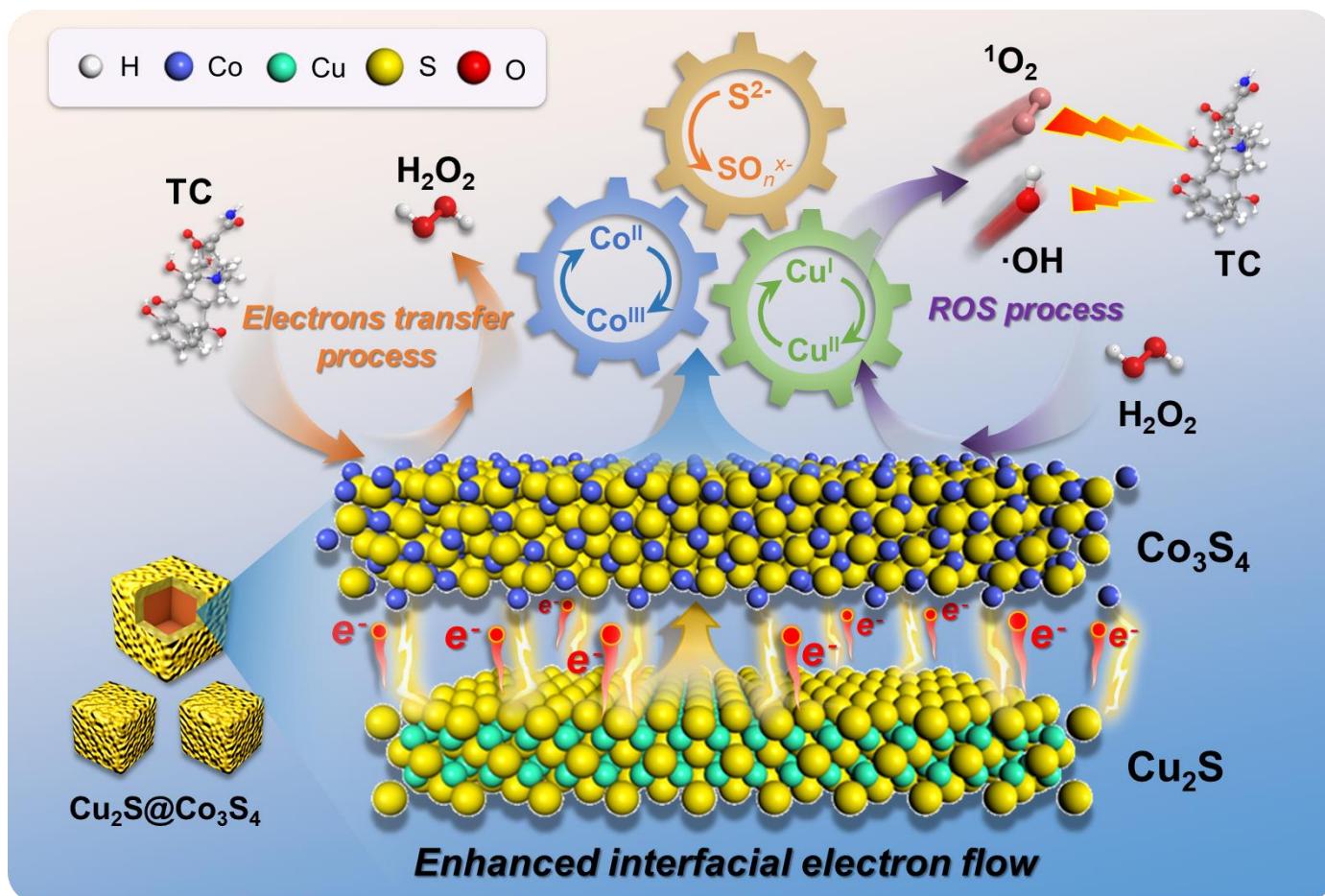


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2 **Regulating interfacial electron flow in Cu<sub>2</sub>S@Co<sub>3</sub>S<sub>4</sub> Core–Shell**  
3 **heterostructures promoting H<sub>2</sub>O<sub>2</sub> activation for singlet oxygen**  
4 **generation to efficiently degrade tetracycline**

5

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18

## Abstract

19

20 The widespread use and improper discharge of tetracycline (TC) pose significant  
21 threats to environmental safety and human health, necessitating the development of  
22 efficient removal technologies. Herein, a core-shell heterostructure,  $\text{Cu}_2\text{S}@ \text{Co}_3\text{S}_4$ , was  
23 successfully synthesized via a hydrothermal method for activating  $\text{H}_2\text{O}_2$  to degrade TC.  
24 Comprehensive characterization confirmed the well-defined cubic morphology and  
25 intimate interfacial contact between the  $\text{Cu}_2\text{S}$  core and  $\text{Co}_3\text{S}_4$  shell. The optimized  
26  $\text{Cu}_2\text{S}@ \text{Co}_3\text{S}_4$  demonstrated outstanding catalytic performance, remarkably removing  
27 over 97% of TC within 30 min and achieving a rate constant of  $0.11 \text{ min}^{-1}$ . This surpassed  
28 pure  $\text{Co}_3\text{S}_4$  ( $0.004 \text{ min}^{-1}$ ) and  $\text{Cu}_2\text{S}$  ( $0.030 \text{ min}^{-1}$ ) by factors of 27.5 and 3.6, respectively.  
29 The system demonstrated high efficiency across a broad pH range (5–11) and showed  
30 strong resistance to common interfering ions. Mechanistic investigations, including  
31 quenching experiments, EPR analysis, and DFT calculations, revealed that  $^1\text{O}_2$  was the  
32 predominant reactive species. The internal electron transfer from  $\text{Cu}_2\text{S}$  to  $\text{Co}_3\text{S}_4$  enhanced  
33  $\text{H}_2\text{O}_2$  adsorption and activation, facilitating efficient electron transfer from TC to the  
34 surface-activated  $\text{H}_2\text{O}_2$  complex. Besides, the redox cycles of  $\text{Cu}^+/\text{Cu}^{2+}$  and  $\text{Co}^{2+}/\text{Co}^{3+}$ ,  
35 promoted by low-valence sulfur, sustained the catalytic activity. Degradation pathways  
36 were proposed, and toxicity assessment indicated the effective detoxification of TC. This  
37 work provides a highly efficient and stable heterostructured catalyst and offers deep  
38 insights into the  $\text{H}_2\text{O}_2$  activation mechanism dominated by  $^1\text{O}_2$  for antibiotic wastewater  
39 remediation.

40 **Keywords:** AOPs;  $\text{Co}_3\text{S}_4$ ;  $\text{Cu}_2\text{S}$ ; Tetracycline degradation;  $^1\text{O}_2$ ; Electron transfer process

## 41 **1. Introduction**

42 Tetracycline (TC) is one of the most commonly used antibiotics for treating bacterial  
43 infections in human medicine and animal husbandry [1]. Globally, annual antibiotic  
44 consumption is estimated to be between 100,000 and 200,000 tons [2]. In livestock and  
45 aquaculture operations, only 20–30% of administered TC is absorbed and utilized by  
46 animals; the remainder is excreted as metabolites and released into surface water,  
47 groundwater, soil, and sediments [3]. Antibiotics, with their complex molecular structures,  
48 inhibit or disrupt bacterial growth [4]. The persistence of TC compounds in the  
49 environment promotes the development of antibiotic-resistant pathogens, posing serious  
50 threats to ecological balance and public health [5]. Hence, there is an urgent need to  
51 develop efficient and robust methods for TC removal to protect environmental safety and  
52 human health.

53 Advanced oxidation processes (AOPs), generating reactive oxygen species (ROS,  
54 e.g.,  $\bullet\text{OH}$ ,  $\text{SO}_4^{\bullet-}$ , etc.), are widely used for the efficient removal of organic contaminants  
55 in drinking water production, elimination of recalcitrant micropollutants in wastewater  
56 treatment, and disinfection strategies [6]. A major advantage of AOPs over conventional  
57 treatment technologies is their ability to effectively degrade refractory compounds  
58 without producing secondary waste streams, a common issue in membrane-based  
59 processes [7]. In particular, Fenton and Fenton-like systems based on  $\text{H}_2\text{O}_2$  activation  
60 have attracted growing interest due to their operational simplicity and high efficiency [8].  
61 Common activation approaches include photocatalysis, electrocatalysis, and the use of  
62 transition metals (e.g., Fe [9], Cu [10]) and bimetallic catalyst activation [11]. The  
63 reaction rate constant between Cu(I) and  $\text{H}_2\text{O}_2$  ( $10^4 \text{ M}^{-1} \text{ s}^{-1}$ ) is significantly higher than

64 that of Fe(II) ( $76 \text{ M}^{-1} \text{ s}^{-1}$ ), which makes copper-containing solid catalysts (such as zero-  
65 valent copper [12], copper oxides [13], and copper-based layered hydroxides [14])  
66 promising alternatives to conventional iron-based catalysts [15].

67 Core-shell nanostructures, with tunable internal voids and flexible manipulation of  
68 core, shell, and void configurations, have attracted considerable interest in energy storage,  
69 sensing, and catalysis [16,17]. The interior voids facilitate efficient mass transport and  
70 provide substantial space for catalytic reactions. Moreover, adjustable structural features  
71 enable the exposure of diverse active sites, enhancing the adsorption and conversion of  
72 intermediates [18,19]. Heterostructured metal sulfides, constructed from interfaces  
73 between two distinct metal sulfides, demonstrate significantly improved catalytic activity  
74 compared to their single-component counterparts [20].

