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1 **Impact of chemoeffectors on bacterial motility, transport and**  
2 **contaminant degradation in sand-filled percolation columns**

3

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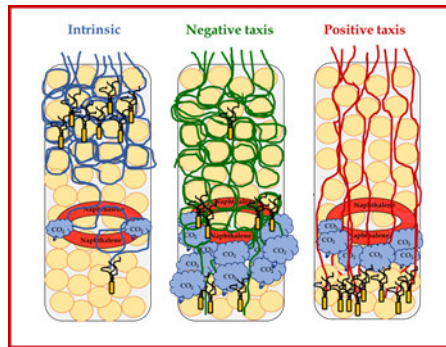
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23 **ABSTRACT:**

24 Chemoeffector-mediated bacterial motility and tactic swimming are major drivers for contaminant  
25 accessibility and biodegradation at submillimeter scales. In sand-filled percolated columns we  
26 tested how and to which degree chemoeffectors influenced bacterial transport and thereby promoted  
27 accessibility and degradation of distantly located <sup>14</sup>C-naphthalene (NAH) at the centimeter scale.  
28 Sunflower root exudates and silver nanoparticles (AgNPs) were used as chemoeffectors to stimulate  
29 opposing effects of motility and tactic swimming of NAH-degrading *Pseudomonas putida* G7.  
30 Sunflower exudates prompted smooth bacterial movement and positive taxis, while AgNPs induced  
31 tortuous movement and repellent responses. Compared to chemoeffector-free controls exudates  
32 reduced deposition and stimulated bacterial transport during percolation experiments. AgNPs,  
33 however, provoked bacterial deposition and concomitant saturation of the collector surfaces (filter  
34 blocking) that led to progressively increased percolation of cells. Despite of mechanistic  
35 differences, both motility patterns supported bacterial transport and promoted mineralization rates  
36 of NAH desorbing from a source placed at the column outlet. Observed mineralization rates in  
37 presence of the chemoeffectors were fivefold higher than in their absence and similar to NAH-  
38 mineralization in well-stirred batch assays. Our results indicate that chemically mediated, small-  
39 scale bacterial motility patterns may become relevant for long-distance bacterial transport and the  
40 biodegradation of patchy contaminants at higher scales, respectively.

## 41 INTRODUCTION

42 Despite of the high relevance of bacterial tactic swimming for the ecology of contaminant  
43 degradation at the sub-millimeter scale,<sup>1-6</sup> the impact of taxis on environmental processes and  
44 applications occurring at centimeter to decimeter scale (e.g. in bioremediation and waste-water  
45 treatments) still remains elusive. Tactic reactions of flagellated bacteria are typically reflected by  
46 distinct shifts in the motility pattern due to modifications of the rotation of their flagella. Motility  
47 patterns may influence bacterial adhesion to solid surfaces; for instance, deposition of *Escherichia*  
48 *coli*<sup>7,8</sup> and *Pseudomonas putida*<sup>9</sup> was favored by abrupt movements, whereas smoother and more-  
49 continuous swimming reduced adhesion of the same cells. By impelling bacterial deposition,  
50 motility may also impact bacterial transport through porous materials.<sup>10, 11</sup> Using NAH-degrading  
51 bacterium *Pseudomonas putida* G7 it was shown that bacterial motility and dispersal can be  
52 controlled by exposure to a suitable choice of tactic effectors. In the absence of a tactic effector, the  
53 spontaneous cell swimming strain G7 was characterized by straight or circular paths and occasional  
54 changes in the direction preventing significant long-distant transport. In the presence of chemical  
55 effectors that provoked positive tactic swimming (such as salicylate<sup>9</sup> or easily biodegradable  
56 dissolved organic matter (DOM) from sunflower root exudates)<sup>12</sup> G7 cells however showed smooth  
57 motility and poor bacterial interaction with collector surfaces. Silver nanoparticles (AgNPs) on the  
58 other hand led to induced abrupt movements, high adhesion rates, fast concomitant saturation of the  
59 collector surfaces (filter blocking) and high transport.<sup>9</sup> Although driven by different mechanisms  
60 (poor deposition rates vs. fast saturation of the collector surface) both tactic responses increased  
61 bacterial transport through porous materials.<sup>9, 12</sup> Still unknown remains how chemoeffector-  
62 mediated transport enables access of catabolically active bacteria to distant contaminant sources  
63 (e.g. soil aggregates and non-aqueous phase liquids (NAPLs)) and concomitant extents of  
64 contaminant biodegradation and mineralization.

65 Following preferential transport of a cell to the vicinity of a pollutant source<sup>13</sup>, chemotactic

66 swimming may allow substrate uptake by a cell to exceed the rate of aqueous pollutant diffusion  
67 and to enhance the rate of biodegradation and mineralization.<sup>4</sup> High contaminant-degrading  
68 biomass in close vicinity to sources of desorbing contaminants additionally promotes contaminant  
69 mass transfer to the aqueous phase by steepening pollutant concentration gradients at the interfaces  
70 as e.g. formed by non-aqueous phase liquids (NAPLs).<sup>5</sup> Once the chemoeffector-mediated transport  
71 to distant pollutant sources occurs, the simultaneous tactic reactions to various stimuli is a pre-  
72 requisite for these accessibility-promoting mechanisms, because chemotaxis to dissolved pollutants  
73 should not be overridden by the effects of the other tactic effectors present in coexisting  
74 concentration gradients. However, the positive tactic response occurring with easily biodegradable  
75 DOM, such as root exudates,<sup>12</sup> suggests that multiple tactic responses are possible.

