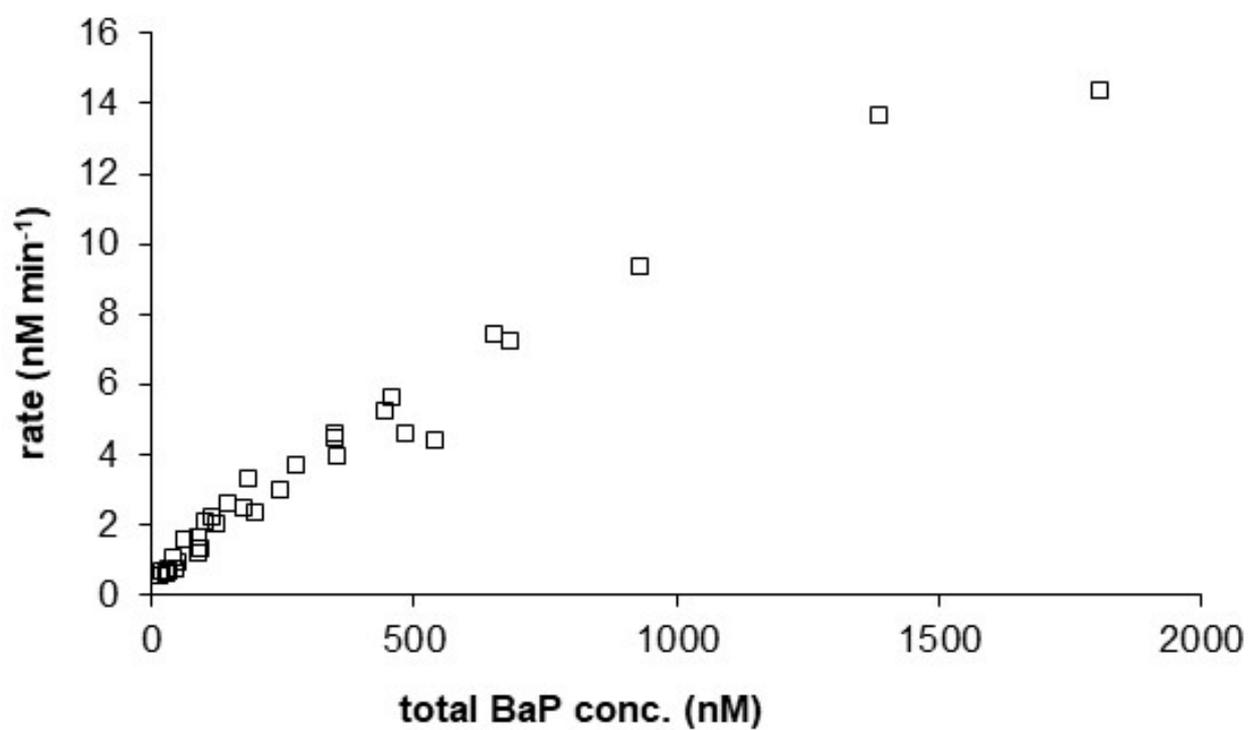


Figure S1. Relationship between degradation rate of benzo[a]pyrene (BaP) in nM min^{-1} and its initial concentration as an example.