75 Owing to the superior catalytic properties of cobalt, considerable research has  
76 focused on heterogeneous cobalt catalysts, such as cobalt oxides, cobalt-containing mixed  
77 metal oxides, and supported cobalt materials [21,22]. Sulfur, with its low  
78 electronegativity and high ionization energy, serves as an effective coordinating element.  
79 Unsaturated sulfur atoms on transition metal sulfide surfaces can capture protons,  
80 exposing reduced metal active sites [23]. Low-valent sulfur species ( $\text{S}^{2-}$ ,  $\text{S}_2^{2-}$ ) in copper  
81 sulfides facilitate the reduction of Cu(II) to Cu(I), enhancing catalytic activity [24]. Sulfur  
82 coordination in structures such as  $\text{MoS}_2@\text{Co}_3\text{S}_4$  promotes efficient electron-hole  
83 separation and increases active site accessibility, boosting sulfamethoxazole degradation  
84 [25].

85 Based on this rationale, we hypothesize that a  $\text{Cu}_2\text{S}@\text{Co}_3\text{S}_4$  composite, synthesized  
86 by growing  $\text{Co}_3\text{S}_4$  on  $\text{Cu}_2\text{S}$ , can function as a highly efficient catalyst for  $\text{H}_2\text{O}_2$  activation

87 to degrade refractory organic pollutants. Herein,  $\text{Cu}_2\text{S}@\text{Co}_3\text{S}_4$  was prepared via a  
88 hydrothermal route. Its morphology, crystal structure, and chemical composition were  
89 systematically characterized. The effects of catalyst dosage,  $\text{H}_2\text{O}_2$  concentration, initial  
90 solution pH, and coexisting ions on TC degradation were evaluated. ROS generation and  
91 contribution were elucidated through EPR spectroscopy and quenching experiments. The  
92 adsorption energy of  $\text{H}_2\text{O}_2$  at the catalyst interface and the number of electrons transferred  
93 were obtained through DFT calculations. A plausible mechanism for TC degradation in  
94 the  $\text{Cu}_2\text{S}@\text{Co}_3\text{S}_4/\text{H}_2\text{O}_2$  system was proposed, along with identification of degradation  
95 intermediates and pathways.

## 96 **2. Experimental methods**

### 97 2.1. Chemicals

98 TC, furfuryl alcohol (FFA), tert-butyl alcohol (TBA), methanol (MeOH), 1,4-  
99 benzoquinone (BQ), methyl phenyl sulfoxide (PMSO), and methyl phenyl sulfone  
100 (PMSO<sub>2</sub>) were obtained from Macklin Biochemical Technology Co., Ltd. (Shanghai,  
101 China). Hydrogen peroxide ( $\text{H}_2\text{O}_2$ , 30%), 5,5-Dimethyl-1-pyrroline N-oxide (DMPO),  
102 2,2,6,6-tetra-methyl-4-piperidone (TEMP) were purchased from Sigma-Aldrich  
103 Chemical Co., Ltd. (China).  $\text{CuCl}_2 \cdot 2\text{H}_2\text{O}$ ,  $\text{CoCl}_2 \cdot 6\text{H}_2\text{O}$ , sodium citrate dihydrate  
104 ( $\text{Na}_3\text{C}_6\text{H}_5\text{O}_7 \cdot 2\text{H}_2\text{O}$ ), L-ascorbic acid ( $\text{C}_6\text{H}_8\text{O}_6$ ), urea ( $\text{CH}_4\text{N}_2\text{O}$ ), thioacetamide ( $\text{C}_2\text{H}_5\text{NS}$ ),  
105 acetic acid (HAc), nitrobenzene (NB), NaOH, HCl, NaCl,  $\text{NaNO}_3$ ,  $\text{Na}_2\text{SO}_4$ , and  $\text{Na}_2\text{CO}_3$   
106 were purchased from Sinopharm Chemical Reagent Co., Ltd. (Shanghai, China). All  
107 chemicals were analytical grade and used without further purification. Ultra-pure water  
108 ( $18.25 \text{ M}\Omega \cdot \text{cm}$ ) was prepared using a Millipore system (Bedford, USA).

### 109 2.2. Catalyst synthesis and characterizations

110           **Synthesis of Cu<sub>2</sub>O nanocubes.** 2 mmol CuCl<sub>2</sub>·2H<sub>2</sub>O and 1 mmol trisodium citrate  
111 were dissolved in 160 mL deionized water. Then, 40 mL of 1.25 M NaOH aqueous  
112 solution was added dropwise under magnetic stirring for 5 min, changing the solution  
113 color from light blue to dark blue. Subsequently, 100 mL of 0.03 M L-ascorbic acid  
114 solution was introduced, and the reaction proceeded for 10 min. The mixture was aged at  
115 room temperature for 1 h. The precipitate was collected by vacuum filtration, washed  
116 with deionized water and anhydrous ethanol, and dried under vacuum at 60 °C for 12 h.

117           **Synthesis of Cu<sub>2</sub>S@Co<sub>3</sub>S<sub>4</sub>.** A total of 71.5 mg of the as-synthesized Cu<sub>2</sub>O was  
118 dispersed in 15 mL deionized water under stirring for 10 min. Separately, a specific  
119 amount of CoCl<sub>2</sub>·6H<sub>2</sub>O, 250 mg urea, and 150 mg (4 mmol) thioacetamide were dissolved  
120 in 25 mL anhydrous ethanol. The Cu<sub>2</sub>O suspension was slowly poured into the ethanol  
121 solution. The mixture was stirred and sonicated for 5 min, transferred into a Teflon-lined  
122 autoclave, and maintained at 180 °C for 22 h. The product was collected via vacuum  
123 filtration, washed with deionized water and ethanol, and dried under vacuum at 60 °C for  
124 12 h. Finally, the material was calcined at 450 °C for 1 h under nitrogen to obtain  
125 Cu<sub>2</sub>S@Co<sub>3</sub>S<sub>4</sub>. Composites with nominal Cu:Co molar ratios of 4:1, 2:1, and 1:1 were  
126 synthesized by adding 29.7 mg, 59.5 mg, and 119.0 mg of CoCl<sub>2</sub>·6H<sub>2</sub>O, respectively. For  
127 comparison, Cu<sub>2</sub>S and Co<sub>3</sub>S<sub>4</sub> were prepared under identical conditions without adding  
128 Cu<sub>2</sub>O or cobalt chloride.

129           The synthesis procedure of Cu<sub>2</sub>S@Co<sub>3</sub>S<sub>4</sub> is illustrated in [Scheme 1](#). Comprehensive  
130 characterization details is described in [Text S1](#) in the [Supplementary Material](#).

### 131 2.3. Degradation tests of TC

132           All degradation experiments were conducted in 100 mL glass beakers. Typically, 4

133 mg of catalyst was dispersed homogeneously in 50 mL of a 20  $\mu$ M TC solution via  
134 ultrasonication for 1 min. The degradation process was initiated by adding  $\text{H}_2\text{O}_2$  to  
135 achieve a final concentration of 5 mM. At predetermined intervals, 0.5 mL aliquots were  
136 collected, filtered through a 0.22  $\mu$ m membrane, and quenched with 0.2 mL of methanol.  
137 The TC concentration was quantified using high-performance liquid chromatography  
138 (HPLC, Agilent 1260, USA) equipped with a Symmetry C18 column  
139 (150mm $\times$ 4.6mm $\times$ 5 $\mu$ m, Agilent, USA) and a VWD detector (Agilent, USA). All  
140 experiments were performed in triplicate, and the results are reported as mean values with  
141 standard deviations. The steady state concentration of  $\bullet\text{OH}$  and  $^1\text{O}_2$  calculation method,  
142 and DFT calculation method can be found in [Text S2](#) and [S3](#).

### 143 **3. Results and discussion**

#### 144 3.1. Characterizations

145 The morphology of  $\text{Cu}_2\text{O}$  and  $\text{Cu}_2\text{S}@ \text{Co}_3\text{S}_4$  composite was characterized using  
146 scanning electron microscopy (SEM) and transmission electron microscopy (TEM). As  
147 shown in [Figure 1a](#),  $\text{Cu}_2\text{O}$  exhibit a well-defined nanocube morphology with an average  
148 size of approximately 500 nm. [Figure 1b](#) shows that  $\text{Cu}_2\text{S}@ \text{Co}_3\text{S}_4$  composite retains the  
149 cubic framework of the  $\text{Cu}_2\text{O}$  precursor, with a rougher surface and an average size of 1  
150  $\mu$ m. The TEM image ([Figure 1c](#)) confirms the distinct cubic architecture. Energy-  
151 dispersive X-ray spectroscopy (EDS) elemental mapping [Figure 1d–f](#) demonstrates  
152 homogeneous distribution of Cu, Co, and S, with Co predominantly located on the outer  
153 region, indicating a core–shell structure of the as-synthesized  $\text{Cu}_2\text{S}@ \text{Co}_3\text{S}_4$ .