76 In this paper, we challenged the hypothesis whether chemoeffector-mediated motility  
77 patterns of the chemotactic bacterium *P. putida* G7 lead to changed centimeter-scale transport of  
78 bacteria, and, subsequently, to enhanced accessibility and mineralization of NAH as compared to  
79 situations in the absence of an effector. For this reason, sunflower root exudates and AgNPs were  
80 selected as tactic effectors to either induce smooth or abrupt motility in sand-filled percolated  
81 columns<sup>9, 11, 12, 14</sup> and differing transport to a <sup>14</sup>C-NAH desorbing from a source at the outflow of the  
82 column. Mineralization rates of desorbed NAH in column experiments was monitored by  
83 radiorespirometric measurements and compared to <sup>14</sup>C-NAH mineralization rates in well stirred  
84 batch systems.

85

## 86 **MATERIAL AND METHODS**

### 87 **Materials**

88 Root exudates, obtained from sunflower plants propagated in vitro, were used at 16 mg L<sup>-1</sup> of total  
89 organic carbon (TOC). The procedure for obtaining the exudates and its composition is described  
90 elsewhere.<sup>12</sup> Silver nanoparticles (AgNPs), purchased from Sigma-Aldrich, Inc. (St. Louis, MO,

91 USA) were used at 0.2 mg L<sup>-1</sup>.<sup>9</sup> Fine-grained sand was obtained from Panreac Quimica SA  
92 (Barcelona, Spain) and sieved to give a fraction between 0.40 mm and 0.25 mm diameter. Silicone  
93 rings (O-rings) were obtained from Altec Products Ltd. (Cornwall, UK) with an inner diameter of  
94 2.57 mm and a cross section of 1.78 mm. Unlabeled NAH and <sup>14</sup>C-UL-NAH (31.3 mCi mmol<sup>-1</sup>;  
95 radiochemical purity >98%) were purchased from Sigma Chemical Co., Steinheim, Germany.

#### 96 **Cultivation of bacteria**

97 NAH-degrading soil bacterium *Pseudomonas putida* G7 was cultivated and prepared as described  
98 elsewhere.<sup>9</sup> Strain G7 is motile by means of polar flagella and exhibits positive taxis towards NAH  
99 and sunflower root exudates, and negative taxis towards silver nanoparticles.<sup>9,12</sup> In all experiments,  
100 strain G7 was grown in an inorganic salts solution (MM) using sodium salicylate (5 mM) as carbon  
101 source.<sup>9</sup> Liquid cultures were performed in 250 mL-Erlenmeyer flasks containing 100 mL of MM  
102 with sodium salicylate. Bacterial cultures were maintained under continuous agitation (150 rpm) at  
103 30 °C. At early stationary phase (48 hours after inoculation of the culture; OD<sub>600nm</sub> of 0.5 (5 x10<sup>8</sup>  
104 cells mL<sup>-1</sup>), cells were centrifuged for 10 minutes at 1000 g and re-suspended in mineral medium  
105 (MM) supplemented with or without tactic effectors. The centrifuge speed was selected to avoid  
106 breakage of flagella and thus loss of motility. The microbial biomass was estimated by the  
107 quantification of the total protein by the Lowry method.<sup>15</sup>

#### 108 **Dynamic doping of <sup>14</sup>C-NAH containing materials**

109 The dynamic doping method was used to load the O-rings with <sup>14</sup>C-NAH.<sup>16</sup> A maximum of 8 rings  
110 were placed on the bottom of a 20 mL-glass tube and 1 mL of an acetone solution of <sup>14</sup>C-NAH and  
111 sufficient unlabeled NAH to give a concentration of 50 mg L<sup>-1</sup> was added. The solution contained  
112 the required radioactivity to make each ring to be loaded with approximately 200,000 dpm. The  
113 tube was left opened overnight in a fume-hood to allow the complete evaporation of the acetone. To  
114 help the homogenous incorporation of NAH into the silicone, drops of milli-Q water were then  
115 applied.<sup>16</sup> Due to the moderate volatility of NAH that eventually led to losses of the compound

116 during loading the amount of NAH present in the loaded rings was determined separately. For this  
117 aim, two loaded rings were separately placed in a glass vial and 1 mL of methanol was added. After  
118 72 hours of extraction,  $^{14}\text{C}$ -NAH present in the methanol extracts was measured by liquid  
119 scintillation. The total amount of NAH initially present in each ring was 6.25  $\mu\text{g}$  for column  
120 experiments with control cells and AgNPs and 8.30  $\mu\text{g}$  for experiments with exudates.

## 121 **Batch adhesion and mineralization experiments**

### 122 *Adhesion experiments*

123 Adhesion experiments were performed in duplicate with sand or O-rings to check the bacterial  
124 affinity to these materials used in a non-flowing system. In brief, 20 mL glass vials containing 1.5 g  
125 of sand or 23 rings (which corresponded to 1.5 g of material) and 1 mL of the test cell suspension  
126 ( $\text{OD}_{600\text{nm}}$  of  $\sim 0.3$ ,  $10^8$  cells  $\text{mL}^{-1}$ ) were maintained in an orbital shaker at 80 rpm at room  
127 temperature. Attachment was determined as a percentage of the initial OD in the cell suspension  
128 after 30 min of incubation. Significant differences between treatments were analyzed using ANOVA  
129 test, Tukey HSD,  $P \leq 0.05$ , using SPSS 11.5 (SPSS, Chicago, IL, USA).