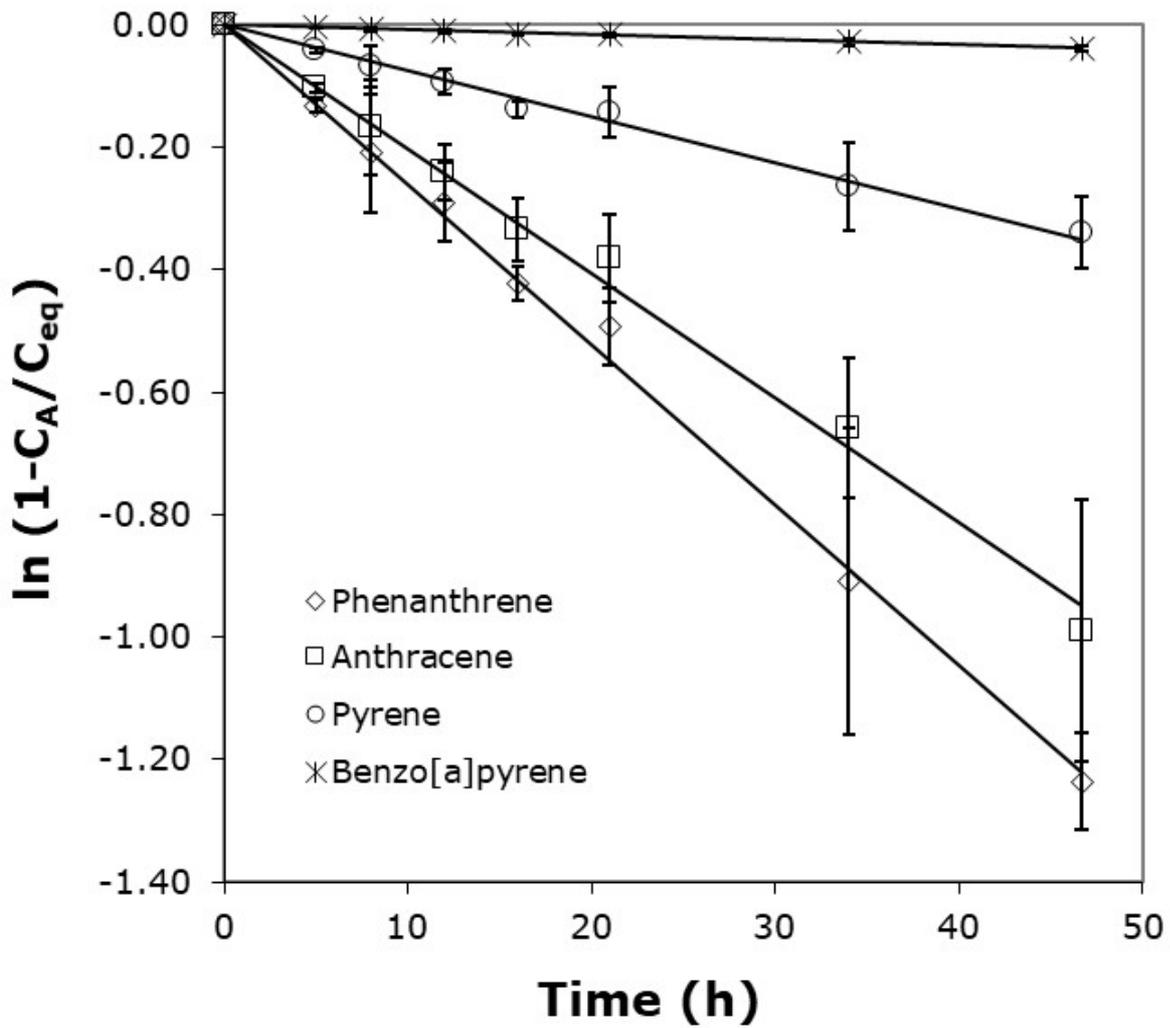


Figure S2. Determination of partition constants between PDMS and the buffer solution ($K_{PDMS/buffer}$) according to Kwon et al. (2007). C_A and C_{eq} present the concentration in the acceptor PDMS and that in equilibrium, respectively. Error bars denote standard deviation of triplicate analysis.