154 [Figure 1g](#) and [h](#) shows the XRD patterns of  $\text{Cu}_2\text{O}$ ,  $\text{Cu}_2\text{S}$ ,  $\text{Co}_3\text{S}_4$ , and  $\text{Cu}_2\text{S}@ \text{Co}_3\text{S}_4$   
155 composites with different molar ratios. In [Figure 1g](#), the diffraction peaks observed at

156 29.6°, 36.5°, 42.4°, 52.6°, 61.5°, 73.7°, and 77.6° are indexed to the (110), (111), (200),  
157 (211), (220), and (222) crystal planes of Cu<sub>2</sub>O (PDF#75-1531), respectively, confirming  
158 the successful synthesis of phase-pure Cu<sub>2</sub>O. As show in [Figure 1h](#), diffraction peaks at  
159 27.7°, 32.1°, 46.0°, 54.5°, 67.1°, and 85.2° are indexed to the (111), (200), (220), (311),  
160 (400), and (422) crystal planes of Cu<sub>2</sub>S (PDF#72-1966), respectively. Meanwhile, peaks  
161 at 16.3°, 26.8°, 31.5°, 41.8°, 50.3°, and 55.1° correspond to the (111), (220), (311), (331),  
162 (511), and (440) planes of Co<sub>3</sub>S<sub>4</sub> (PDF#75-1561), respectively. No impurity peaks were  
163 detected, indicating successful preparation of a highly crystalline composite.

164 Electron paramagnetic resonance (EPR) spectroscopy is a highly sensitive technique  
165 used to characterize material defects by detecting unpaired electrons associated with such  
166 imperfections [\[26\]](#). As shown in [Figure S1](#), the EPR spectra of Cu<sub>2</sub>S, Co<sub>3</sub>S<sub>4</sub>, and  
167 Cu<sub>2</sub>S@Co<sub>3</sub>S<sub>4</sub> all exhibit signals corresponding to sulfur vacancy (Sv). Among these,  
168 Co<sub>3</sub>S<sub>4</sub> shows the most intense Sv signal, whereas both Cu<sub>2</sub>S and the Cu<sub>2</sub>S@Co<sub>3</sub>S<sub>4</sub>  
169 composite display weaker and comparable signal intensities, suggesting similar sulfur  
170 vacancies contents in these two materials. The XRD signal intensities for Cu<sub>2</sub>S and  
171 Cu<sub>2</sub>S@Co<sub>3</sub>S<sub>4</sub> are strikingly higher than those of CoS<sub>2</sub>, demonstrating significantly greater  
172 crystallinity ([Figure 1h](#)). This clearly demonstrates that metal and sulfur atoms within  
173 Cu<sub>2</sub>S and Cu<sub>2</sub>S@Co<sub>3</sub>S<sub>4</sub> are more fully integrated, leading to a substantially reduced defect  
174 density. This superior structural integrity further attests to their enhanced stability, which  
175 underpins sustained long-term catalytic performance.

176 X-ray photoelectron spectroscopy (XPS) was employed to analyze the elemental  
177 states and surface composition of the Cu<sub>2</sub>S@Co<sub>3</sub>S<sub>4</sub> composite. The XPS survey spectrum  
178 of Cu<sub>2</sub>S@Co<sub>3</sub>S<sub>4</sub> ([Figure 2a](#)) shows the main elements of Cu<sub>2</sub>S@Co<sub>3</sub>S<sub>4</sub> including Cu, Co

179 and S. Two characteristic peaks of Cu<sup>+</sup> at 932.5 eV (2p<sub>3/2</sub>) and 952.3 eV (2p<sub>1/2</sub>) are found  
180 in the high-resolution Cu 2p spectrum (Figure 2b), consistent with the typical valence  
181 state in Cu<sub>2</sub>S [27]. Additionally, peaks identified at 934.4 eV (Cu<sup>2+</sup> 2p<sub>3/2</sub>) and 954.7 eV  
182 (Cu<sup>2+</sup> 2p<sub>1/2</sub>), along with satellite features at 943.9 eV and 963.2 eV, are likely due to  
183 surface oxidation of Cu<sub>2</sub>S [28]. The Co 2p spectrum (Figure 2c) reveals two spin-orbit  
184 doublets and two satellite peaks. The peaks at binding energies of 778.9 eV and 793.7 eV  
185 are assigned to Co<sup>3+</sup> 2p<sub>3/2</sub> and Co<sup>3+</sup> 2p<sub>1/2</sub>, respectively, while those at 781.0 eV and 796.4  
186 eV correspond to Co<sup>2+</sup> 2p<sub>3/2</sub> and Co<sup>2+</sup> 2p<sub>1/2</sub>. Satellite peaks are observed at 784.4 eV and  
187 801.1 eV. These spectral features align well with previously reported valence states of  
188 Co<sub>3</sub>S<sub>4</sub> [29,30]. The S 2p spectrum (Figure 2d) can be deconvoluted into two spin-orbit  
189 doublets and an additional peak. The doublets consist of components at 161.5 eV (S<sup>2-</sup>  
190 2p<sub>3/2</sub>), 162.7 eV (S<sup>2-</sup> 2p<sub>1/2</sub>), 162.9 eV (S<sub>2</sub><sup>2-</sup> 2p<sub>3/2</sub>), and 164.3 eV (S<sub>2</sub><sup>2-</sup> 2p<sub>1/2</sub>), along with a  
191 peak at 168.4 eV attributed to SO<sub>3</sub><sup>2-</sup> species [31].

### 192 3.2. Catalytic activity tests

193 The catalytic performance of the Cu<sub>2</sub>S@Co<sub>3</sub>S<sub>4</sub> composite for activating H<sub>2</sub>O<sub>2</sub> toward  
194 TC degradation was systematically evaluated. As depicted in Figure 3a, control  
195 experiments revealed that neither H<sub>2</sub>O<sub>2</sub> alone nor the Co<sub>3</sub>S<sub>4</sub>/H<sub>2</sub>O<sub>2</sub> system achieved  
196 significant TC removal within 30 min, underscoring the limited non-catalytic oxidation  
197 and the low intrinsic activity of Co<sub>3</sub>S<sub>4</sub>. When employed as an adsorbent without H<sub>2</sub>O<sub>2</sub>,  
198 the Cu<sub>2</sub>S@Co<sub>3</sub>S<sub>4</sub> composite itself removed 51% of TC, while the Cu<sub>2</sub>S/H<sub>2</sub>O<sub>2</sub> system led  
199 to a 63% degradation. In stark contrast, all Cu<sub>2</sub>S@Co<sub>3</sub>S<sub>4</sub> composites with varying  
200 Cu:Co ratios, in the presence of H<sub>2</sub>O<sub>2</sub> (5 mM) and catalyst (0.08 g/L), achieved  
201 exceptional TC removal exceeding 92%. Among them, the composite with a Cu:Co ratio

202 of 2:1 demonstrated the highest efficiency. The kinetic analysis (Figure 3b) further  
203 confirmed this trend, yielding pseudo-first-order kinetic rate constants ( $k$ ) of  $0.077 \text{ min}^{-1}$ ,  
204  $0.110 \text{ min}^{-1}$ , and  $0.076 \text{ min}^{-1}$  for the composites with Cu:Co ratios of 4:1, 2:1, and 1:1,  
205 respectively. Impressively, the rate constant for the optimal  $\text{Cu}_2\text{S}@ \text{Co}_3\text{S}_4$  (2:1) was 27.5  
206 times and 3.6 times greater than that of  $\text{Co}_3\text{S}_4$  ( $0.004 \text{ min}^{-1}$ ) and  $\text{Cu}_2\text{S}$  ( $0.030 \text{ min}^{-1}$ ),  
207 respectively.

### 208 3.3. Influencing factors on TC degradation

209 The effects of various operational parameters, including catalyst dosage (0.04–0.16  
210 g/L),  $\text{H}_2\text{O}_2$  concentration (1–7 mM), initial pH (3–11), and coexisting ions (such as  $\text{Cl}^-$ ,  
211  $\text{NO}_3^-$ ,  $\text{SO}_4^{2-}$ , and  $\text{CO}_3^{2-}$ ) on TC degradation by the  $\text{Cu}_2\text{S}@ \text{Co}_3\text{S}_4/\text{H}_2\text{O}_2$  system are  
212 discussed below. As shown in Figure 3c, the degradation efficiency improved with  
213 increasing catalyst dosage. Specifically, when the dosage increased from 0.04 to 0.08 g/L,  
214 the TC removal rate rose from 85% to 97% within 30 min. This enhancement can be  
215 attributed to the increased number of active sites available for  $\text{H}_2\text{O}_2$  activation and the  
216 consequent generation of reactive species [32]. However, further increases in catalyst  
217 dosage did not yield a significant enhancement in degradation efficiency, suggesting that  
218 excessive catalyst addition is unnecessary. Accordingly, a dosage of 0.08 g/L was selected  
219 as optimal for subsequent experiments. The concentration of  $\text{H}_2\text{O}_2$  also played a critical  
220 role in the degradation process (Figure 3d). TC degradation improved slightly as the  $\text{H}_2\text{O}_2$   
221 concentration increased from 1 to 7 mM, which can be explained by the greater abundance  
222 of reactive species generated at higher  $\text{H}_2\text{O}_2$  levels, promoting more efficient TC  
223 elimination [33]. Based on these results, an  $\text{H}_2\text{O}_2$  concentration of 5 mM was chosen for  
224 further studies.