### 130 *Mineralization experiments*

131 Batch mineralization experiments were performed in 10-mL test tubes with 5 mL of a bacterial  
132 suspension in MM with the dissolved chemical effectors. Approximately 20,000 dpm of labeled  
133 NAH and unlabeled NAH to give a final concentration of 10  $\mu\text{g mL}^{-1}$  was completely dissolved in  
134 the bacterial suspension ( $\text{OD}_{600\text{nm}}$  of  $\sim 0.3$ ,  $10^8$  cells  $\text{mL}^{-1}$ ). The aqueous solubility of NAH is 30  $\mu\text{g}$   
135  $\text{mL}^{-1}$ .<sup>11</sup> The test tubes were closed with Teflon-lined stoppers equipped with a suspended 2-mL vial  
136 that contained 1 mL of 0.5 M NaOH and were maintained at  $23 \pm 2$  °C on an orbital shaker  
137 operating at 150 rpm. Then,  $^{14}\text{C}$ -NAH mineralization was measured as radioactivity incorporated in  
138 the alkali trap. The sample (1 mL) was collected from the trap and mixed with 5 mL of scintillation  
139 fluid (Ready Safe, Beckman Instruments, Fullerton, California, USA). Radioactivity was measured  
140 on a liquid scintillation counter model LS6500 Beckman (Beckman Instruments, Fullerton,



141 California, USA). The maximum rates ( $V_s$ , in  $\text{ng } \mu\text{g}_{\text{prot}}^{-1} \text{ min}^{-1}$ ) and extents ( $E_{\text{min}}$ , %) of  $^{14}\text{CO}_2$   
142 production were calculated as described earlier.<sup>11</sup>

### 143 *Column transport and mineralization experiments*

144 Bacterial transport and NAH mineralization was tested simultaneously in duplicate at 25°C in  
145 vertical (10 cm length and 0.9 cm inner diameter) percolated sand columns with an porosity  
146 (estimated gravimetrically) of 0.34, corresponding to a pore volume (PV) of 2.3 mL.<sup>9, 12</sup> Silicone  
147 rings (O-rings), containing sorbed  $^{14}\text{C}$ -NAH (cf. above), were placed two centimeters from the  
148 outlet of the columns to simulate a distant NAH source (cf. Figure S1). Each ring was collected  
149 with forceps and washed separately in milli-Q water before being introduced (once dried with  
150 blotting paper) to the column. Bacterial suspensions ( $\text{OD}_{600\text{nm}} = 0.3$ , i.e. ca.  $10^8$  cells  $\text{mL}^{-1}$ ) were  
151 pumped through the columns at a constant flow rate of  $0.135 \pm 0.02$   $\text{mL min}^{-1}$  (hydraulic flow rate  
152  $0.50$   $\text{cm min}^{-1}$ ). The column effluent was collected every 20 minutes into 20 mL test tubes in order  
153 to photometrically measure cell concentrations. The total radioactivity and  $^{14}\text{CO}_2$  produced was also  
154 measured by liquid scintillation counting as detailed below. The column breakthrough of the  
155 bacteria was followed by comparing the  $\text{OD}_{600\text{nm}}$  of the influent ( $C_0$ ) and effluent ( $C$ ) at given time  
156 intervals. The breakthrough curves also allowed us to calculate the percolated biomass ( $X_{\text{sus}}$ ) and the  
157 total attached biomass ( $X_{\text{att}}$ ) in the columns at given time points. These values were inferred by  
158 difference from the input and output OD measurements. Control determinations excluded any  
159 interference on OD measurements by the chemoeffector solutions used. Based on the data of the  
160 breakthrough curves the clean-bed adhesion efficiency ( $\alpha_o$ ) and the blocking factor ( $B_f$ ) was  
161 determined as previously described.<sup>9</sup> Shortly,  $\alpha_o$  is defined as the ratio of the rate of bacterial  
162 attachment to the rate of bacterial transport to the collector surfaces, whereas  $B_f$  is defined as the  
163 ratio of the area of the collector blocked by a deposited particle to the area of that particle. A more  
164 detailed description of the theoretical background and calculation method for  $\alpha_o$  and  $B_f$  can be found  
165 elsewhere.<sup>9, 11</sup>

166 An aliquot of the column effluent (0.5 mL) was used to measure total radioactivity by liquid  
 167 scintillation. This measurement was carried out to determine the total concentration of NAH  
 168 leached from the columns ( $C_{tot,n}$ ). To the remaining volume, 1 mL of 2N HCl was added in order to  
 169 inactivate the bacterial cells and the mixture stirred at 80 rpm for 12 hours to remove and  
 170 incorporate  $^{14}\text{CO}_2$  present in the effluent fractions in an alkali trap (cf. Figure S1). Radioactivity  
 171 incorporated into the trap was measured by liquid scintillation. Specific mineralization rates  $V_s$  (ng  
 172  $\mu\text{g}_{\text{prot}}^{-1} \text{min}^{-1}$ ) were calculated as described in a previous study: <sup>14</sup>

$$173 \quad V_s = \frac{C_{CO_2,n} V_{\text{sample}}}{X_{\text{sus}} t_{\text{res}} + X_{\text{att}} t_{\text{sample}}} \quad (1)$$