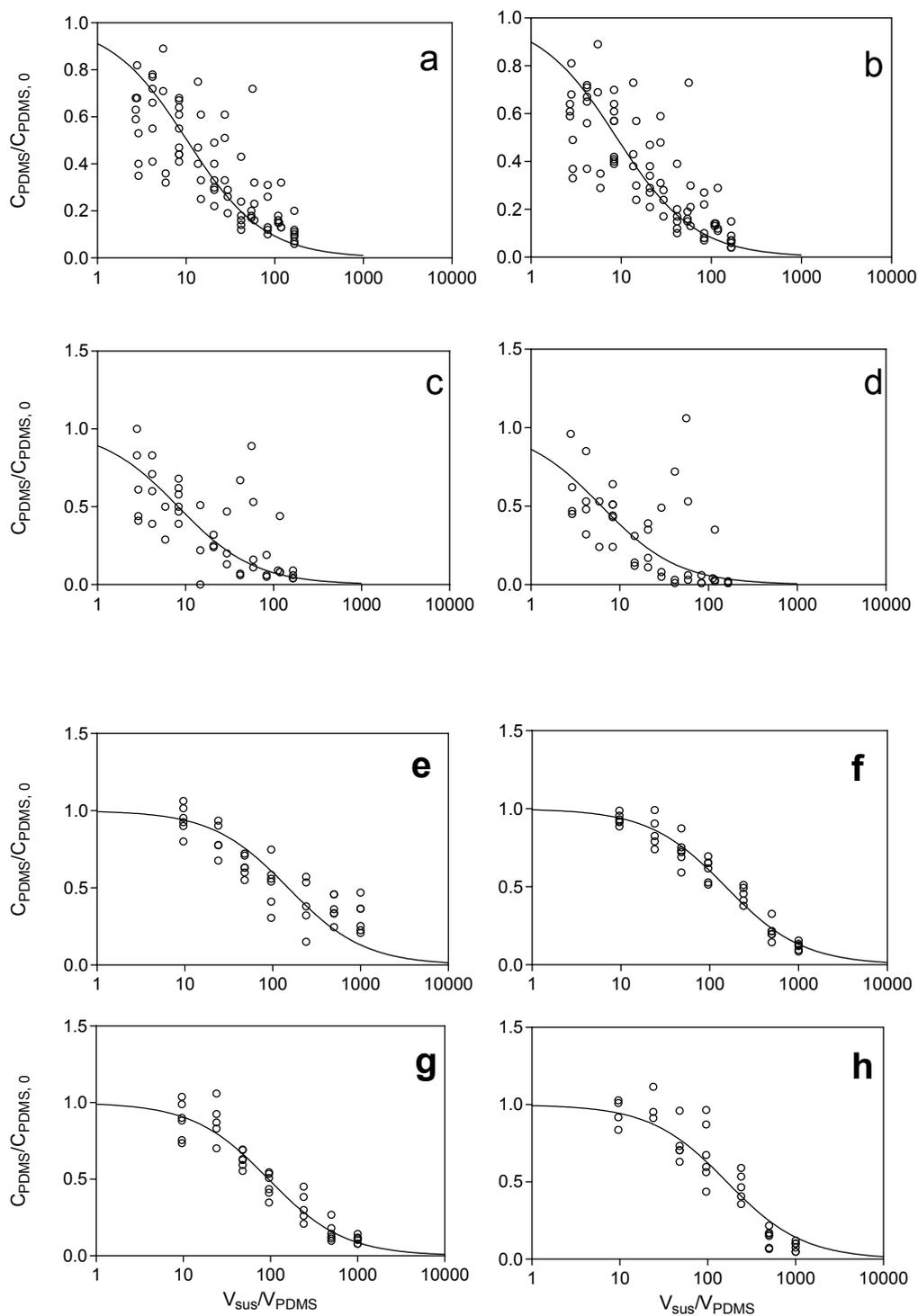


Figure S3. Determination of partition constants $K_{\text{PDMS}/\text{sus}}$ of (a) phenanthrene, (b) anthracene, (c) pyrene, and (d) benzo[*a*]pyrene between PDMS and deactivated S9 protein suspension and (e) phenanthrene, (f) anthracene, (g) pyrene, and (h) benzo[*a*]pyrene between PDMS and BSA suspension. The lines represent the best fits of the data to equation 9 (main text).