225 The initial solution pH also significantly influenced the degradation efficiency. As  
226 depicted in Figure 3e, high acidic conditions (pH=3) inhibited TC degradation. In contrast,  
227 over a broad pH range (5–11), the Cu<sub>2</sub>S@Co<sub>3</sub>S<sub>4</sub>/H<sub>2</sub>O<sub>2</sub> system maintained a TC removal  
228 efficiency exceeding 97%, indicating that the catalyst can perform effectively without pH  
229 adjustment, a notable advantage for practical applications. The inhibitory effect under  
230 acidic conditions may be due to H<sup>+</sup> ions scavenging •OH radicals ( $H^+ + \bullet OH + e^- \rightarrow H_2O$ )  
231 [34], thereby reducing oxidative capacity. Moreover, higher pH values promote the  
232 deprotonation of TC into anionic forms, which exhibit higher electron density and are  
233 more susceptible to attack by H<sub>2</sub>O<sub>2</sub> and free radicals, facilitating molecular  
234 decomposition [35].

235 The effects common inorganic anions on TC degradation were investigated to  
236 simulate natural water conditions (Figure 3f). The presence of 5 mM Cl<sup>-</sup> resulted in  
237 approximately 5% inhibition, likely due to the formation of less reactive chlorine species  
238 (e.g., ClOH•<sup>-</sup> via  $\bullet OH + Cl^- \rightarrow ClOH\bullet^-$ ) [36]. Both NO<sub>3</sub><sup>-</sup> and SO<sub>4</sub><sup>2-</sup> showed slight  
239 inhibitory effects, possibly due to competitive adsorption at catalyst active sites [37]. In  
240 contrast, CO<sub>3</sub><sup>2-</sup> enhanced degradation, potentially because it raises the solution pH and  
241 generates carbonate radicals that participate in electron transfer processes with aromatic  
242 rings in TC. It has been reported that TC degradation proceeds mainly through electron  
243 addition to aromatic rings rather than hydroxylation [38], a pathway further promoted by  
244 carbonate radicals. Despite the presence of these coexisting ions, the system still achieved  
245 over 90% TC removal, demonstrating robust performance and stability under  
246 environmentally relevant conditions.

247 The stability and practical applicability of solid catalysts hinge critically on their

248 recyclability. The recyclability of Cu<sub>2</sub>S@Co<sub>3</sub>S<sub>4</sub> was rigorously evaluated over five  
249 consecutive degradation cycles. Following each cycle, the catalyst was meticulously  
250 recovered, washed with ultrapure water and ethanol, and vacuum-dried prior to reuse. As  
251 shown [Figure S2](#), the catalyst maintained a robust TC degradation efficiency of 80% even  
252 after five cycles, underscoring its satisfactory recyclability and structural stability.  
253 Analysis by atomic absorption spectrophotometry furthermore revealed that the leaching  
254 concentration of copper ions was 1.2 mg/L, which was below the stringent EU Drinking  
255 Water Directive limit of 2 mg/L. While no cobalt ion leaching was detected,  
256 unequivocally confirming the catalyst's high stability under operational conditions.

#### 257 3.4. Identification of reactive species

258 The reactive species governing the TC degradation in the Cu<sub>2</sub>S@Co<sub>3</sub>S<sub>4</sub>/H<sub>2</sub>O<sub>2</sub> system  
259 were systematically identified through a combination of scavenging and spectroscopic  
260 techniques. TBA was applied as an effective quencher for •OH (rate constant: 3.8–7.6 ×  
261 10<sup>8</sup> M<sup>-1</sup> s<sup>-1</sup>) [39], FFA for both •OH (1.5 × 10<sup>10</sup> M<sup>-1</sup> s<sup>-1</sup>) and <sup>1</sup>O<sub>2</sub> (1.2 × 10<sup>8</sup> M<sup>-1</sup> s<sup>-1</sup>) [40],  
262 and BQ for •O<sub>2</sub><sup>-</sup> [41]. As shown in [Figure 4a](#), the drastic inhibition by FFA pointed to <sup>1</sup>O<sub>2</sub>  
263 as a pivotal species, the partial suppression by TBA indicated a secondary role for •OH,  
264 and the non-inhibition by BQ effectively excluded •O<sub>2</sub><sup>-</sup> as a primary contributor. This  
265 interpretation was directly validated by EPR spectroscopy, using DMPO and TEMP as  
266 spin-trapping agents to identify the ROS generated in the Cu<sub>2</sub>S@Co<sub>3</sub>S<sub>4</sub>/H<sub>2</sub>O<sub>2</sub> system. As  
267 shown in [Figure 4b-d](#), no radical signals emerged in the absence of H<sub>2</sub>O<sub>2</sub>, demonstrating  
268 conclusively that Cu<sub>2</sub>S@Co<sub>3</sub>S<sub>4</sub> alone fails to generate radicals. However, distinct signals  
269 for DMPO-•OH, TEMP-<sup>1</sup>O<sub>2</sub>, and DMPO-•O<sub>2</sub><sup>-</sup> adducts emerged when both Cu<sub>2</sub>S@Co<sub>3</sub>S<sub>4</sub>  
270 and H<sub>2</sub>O<sub>2</sub> were present, unequivocally verifying the generation of •OH, <sup>1</sup>O<sub>2</sub>, and •O<sub>2</sub><sup>-</sup>

271 radicals.

272 To quantitatively differentiate the roles of ROS, the steady-state concentrations of  
273  $\bullet\text{OH}$  and  $^1\text{O}_2$  were measured, while  $\bullet\text{O}_2^-$  was excluded due to its low oxidative potential  
274 ( $-0.2\text{ V}$ ) [42]. As illustrated in Figure 5a, probe experiments using nitrobenzene (NB) and  
275 FFA revealed that the steady-state concentration of  $^1\text{O}_2$  was  $3.39 \times 10^{-10}\text{ M}$ , which was  
276 nearly two orders of magnitude higher than that of  $\bullet\text{OH}$  ( $5.34 \times 10^{-12}\text{ M}$ ). Additionally,  
277 the potential formation of high-valent metal species was examined, but no conversion of  
278 PMSO to PMSO<sub>2</sub> was observed (Figure 5b), confirming their absence. Together, the  
279 quantitative predominance of  $^1\text{O}_2$  and the exclusion of other potent oxidants definitively  
280 establish  $^1\text{O}_2$  as the primary species driving TC degradation.

281 The generation of  $^1\text{O}_2$  in AOPs can originate from multiple pathways, such as light  
282 irradiation [43], energy transfer from dissolved oxygen [44], or the recombination of  $\bullet\text{O}_2^-$   
283 radicals [45]. To distinguish the operative mechanism in the Cu<sub>2</sub>S@Co<sub>3</sub>S<sub>4</sub>/H<sub>2</sub>O<sub>2</sub> system,  
284 were conducted degradation experiments under critical controlled conditions. The results  
285 (Figure 5c) show that excluding either light (dark conditions) or DO (N<sub>2</sub> purging) did not  
286 impair the reaction efficiency, thereby eliminating these two as major  $^1\text{O}_2$  sources. This  
287 experimental exclusion, coupled with the earlier finding that  $\bullet\text{O}_2^-$  quenching did not  
288 inhibit degradation, allow us to definitively rule out the recombination route. Therefore,  
289 the evidence collectively points to the direct activation of H<sub>2</sub>O<sub>2</sub> at the catalyst interface  
290 as the principal mechanism for  $^1\text{O}_2$  production.

### 291 3.5. Enhanced electron transfer process

292 We investigated the electron transfer process, a pivotal degradation mechanism in  
293 heterogeneous catalysis [46], by analyzing open circuit potential (OCP). The potential

294 increase upon the addition of  $\text{H}_2\text{O}_2$  (Figure 5d) corresponded to the adsorption and surface  
295 complexation of  $\text{H}_2\text{O}_2$  (forming  $\text{H}_2\text{O}_2^*$ ). The swift potential equilibration observed in the  
296  $\text{Cu}_2\text{S}@/\text{Co}_3\text{S}_4/\text{H}_2\text{O}_2$  system pointed to a highly efficient interfacial charge transfer with  
297 the  $\text{Cu}_2\text{S}@/\text{Co}_3\text{S}_4$  heterojunction. This was directly explained by our DFT results (Figure  
298 S3), which visualized electron redistribution and a net transfer of 0.12 electrons from  
299  $\text{Cu}_2\text{S}$  to  $\text{Co}_3\text{S}_4$ . This electron enrichment on  $\text{Co}_3\text{S}_4$  optimally primed the surface for  $\text{H}_2\text{O}_2$   
300 activation. The subsequent potential surge upon TC addition provided direct  
301 electrochemical evidence that TC acted as an electron donor to the activated  $\text{H}_2\text{O}_2^*$   
302 complex [47]. The magnitude of the total potential change (0.07 V) was greatest for the  
303  $\text{Cu}_2\text{S}@/\text{Co}_3\text{S}_4$  composite, offering definitive proof that the heterojunction structure  
304 fostered the most powerful electron transfer process, thereby driving the exceptional  
305 catalytic activity.