174 where  $C_{CO_2,n}$  is the concentration of mineralized NAH in the effluent ( $\text{ng mL}^{-1}$ ),  $V_{\text{sample}}$  is the sample  
 175 volume (mL),  $X_{\text{sus}}$  is the biomass of suspended bacteria transported with the sample volume ( $\mu\text{g}$   
 176 prot),  $t_{\text{res}}$  is the residence time in the column portion below the ring or exposure zone (min),  $X_{\text{att}}$  is  
 177 the biomass attached to the column matrix ( $\mu\text{g prot}$ ), and  $t_{\text{sample}}$  is the sampling interval (min). Due  
 178 to operational limitations, some samples for  $C_{CO_2,n}$  measurements were not accompanied by  
 179 simultaneous OD determinations. In those cases,  $X_{\text{sus}}$  and  $X_{\text{att}}$  were calculated from the slope of OD  
 180 measurements immediately before and after the corresponding  $C_{CO_2,n}$  sampling point. Equation 1  
 181 accounts for the fact that suspended cells can mineralize NAH only during their passage through the  
 182 column portion exposed to NAH (i.e., desorbed from the ring), the duration of which is  $t_{\text{res}}$ . Time-  
 183 dependent mineralization extents  $E_{\text{min}}$  (%) were further calculated, by dividing the amount of NAH  
 184 appearing in the effluent as  $\text{CO}_2$  by the accumulative amount of total NAH ( $C_{\text{tot}}$ ) leached from the  
 185 columns up to that sampling point:

$$186 \quad E_{\text{min}} = \frac{\sum C_{CO_2,n} V_{\text{sample}}}{\sum C_{\text{tot}} V_{\text{sample}}} \times 100 \quad (2)$$

187 To have comparable values, the extents of mineralization were calculated in the different column  
 188 experiments at the point when 1  $\mu\text{g}$  of NAH had been leached from the columns (approximately at 8

189 PV). It should be noted that  $C_{tot}$  in eq. 2 differs from  $C_{tot,n}$ , which denotes the concentration of total  
190 NAH measured in each effluent sample.

191

## 192 **RESULTS**

### 193 **Effect of motility patterns on bacterial adhesion and NAH mineralization in batch** 194 **experiments**

#### 195 *Bacterial motility patterns and adhesion*

196 Batch experiments were used to study the effects of chemoeffector-induced motility patterns on  
197 adhesion to sand and silicone O-rings, and to quantify resulting effects on mineralization of NAH in  
198 well stirred system, respectively. Motility patterns were described by the number of peaks in the  
199 rate of changes in the direction higher than  $1000\text{ }^\circ\text{s}^{-1}$  (RCDI; Table 1 and Figure S2). These  
200 distinctive patterns are stable upon exposure to the chemical effectors at least during 30 min.<sup>9, 12</sup>  
201 Abrupt movement, with a high number of turning events, was acquired by cells in reaction to  
202 repellent AgNPs. This caused higher adhesion to sand (58 %) relative to control cells (38 %) in the  
203 absence of a chemoeffector (Table 1). By contrast, smooth motility (as characterized by a low  
204 number of turning events) was found in response to sunflower exudates. These exudates provoked  
205 positive taxis in strain *P. putida* G7 and reduced its adhesion to sand surfaces (9 %, Table 1) relative  
206 to the control. Likewise, bacterial adhesion to NAH-free silicone O-rings was significantly different  
207 ( $P \leq 0.05$ ) in the presence of AgNPs and exudates, as compared to the control, following the same  
208 trend as with sand.

#### 209 *NAH mineralization*

210 Batch mineralization experiments with completely dissolved NAH demonstrated the ability of  
211 strain *P. putida* G7 to mineralize NAH in the presence of chemoeffectors. The specific  
212 mineralization rates and final extents in presence of chemoeffectors however were not statistically  
213 different ( $t$ -test,  $P = 0.05$ ) to chemoeffector-free controls (Table 1). The final extents of

214 mineralization measured ( $\approx 40\%$ ) were within the expected values, whereas the rest of the substrate  
215 was probably incorporated into microbial biomass or transformed to partially oxidized byproducts.<sup>17</sup>  
216

## 217 **Effect of motility patterns on bacterial transport and NAH mineralization in percolation** 218 **column experiments**

### 219 *Bacterial transport*

220 Single cell motility effects on macroscale bacterial transport and contaminant mineralization was  
221 studied in sand-filled laboratory percolation columns in presence and absence of chemoeffectors.  
222 Control cells in the absence of a chemoeffector exhibited an initial adhesion efficiency ( $\alpha_0$ ) of  
223  $\approx 0.38$ , and reached final  $C/C_0$  values of  $\approx 0.4$  after 5 PV (Table 1, Figure 1A). The calculated filter  
224 blocking factor was  $B_f = 0.3$ . The presence of AgNPs however led to high initial adhesion efficiency  
225 ( $\alpha_0 \approx 0.6$ ) yet a sharp increase of  $C/C_0$  values after two PV (Figure 1C) likely due to progressive  
226 saturation of the collector surfaces (filter blocking;  $B_f = 0.7$ ) and subsequent improved transport.<sup>9</sup>  
227 Low adhesion efficiencies ( $\alpha_0 \approx 0.18$ ), high bacterial transport were observed in presence of  
228 sunflower root exudates (Figure 1E, Table 1): Suspensions of exudate-exposed cells broke through  
229 at  $C/C_0 \approx 0.5$  at 1 PV, and rapidly reached  $C/C_0$  values of 0.9 at two PV likely due to the smooth  
230 cellular motility pattern of G7 cells in presence of the exudates at the low TOC used ( $16 \text{ mg L}^{-1}$ ),  
231 which is significantly lower than the TOC levels (above  $100 \text{ mg L}^{-1}$ ) at which DOM enhances  
232 bacterial transport through competition effects with collector surfaces.<sup>12</sup> This was reflected by a  
233 high estimated  $B_f$  of 1.2.