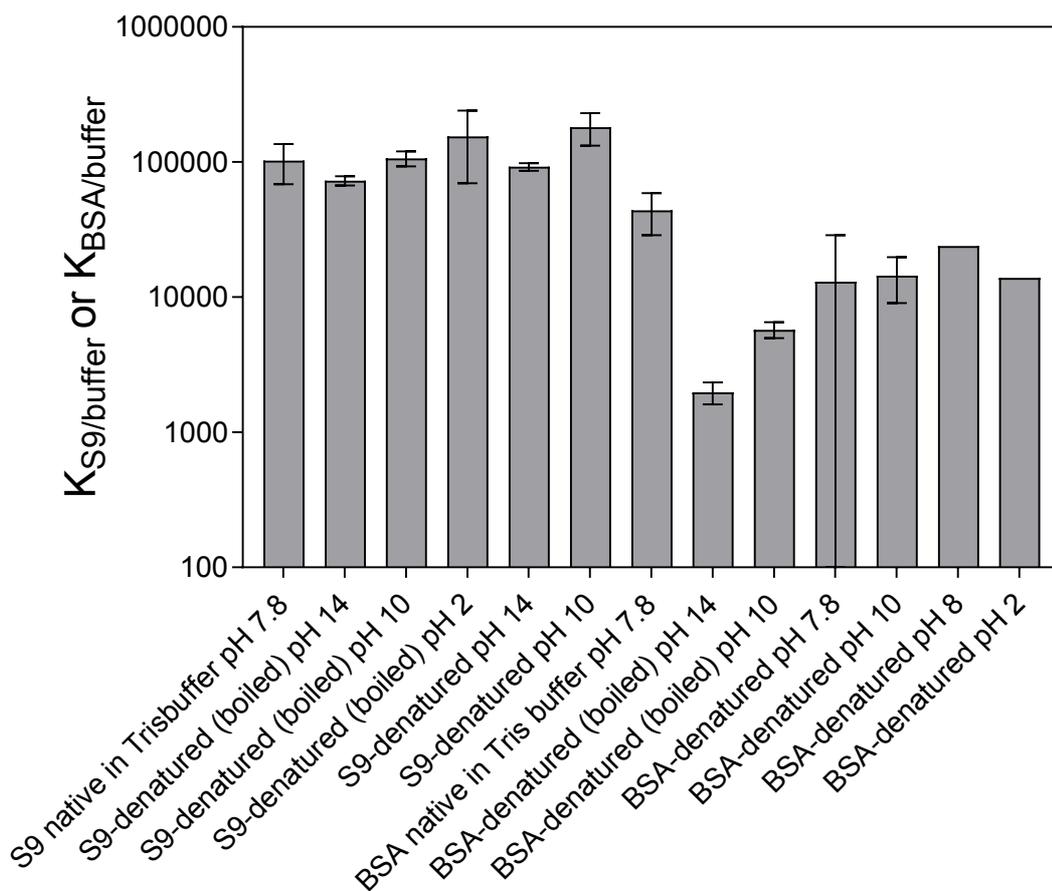


Figure S4. Determination of partition constants $K_{S9/buffer}$ or $K_{BSA/buffer}$ of hexachlorobenzene between S9 protein or BSA suspension and water, in native state or denatured with using various methods, including pH change, pH adjusted to 14 and then boiling for 5 min, and adjustment to various pH-values.

Table S1. Best-fit parameters for apparent first-order rate constants (k_{S9}) using model 2 and 3.

	phenanthrene	anthracene	pyrene	benzo[a]pyrene
Model 2				
$A \left(\frac{k_1 k_2}{k_{-1} + k_2} \right)$	0.557(± 0.047)	1.142(± 0.061)	1.182(± 0.115)	13.7(± 2.1)
r^2	0.297	0.294	0.119	0.078
Degree of freedom	28	37	21	17
Model 3				
$A \left(\frac{k_1 k_2}{k_{-1} + k_{-1}' + k_2} \right)$	0.247(± 0.044)	1.099(± 0.104)	0.621(± 0.098)	6.27(± 0.40)
$B \left(\frac{k_1'}{k_1} \right) \times 10^{-3}$	43.9(± 6.4)	0.905(± 1.814)	9.96(± 2.77)	4.30(± 0.39)
r^2	0.938	0.299	0.760	0.982
Degree of freedom	27	36	20	16