306 Furthermore, DFT calculations were performed to compare the  $\text{H}_2\text{O}_2$  adsorption  
307 behavior and electron transfer capability of  $\text{Co}_3\text{S}_4$  and  $\text{Cu}_2\text{S}@/\text{Co}_3\text{S}_4$  (Figure 5e and f).  
308 The calculated adsorption energy for  $\text{H}_2\text{O}_2$  on  $\text{Cu}_2\text{S}@/\text{Co}_3\text{S}_4$  was  $-1.91$  eV, substantially  
309 more negative than that on pure  $\text{Co}_3\text{S}_4$  ( $-0.37$  eV), indicating a much stronger affinity and  
310 more favorable capture of  $\text{H}_2\text{O}_2$  by the composite, which promoted its subsequent  
311 activation. The enhanced activation was further evidenced by the pronounced elongation  
312 of the O–O bond in  $\text{H}_2\text{O}_2$  adsorbed on  $\text{Cu}_2\text{S}@/\text{Co}_3\text{S}_4$ , which was stretched to  $2.69$  Å,  
313 suggesting a greatly facilitated cleavage tendency. Differential charge density analysis  
314 (where red and blue regions denote electron depletion and accumulation, respectively)  
315 provided deeper insight into the interfacial electron transfer. The internal electron  
316 donation from the  $\text{Cu}_2\text{S}$  core to the  $\text{Co}_3\text{S}_4$  shell ( $0.12 e^-$ ) created an electron-rich surface,

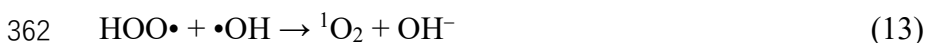
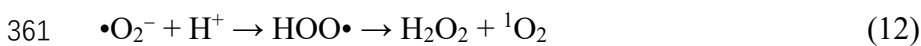
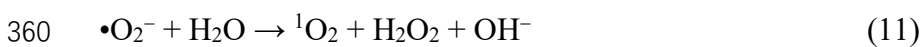
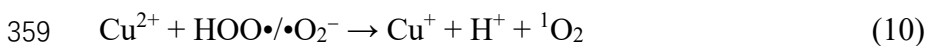
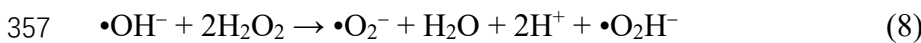
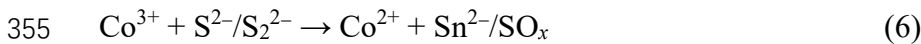
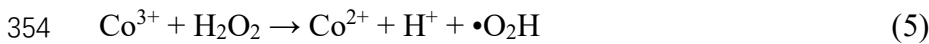
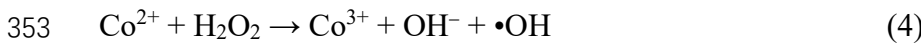
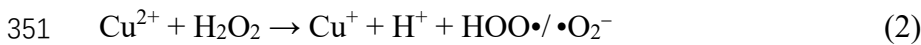
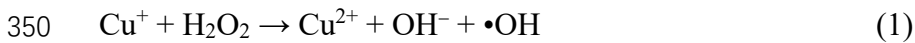
317 enabling  $\text{Co}_3\text{S}_4$  to transfer a significantly large number of electrons to the adsorbed  $\text{H}_2\text{O}_2$ .  
318 Consequently,  $\text{H}_2\text{O}_2$  gained  $0.41 \text{ e}^-$  from the  $\text{Cu}_2\text{S}@ \text{Co}_3\text{S}_4$  composite, a value six times  
319 greater than the  $0.07 \text{ e}^-$  transferred from  $\text{Co}_3\text{S}_4$  alone. These results collectively offer  
320 compelling theoretical evidence that the synergistic electron transfer within the  
321  $\text{Cu}_2\text{S}@ \text{Co}_3\text{S}_4$  heterostructure is crucial for the highly efficient activation of  $\text{H}_2\text{O}_2$ .

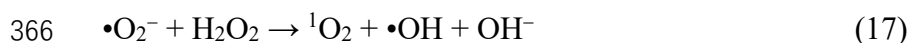
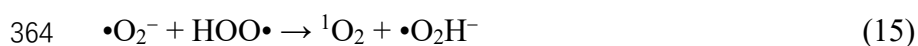
### 322 3.6. Possible $\text{H}_2\text{O}_2$ activation mechanism by $\text{Cu}_2\text{S}@ \text{Co}_3\text{S}_4$

323 To elucidate the TC degradation mechanism in the  $\text{Cu}_2\text{S}@ \text{Co}_3\text{S}_4/\text{H}_2\text{O}_2$  system, the  
324 catalyst was characterized by XPS before and after the reaction (Figure 6a). As shown in  
325 Figure 6b, the Cu 2p spectra demonstrate a marked shift in valence states: the proportion  
326 of  $\text{Cu}^+$  decreased from 79.0% to 62.9%, while  $\text{Cu}^{2+}$  increased from 21.0% to 37.1%,  
327 directly evidencing in oxidation of  $\text{Cu}^+$  and its crucial role in the catalytic cycle. Parallel  
328 changes were observed in the Co 2p spectrum (Figure 6c), where the  $\text{Co}^{3+}/\text{Co}^{2+}$  ratio  
329 increased, confirming the involvement of cobalt redox pairs. Additionally, the S 2p  
330 spectra (Figure 5d) indicated consumption of low-valence  $\text{S}^{2-}$  species and a notable rise  
331 in sulfate content (from 17% to 35%), underscoring the participation of sulfur in redox  
332 cycles. This is consistent with literature suggesting that sulfur moieties facilitate the  
333 reduction of high-valence metals (e.g.,  $\text{Cu}^{2+}$  to  $\text{Cu}^+$ ), thereby sustaining catalytic activity  
334 [48].

335 Integrating these spectroscopic insights, we propose a concerted activation  
336 mechanism (Figure 6e). The process begins with  $\text{H}_2\text{O}_2$  adsorption and activation on Co  
337 sites of  $\text{Cu}_2\text{S}@ \text{Co}_3\text{S}_4$ , initiating a redox cycle (Eqs. 4 and 5) [49]. Simultaneously,  $\text{H}_2\text{O}_2$   
338 penetrating to the core interacts with  $\text{Cu}_2\text{S}$ , triggering a complementary  $\text{Cu}^+/\text{Cu}^{2+}$  redox  
339 cycle (Eqs. 1 and 2) [50]. Critically, the low-valence sulfur acts as an electron reservoir,

340 efficiently regenerating  $\text{Cu}^+$  from  $\text{Cu}^{2+}$  and  $\text{Co}^{2+}$  from  $\text{Co}^{3+}$  (Eqs. 3 and 6) [49,51], which  
 341 amplifies the production of  $\bullet\text{OH}$  via Eqs. 1 and 4. Beyond  $\bullet\text{OH}$  generation, the system  
 342 engages multiple radical pathways. Single-electron transfer from  $\text{H}_2\text{O}_2$  to  $\text{Cu}^{2+}$  yields  
 343  $\text{HOO}\bullet/\bullet\text{O}_2^-$  (Eq. 2). while a parallel reaction at  $\text{Co}^{3+}$  sites produces  $\bullet\text{O}_2\text{H}$  radicals (Eq. 5).  
 344 These species further react to form  $\bullet\text{O}_2^-$  (Eqs. 7–9) [49,52,53].  $^1\text{O}_2$  is then generated via  
 345 three dominant routes: (i) oxidation of  $\text{Cu}^{2+}$  by  $\text{HOO}\bullet/\bullet\text{O}_2^-$  (Eq. 10); (ii) interconversion  
 346 and recombination of  $\text{HOO}\bullet$ ,  $\bullet\text{O}_2^-$ , and  $\bullet\text{OH}$  (Eqs. 11–15); and (iii) reactions between  
 347  $\text{H}_2\text{O}_2$  and peroxide radicals (Eqs. 16 and 17). Finally, direct electron transfer from TC to  
 348 the catalyst surface, enhanced by the internal electron flow between  $\text{Cu}_2\text{S}$  and  $\text{Co}_3\text{S}_4$ ,  
 349 constitutes a vital non-radical degradation pathway.





### 367 3.7. Degradation pathways and toxicity analysis of intermediates

368 The degradation intermediates of TC by the  $\text{Cu}_2\text{S}@/\text{Co}_3\text{S}_4/\text{H}_2\text{O}_2$  system were  
369 identified by high-performance liquid chromatography-mass spectrometry (HPLC-MS).  
370 A total of 17 intermediates were detected (Figure S4 and Table S1), and three potential  
371 degradation pathways are proposed in Figure 7, involving terminal oxidation,  
372 dealkylation, deamidation, and ring-opening reactions [54]. In Pathway 1, a nucleophilic  
373 reaction yields intermediate P1 ( $m/z = 461$ ), which is subsequently dehydrogenated via  
374  $\bullet\text{O}_2^-$  attack to form P2 ( $m/z = 459$ ) [51], followed by deamidation to produce P3 ( $m/z =$   
375 416) [55]. Pathway 2 begins with the removal of two methyl groups from the tertiary  
376 amine, forming P4 ( $m/z = 417$ ). This pathway then bifurcates: one branch proceeds  
377 through ring cleavage, dehydration, and loss of an amide group to generate P5 ( $m/z = 379$ )  
378 and P7 ( $m/z = 362$ ). Cleavage of a two-carbon unit and carbonyl loss from P5 leads to P6  
379 ( $m/z = 239$ ) [56], while ring-opening of the carbonyl-containing moiety in P7 produces  
380 P8 ( $m/z = 318$ ) [57], which further undergoes hydrolysis and decarbonylation to yield P6  
381 as well. In Pathway 3, TC undergoes terminal oxidation to form P9 ( $m/z = 475$ ), which is  
382 subsequently degraded via dealkylation and benzene ring cleavage to P10 ( $m/z = 362$ )  
383 [51]. Subsequent removal of an amino group and a carbonyl leads to P11 ( $m/z = 309$ ),  
384 followed by dehydration to form P12 ( $m/z = 242$ ) [58]. Additionally, several small  
385 molecular intermediates were identified, including P13 ( $m/z = 239$ ), P14 ( $m/z = 164$ ) [55],

386 P15 ( $m/z = 132$ ), P16 ( $m/z = 118$ ), and P17 ( $m/z = 60$ ) [51]. All these intermediates can  
387 be further mineralized into low-molecular-weight compounds such as  $H_2O$ ,  $CO_2$ , and  
388  $NO_3^-$  through ongoing reactions with  $^1O_2$ ,  $\bullet OH$ , and  $\bullet O_2^-$ .