### 234 *NAH mineralization*

235 The mineralization of NAH was assessed by quantifying the concentrations of total  $^{14}\text{C}$ -NAH ( $C_{tot,n}$ )  
236 and the  $^{14}\text{CO}_2$  concentrations in the effluent ( $C_{\text{CO}_2,n}$ ) in the effluent. Quasi steady-state effluent  
237 concentrations of total  $^{14}\text{C}$ -NAH in chemoeffector-free columns were  $\approx 45 \text{ ng mL}^{-1}$  and, hence,  
238 significantly lower than the initial concentration ( $10 \text{ } \mu\text{g mL}^{-1}$ ) tested in batch mineralization

239 experiments in order to determine the maximum mineralization potential. The  $^{14}\text{CO}_2$  concentrations  
240 in the effluent ( $C_{\text{CO}_2,\text{n}}$ ) (expressed as ng NAH  $\text{mL}^{-1}$  mineralized, cf. Materials and Methods section)  
241 increased linearly up to 8 PV reflecting increasing access of percolated bacteria to the NAH source  
242 (Figure 1A). In presence of exudates (Figure 1C) similar  $C_{\text{tot}}$  ( $\approx 45 \text{ ng mL}^{-1}$ ) as the control and  
243 AgNPs-exposed columns were observed after approximately 4 PV despite of somewhat higher  
244 initial  $^{14}\text{C}$ -NAH values ( $\approx 60 \text{ ng mL}^{-1}$ ). Unexpectedly however,  $C_{\text{CO}_2,\text{n}}$  was significantly higher in  
245 presence of the AgNPs and, to a lesser extent, sunflower exudates than control cells, in spite of  
246 similar steady-state concentrations of total  $^{14}\text{C}$ -NAH (Figure 1A).

247       Whereas the  $C_{\text{CO}_2,\text{n}}$  values reflect the overall biodegradation process in the column, a further  
248 analysis of the results was performed by combining effluent data from  $C_{\text{tot}}$ ,  $C_{\text{CO}_2,\text{n}}$  and estimations of  
249 suspended ( $X_{\text{sus}}$ ) and attached ( $X_{\text{att}}$ ) bacterial biomass to approximate the specific mineralization rate  
250 ( $V_s$ ) and mineralization extent ( $E_{\text{min}}$ ; cf. eqs. 1 & 2). The results are shown in Figures 1B, 1D, and 1F,  
251 and in Table 1. In control experiments  $X_{\text{att}}$  increased linearly and was higher than the suspended  
252 biomass ( $X_{\text{sus}}$ ; Figure 1B) as evidenced by low  $X_{\text{sus}}/X_{\text{att}}$  ratios of  $\approx 0.1$ - $0.3$ . Corresponding values of  
253  $V_s$  remained constant ( $V_s \approx 0.004 \text{ ng mg}_{\text{prot}}^{-1} \text{ min}^{-1}$ ) and hence were about fivefold lower than  $V_s$  of  
254 batch ( $\approx 0.02 \text{ ng mg}_{\text{prot}}^{-1} \text{ min}^{-1}$ ) mineralization experiments (Table 1). As  $X_{\text{att}}$  reflects the total biomass  
255 in the columns (i.e. does not discriminate attached cells placed outside from cells inside the  
256 exposure zone) calculated values of  $V_s$  underestimate the activity of cells exposed to NAH. Final  
257 extents of NAH mineralization in column experiments ( $\approx 41 \%$ ) however were comparable to  $E_{\text{min}}$  of  
258 batch experiments ( $\approx 44 \%$ ). Cells exposed to AgNPs provoked a significantly higher NAH  
259 mineralization rate ( $V_s = 0.017 \text{ ng } \mu\text{g}_{\text{prot}}^{-1} \text{ min}^{-1}$ ) than was observed for control cells ( $V_s = 0.004 \text{ ng}$   
260  $\mu\text{g}_{\text{prot}}^{-1} \text{ min}^{-1}$ ); a value that was similar to  $V_s$  of NAH mineralization of dissolved NAH by suspended  
261 cells in well-stirred batch experiments (Table 1). At 8.5 PV however,  $V_s$  decreased to  $0.005 \text{ ng}$   
262  $\mu\text{g}_{\text{prot}}^{-1} \text{ min}^{-1}$  and was similar to  $V_s$  of control cells. Such decrease went along with a drop of the  
263 initial  $X_{\text{sus}}/X_{\text{att}}$  ratio of  $\approx 1.3$  to  $\approx 0.3$  (Table 1). At 8.5 PV the mineralization extent was 79 % and

264 exceeded batch mineralization extents of 34 % in presence of AgNPs. The presence of sunflower  
265 exudates provoked highest  $X_{\text{sus}}/X_{\text{att}}$  ratios that dropped 6.5 (at 2.6 PV) to 1.3 (at 6.7 PV). Similar to  
266 the  $X_{\text{sus}}/X_{\text{att}}$  ratio the  $V_s$  decreased from 0.020 to 0.006 ng  $\mu\text{g}_{\text{prot}}^{-1} \text{min}^{-1}$ . The presence of the exudates  
267 however, did not impact mineralization extents, which were similar to  $E_{\text{min}}$  of batch experiments  
268 ( $\approx 42\%$ ).