389 The developmental toxicity and mutagenicity of TC and its major degradation  
390 intermediates were predicted using the Toxicity Estimation Software Tool (T.E.S.T.  
391 Version 5.1.2) based on quantitative structure–activity relationship (QSAR) modeling. As  
392 shown in Figure S5, TC exhibits pronounced developmental toxicity (score: 0.86) and  
393 positive mutagenicity (score: 0.6). In contrast, most intermediates demonstrate reduced  
394 toxicity. Specifically, developmental toxicity decreases for all identified intermediates  
395 except P4, P8, and P12 (Figure S5a), and similarly, mutagenicity is lower for the majority  
396 of products (Figure S5b). These findings confirm that the  $Cu_2S@Co_3S_4/H_2O_2$  system not  
397 only degrades TC effectively but also reduces the ecological toxicity of the resulting  
398 products, highlighting its potential for mitigating the environmental risks of TC  
399 contamination.

#### 400 4. Conclusions

401 In this study, a highly efficient and stable  $Cu_2S@Co_3S_4$  core-shell heterostructure  
402 catalyst was successfully fabricated and applied to activate  $H_2O_2$  for the degradation of  
403 TC. The composite demonstrated superior catalytic performance compared to its  
404 individual components, achieving rapid and nearly complete TC removal under optimized  
405 conditions. The key findings and implications of this work are summarized as follows: (i)  
406 the  $Cu_2S@Co_3S_4/H_2O_2$  system operated effectively over a wide pH range (5–11) and  
407 maintained robust performance in the presence of common anions, highlighting its  
408 potential for practical applications; (ii) a comprehensive mechanistic study unveiled that

409  $^1\text{O}_2$  produced from the activation of  $\text{H}_2\text{O}_2$  at the catalyst interface rather than via energy  
410 transfer from dissolved oxygen, was the primary reactive species; (iii) DFT calculations  
411 and electrochemical analysis confirmed that internal electron transfer from the  $\text{Cu}_2\text{S}$  core  
412 to the  $\text{Co}_3\text{S}_4$  shell created an electron-rich surface, which significantly strengthened  $\text{H}_2\text{O}_2$   
413 adsorption, facilitated O–O bond elongation, and promoted efficient electron transfer  
414 from TC to the oxidant; (iv) the identification of degradation intermediates and  
415 subsequent toxicity evaluation confirmed that the catalytic process effectively reduced  
416 the toxicity of the reaction products, thereby mitigating the environmental risk. In  
417 conclusion, this work not only presents  $\text{Cu}_2\text{S}@ \text{Co}_3\text{S}_4$  as a promising, durable catalyst for  
418 antibiotic wastewater treatment via  $\text{H}_2\text{O}_2$  activation but also provides a profound and  
419 detailed understanding of the non-radical  $^1\text{O}_2$  dominated mechanism and the critical role  
420 of interfacial electron transfer in heterostructure catalysts. The insights gained could  
421 guide the rational design of advanced catalytic materials for environmental remediation.