269

## 270 **DISCUSSION**

### 271 **Effect of chemoeffectors on bacterial motility, transport and NAH mineralization**

272 In this study we analyzed the effect of chemoeffector-induced motility patterns on bacterial  
273 transport and the accessibility and degradation of NAH in a spatially separated source. Towards this  
274 question we compared deposition and mineralization results in batch and column assays with *P.*  
275 *putida* G7 cells that were induced to exhibit three distinct motility patterns: intrinsic (= control  
276 cells), negative taxis, and positive taxis. The mechanistic basis for the enhancement of bacterial  
277 transport through porous materials caused by taxis-mediated swimming modes has been described  
278 elsewhere.<sup>9, 11, 12</sup> These studies revealed that chemoeffectors enhanced long-range transport by  
279 changes in the motility pattern of individual cells at a pore-scale rather than modifying properties of  
280 the grain surfaces or the solution, respectively. Our results extend those findings by highlighting  
281 two factors influencing the bioaccessibility of NAH in percolation columns: i) transport efficiency  
282 of bacteria towards the exposure zone and ii) deposition efficiency of bacteria at the exposure zone.  
283 Both factors were responsible, respectively, for the observed enhancements in the specific rates and  
284 extents of NAH mineralization.

285 Independent of their tactic effects, chemoeffectors led to about fivefold enhanced initial  $V_s$   
286 relative to controls and were similar to  $V_s$  of NAH degradation under well-stirred batch conditions.  
287 This observation proposes that taxis-mediated motility facilitates the access of bacteria to a spatially  
288 separated NAH source despite of opposite chemoeffector effects on cellular swimming. As  $C_{\text{tot},n}$  of

289 NAH (45-60 ng mL<sup>-1</sup>) in column effluents was smaller than the concentration in batch experiments,  
290 significantly smaller  $V_s$  in column experiments would be expected, given an affinity constant (or  
291  $K_m$ ) of NAH degradation by strain *P. putida* G7 of 130 ng mL<sup>-1</sup>.<sup>4</sup> This reveals that our observations  
292 of emerging, apparent effluent concentrations may not entirely reflect cellular exposure to  
293 microscale NAH gradients forming in close vicinity to the NAH containing O-rings. Cellular  
294 proximity to the NAH source allows for high NAH mass transfer, high NAH concentrations and  
295 similar degradation activity of the *P. putida* G7 cells<sup>14, 17, 21</sup> as in well-stirred batch assays. Such  
296 proximity can be promoted by chemoeffector-mediated facilitated transport of bacteria to the  
297 NAH source and, eventually, by coinciding chemotactic movement along NAH gradients.<sup>20</sup>  
298 Changing the relative presence of bacterial biomass in the NAH exposure zone thereby can explain  
299 continuously decreasing  $V_s$  values observed in column experiments, as  $V_s$  depends on the biomass  
300 ( $X_{\text{sus}}$  and  $X_{\text{att}}$ ) and bacterial residence time ( $t_{\text{res}}$ ): Given quasi similar or even increased  $C_{\text{CO}_2, \text{n}}$  at  
301 higher PV, decreasing  $V_s$  values are the result of higher attached biomass above the NAH exposure  
302 zone (eq.1). Sunflower exudates e.g. allowed mobilizing bacteria by inducing smooth motility,  
303 efficient transport to and enhanced accumulation of percolated cells in the NAH exposure zone.  
304 AgNP-induced negative taxis motility, by contrast, promoted both high bacterial transport to and  
305 efficient deposition in the contaminant zone.

306 Increased  $V_s$  in presence of exudates may also be due to facilitated NAH desorption induced  
307 by this natural dissolved organic matter.<sup>18</sup> However, this process is unlikely to occur: Given 16 mg  
308 L<sup>-1</sup> of the exudates, a log  $K_{oc}$  of NAH of 2.98<sup>19</sup> and instantaneous equilibrium apparent NAH  
309 aqueous concentration would increase by  $\approx 2\%$  only and hence be negligible. Likewise poor impact  
310 of sorption of NAH to AgNPs is to be expected, given the low concentration and organic carbon  
311 content of AgNPs.<sup>9</sup>

### 312 **Effect of AgNPs on NAH mineralization**

313 The unexpectedly high mineralization extent (79 % of the leached compound, Table 1) seems rather

314 to be result of the effects induced by AgNPs promoting negative taxis by *P. putida* G7 cells.  
315 Although we did not measure directly the deposition of bacteria in the exposure zone, we suggest,  
316 as a plausible explanation, that the spatial confinement due to increased deposition of the cells in  
317 this zone contributed to this highest NAH mineralization extent. This enhancement of pollutant  
318 biodegradation as a result of an enhanced bioavailability constitutes, therefore, a new endpoint for  
319 the interactions of *P. putida* G7 cells with AgNPs at low, sub-toxic concentrations, to be added to  
320 the repellence due to nanoparticle-specific physical effects, independent of the release of silver  
321 ions,<sup>22, 23</sup> and to an enhanced transport through porous materials due to collector saturation.<sup>9</sup> Indeed,  
322 attachment to surfaces has been discussed as bioavailability promoting effect due to steeper  
323 contaminant concentration gradients and higher mass transfer rates of desorbing contaminants to the  
324 cells.<sup>14, 17, 21</sup> Such enhanced desorption may explain the high observed mineralization extents that  
325 were higher than mineralization typically observed in other experimental situations,<sup>24</sup> including the  
326 batch assays ( $\approx 40\%$ ) described in this study. Attached bacteria actively assimilating NAH also  
327 produced  $^{14}\text{CO}_2$ , but remained in the column with biochemically incorporated  $^{14}\text{C}$ , thus resulting in a  
328 higher fraction of mineralized NAH in the column effluents. Assuming a mineralization efficiency  
329 of  $\approx 40\%$  (in accordance with batch mineralization assays), the mineralization extent in column  
330 experiments indicates that attached bacteria were responsible for a two-fold increase of NAH  
331 transformation. Alternately, bacteria sitting on the O-rings and sand grains may also have changed  
332 their mineralization efficiency, as a part of up to date unknown physiological modifications  
333 occurring in bacterial cells upon adhesion. However, the initial  $V_s$  value detected, which is the same  
334 as that of suspended cells operating in batch experiments at their maximum potential, indicated that  
335 this explanation is unlikely.