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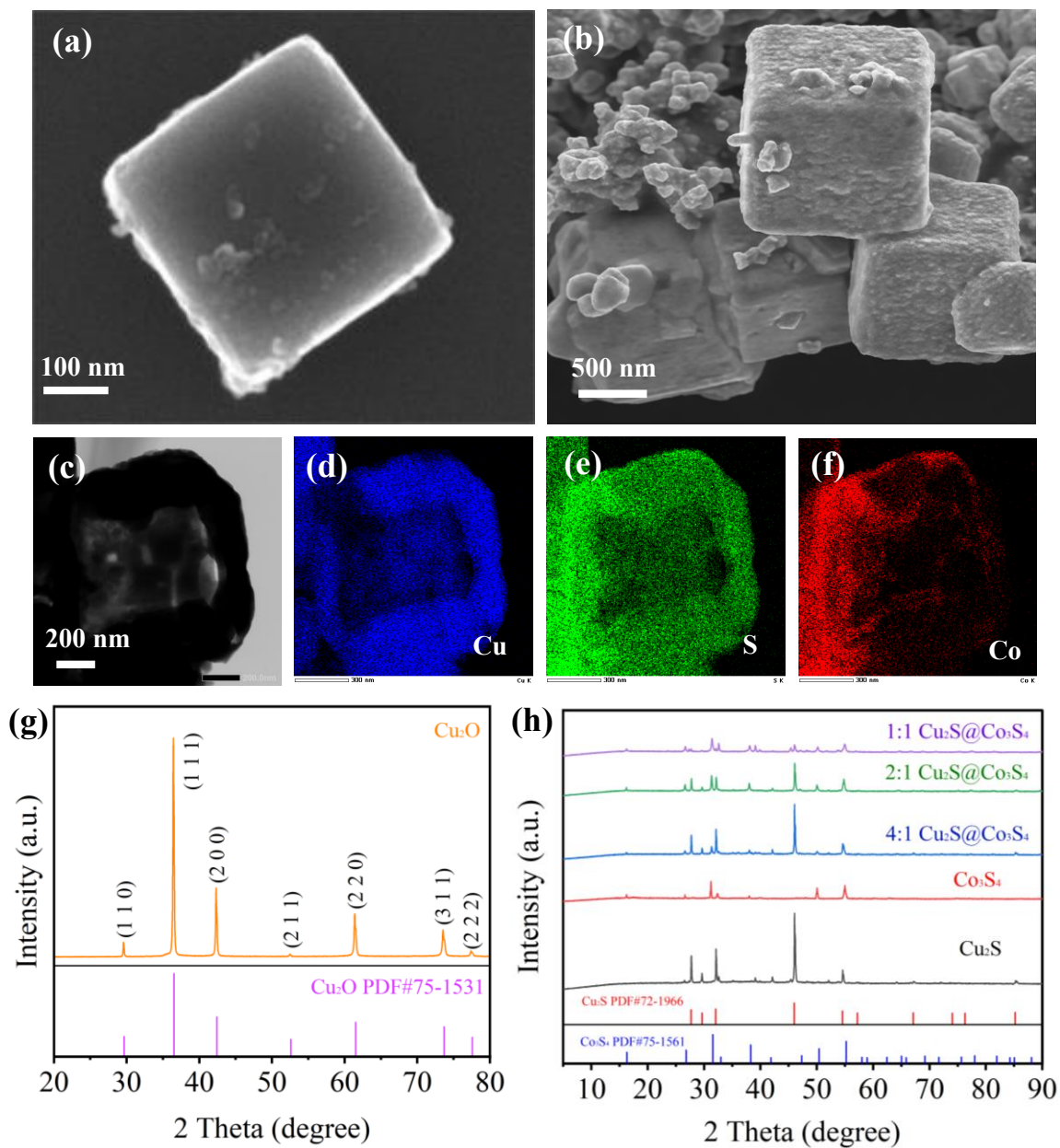
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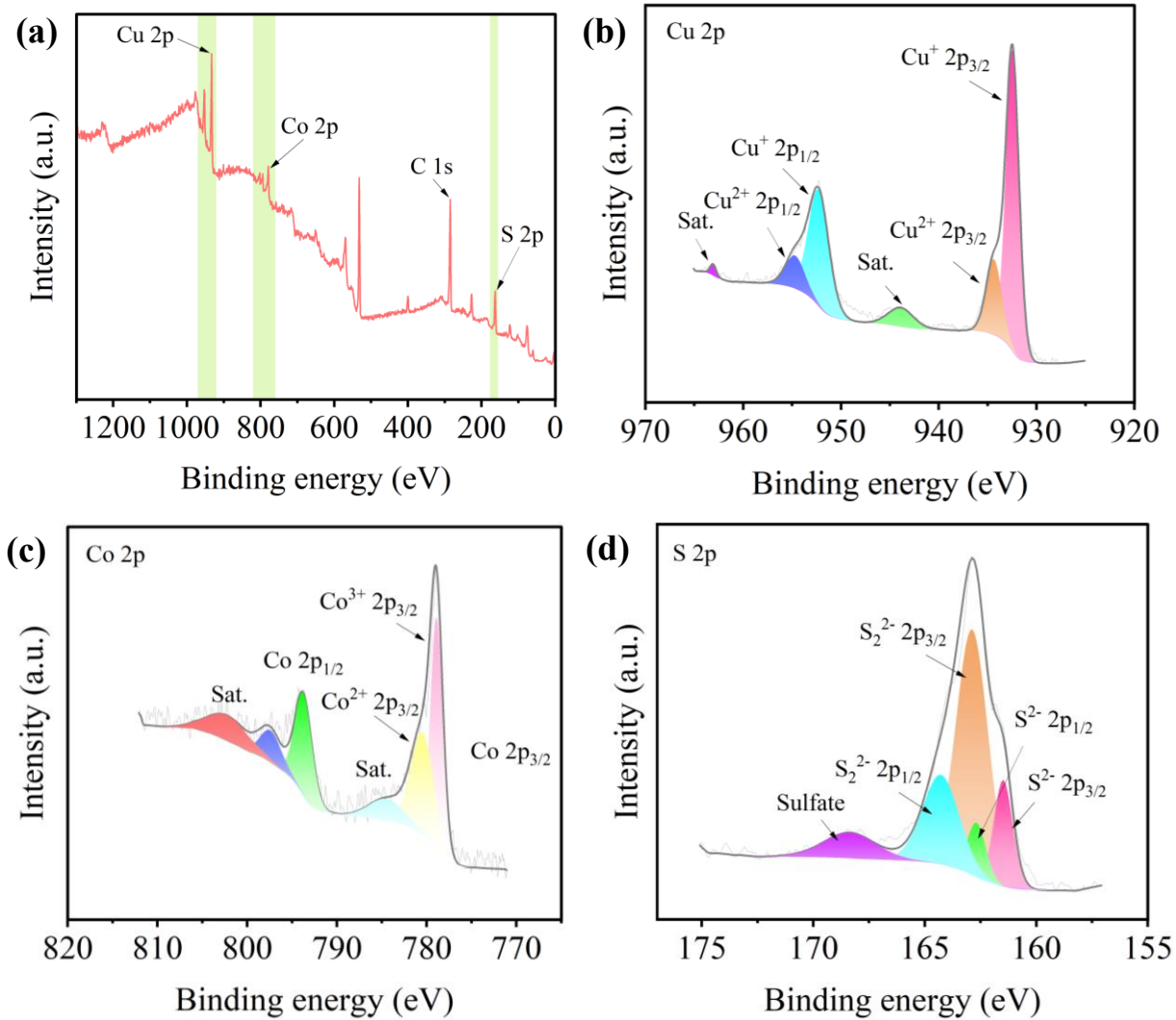
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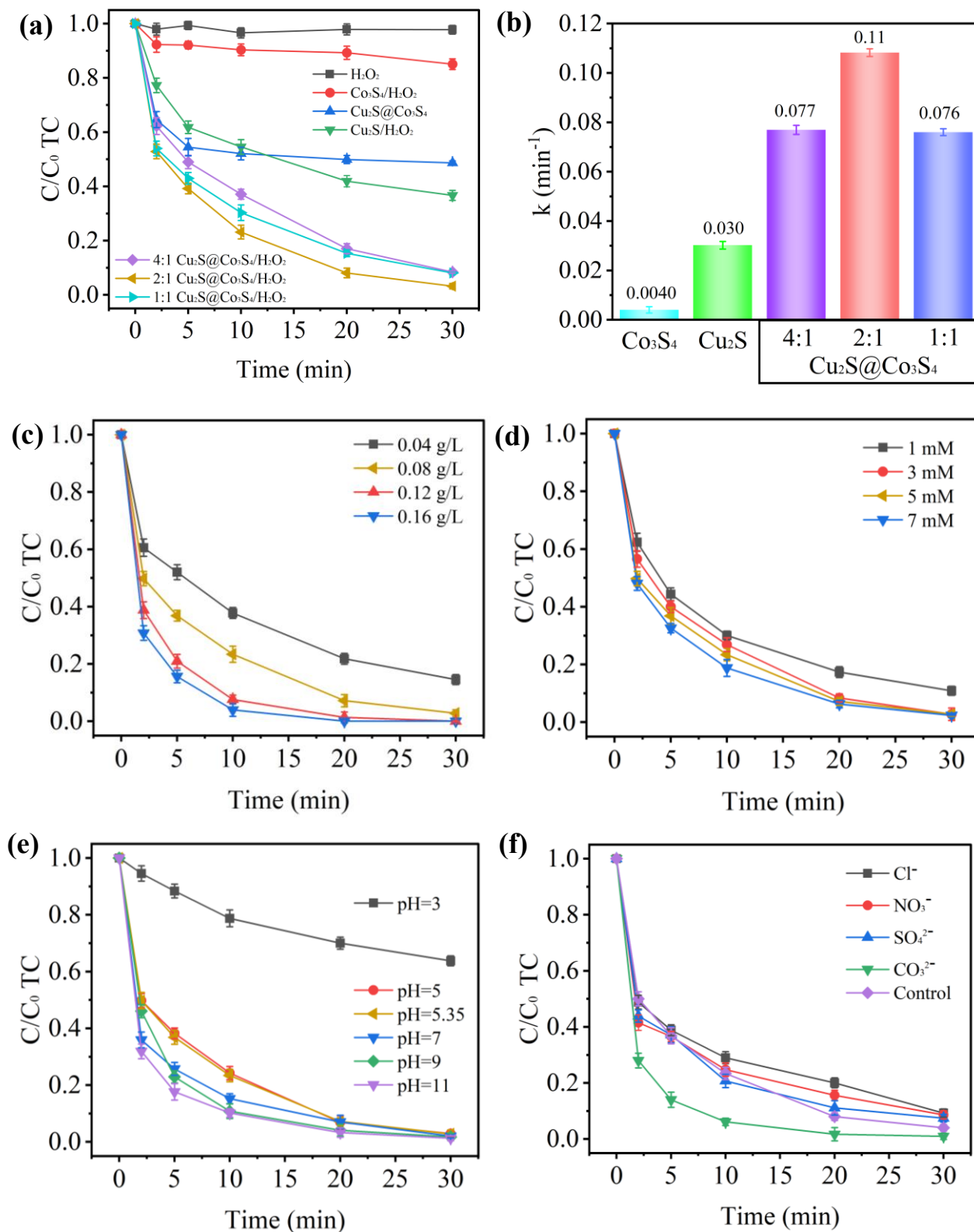
**Scheme 1.** The synthesis route of  $\text{Cu}_2\text{S}@ \text{Co}_3\text{S}_4$



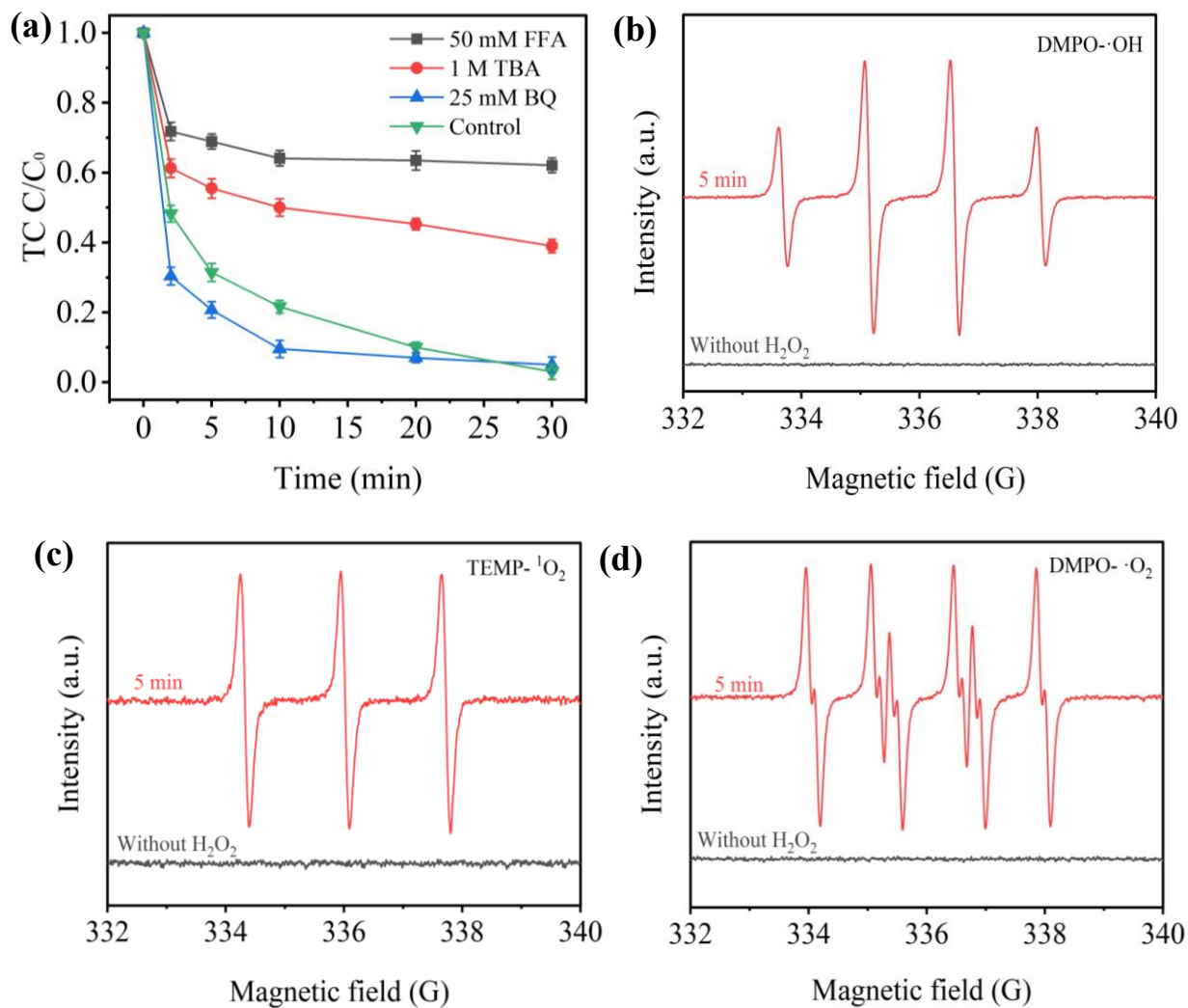
**Figure 1.** SEM images of (a) Cu<sub>2</sub>O and (b) Cu<sub>2</sub>S@Co<sub>3</sub>S<sub>4</sub>; (c) TEM image and (d-f) corresponding EDX mappings of Cu<sub>2</sub>S@Co<sub>3</sub>S<sub>4</sub>; (g) XRD patterns of Cu<sub>2</sub>O; and (h) XRD patterns of Cu<sub>2</sub>S, Co<sub>3</sub>S<sub>4</sub>, and various Cu<sub>2</sub>S@Co<sub>3</sub>S<sub>4</sub> composites.