### 336 **Relevance of single cell phenomena for macroscale natural attenuation processes**

337 Our results underpin the role of cellular bacterial motility patterns (e.g. in response to chemical  
338 effectors) for natural and technically-enhanced contaminant attenuation processes: smooth motility



339 without changes in the direction hence would promote suspended bacterial cells to be mobilized  
340 towards the contamination source, while abrupt motility (as characterized by a high frequency in  
341 turning events) would additionally lead to bacterial retention at the vicinity of the contaminant. In  
342 the absence of an external modulator the spontaneous motility, (as characterized by occasional  
343 changes in the direction) would make it for the bacteria more difficult to access the pollutant due to  
344 a limited dispersal. This knowledge has several potential applications. The treatment of extended  
345 areas of contamination and pollutants present at a certain depth can benefit from the use of positive  
346 tactic effectors that increase the mobilization of bacterial cells towards the contamination source.  
347 Such effectors could be present, for example in certain DOC sources enriched with  
348 chemoeffectors,<sup>12</sup> able to promote bacterial transport at very low OC concentrations, what would  
349 not represent a risk for pollutant mobilization due to sorption to dissolved macromolecules and/or  
350 bacterial inoculants. For localized treatments in bioreactors, negative chemoeffectors would be  
351 useful in rapidly confining motile bacteria, by promoting the bacterial adhesion and retention in the  
352 contaminated matrices. In this study, we used AgNPs as a model repellent but other chemicals  
353 causing this tactic behavior, such as zero-valent iron nanoparticles,<sup>25</sup> could also be tested for  
354 environmental applications. Our results could be also applied in waste-water bio-treatment in fixed-  
355 bed reactors where biofilm establishment and maintenance is fundamental in the bioreactor  
356 performance. This research work could be the initial point of a research conducted to generate  
357 biotechnologically new chemoeffectors and to use mutant strains that exhibit continuous smooth-  
358 swimming or continuous tumbling even in the absence of any chemoeffectors that could promote  
359 the specific and directed mineralization of the contaminants.

360

## 361 **ASSOCIATED CONTENT**

### 362 **Supporting Information**

363 Figures showing the experimental setting of the column system to test the bacterial mobilization,

364 and cell-track computer analysis of *Pseudomonas putida* G7 motility patterns in response towards  
365 chemoeffectors. This material is available free of charge via the Internet at <http://pubs.acs.org>.

366

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377

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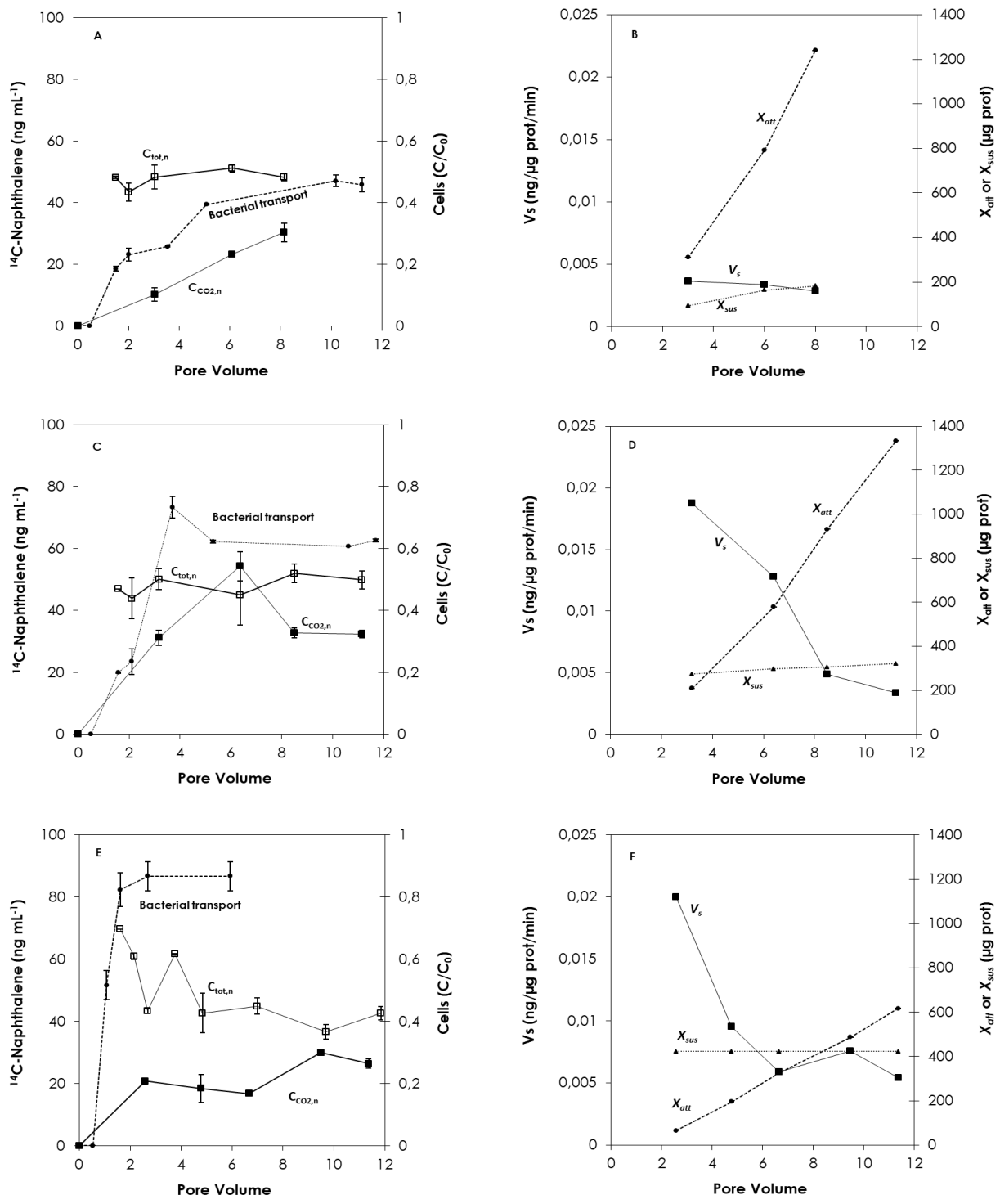
448 **Figure legend**

449

450 **FIGURE 1.** A, C and E: Experimental results on NAH mineralization and transport of  
451 *Pseudomonas putida* G7 cells in percolated sand columns. The columns received a suspension of  
452 cells exhibiting intrinsic motility (1A), a negative tactic motility pattern in the presence of silver  
453 nanoparticles at 0.2 mg L<sup>-1</sup> (1B), and a positive tactic motility pattern in the presence of sunflower  
454 root exudates at 16 mg L<sup>-1</sup> of organic carbon (1C). The symbols represent the normalized outflow  
455 concentration of cells (●), total <sup>14</sup>C expressed as NAH equivalents  $C_{\text{tot,n}}$  (□) and NAH equivalents  
456 converted into CO<sub>2</sub>,  $C_{\text{CO}_2,\text{n}}$  (■) in the column effluent. Data are presented as means of determinations  
457 in duplicate columns. Error bars represent one standard deviation. B, D and F: Specific rates of  
458 NAH mineralization at given pore volumes ( $V_s$ , ■) and biomass of suspended ( $X_{\text{sus}}$ , ▲) and sand-  
459 attached bacteria ( $X_{\text{att}}$ , ●), calculated from the experimental results shown in the respective panels to  
460 the right. Data are presented as means of calculated values in duplicate columns.

461  
462  
463  
464

FIGURE 1



465

**TABLE 1. Influence of motility patterns of *Pseudomonas putida* G7 cells on deposition, transport and naphthalene mineralization in batch experiments or during transport in saturated sand-filled columns.**

468

Motility (Treatment)	Batch Experiments				Column Experiments						
	Turning events <sup>a,b,c</sup>	Adhesion <sup>d</sup> (%)		Naphthalene Mineralization <sup>b</sup>		Naphthalene Mineralization <sup>b</sup>			Deposition and transport <sup>e</sup>		
		Sand <sup>e</sup>	Silicone	$V_s^c$ (ng $\mu\text{g}^{-1}\text{min}^{-1}$ )	$E_{\text{min}}^f$ (%)	$V_s^g$ (ng $\mu\text{g}^{-1}\text{min}^{-1}$ )	$E_{\text{min}}^h$ (%)	$X_{\text{sys}}/X_{\text{att}}^i$	PV <sup>j</sup>	$\alpha_0^k$	$B_f^l$
Control (intrinsic)	51 ± 1	38 ± 2	46 <sup>m</sup>	0.025 ± 0.003	44 ± 4	0.004 <sup>m</sup>	21 ± 10	0.30	3.0	0.38	0.33
Negative taxis (AgNPs)	114 ± 3	58 ± 4	55 ± 2	0.017 ± 0.005	34 ± 5	0.017 ± 0.001	56 ± 18	1.31	3.2	0.60	0.70
Positive taxis (Root exudates)	13 <sup>m</sup>	9 ± 1	31 ± 2	0.022 ± 0.003	42 ± 4	0.020 ± 0.005	33 ± 4	6.50	2.6	0.18	1.20
						0.006 ± 0.001	35 ± 7	1.30	6.7		

469

470 Total number of turning events (rate of change of direction greater than 1,000 s<sup>-1</sup>); <sup>b</sup> Values are reported as mean ± one standard deviation; <sup>c</sup> Data from previous  
471 publications; <sup>d</sup> Percentage of cells adhered to sand or silicone pieces in batch experiments; <sup>e</sup>  $V_s$ , specific mineralization rate; <sup>f</sup> Mineralization extent; <sup>g</sup>  $V_s$  value in  
472 column experiments at PV as defined in the column 'PV'; <sup>h</sup> Percentage of leached naphthalene mineralized at PV defined in the column 'PV'; <sup>i</sup>  $X_{\text{sys}}/X_{\text{att}}$  biomass ratio of  
473 suspended to attached bacteria at PV as defined in the column 'PV'; <sup>j</sup> PV, pore volume; <sup>k</sup> adhesion efficiency; <sup>l</sup> Blocking factor. <sup>m</sup> Standard Deviation <0.1%;

23

23