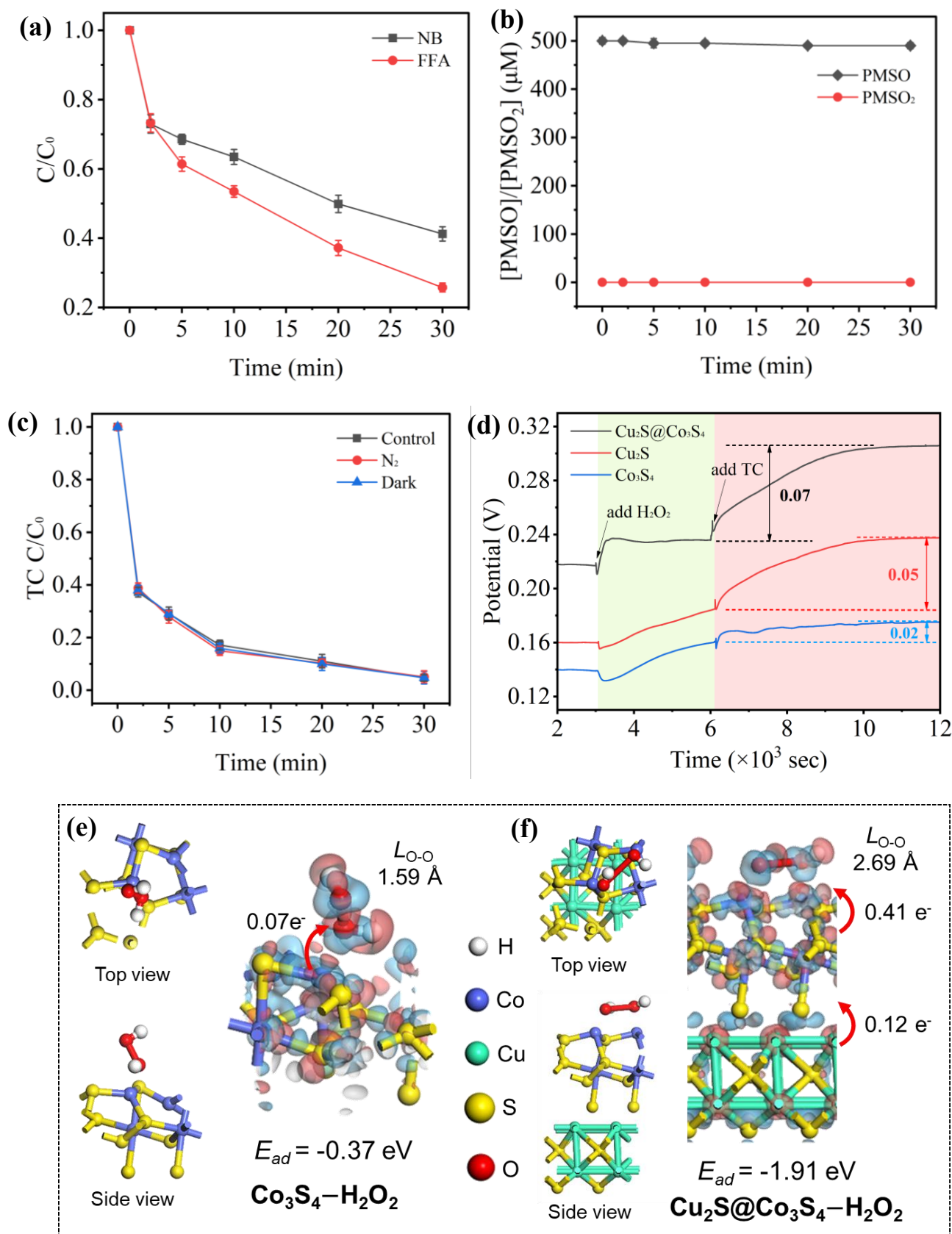
**Figure 2.** (a) XPS survey spectrum of Cu<sub>2</sub>S@Co<sub>3</sub>S<sub>4</sub>; high-resolution XPS spectrum of (b) Cu 2p, (c) Co 2p, (d) S 2p.



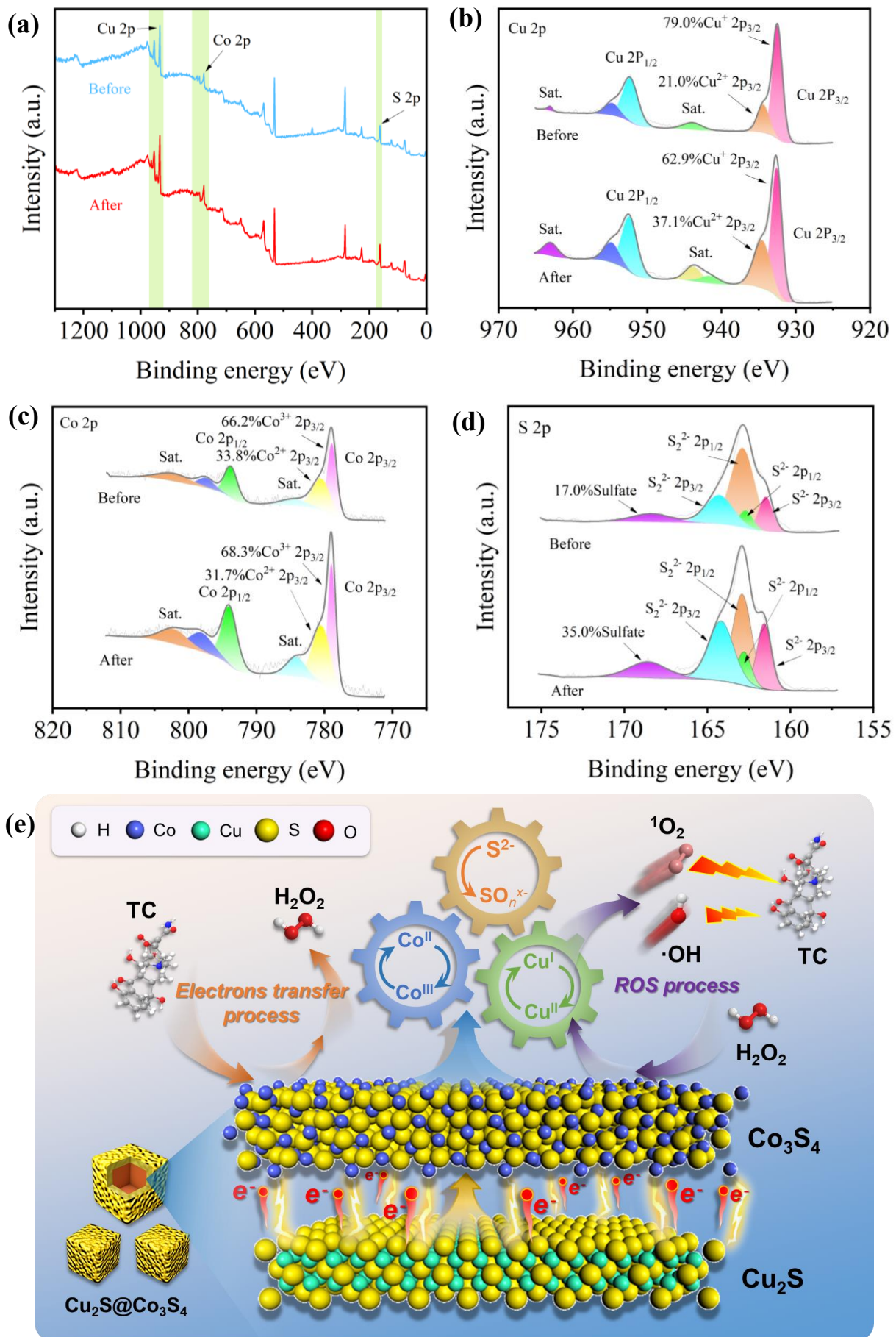
**Figure 3.** (a) Comparison of TC removal in different systems; (b) reaction rate constants achieved by  $Cu_2S$ ,  $Co_3S_4$ , and various  $Cu_2S@Co_3S_4$ ; effects of (c) catalyst dosage, (d)  $H_2O_2$  concentration, (e) initial solution pH, and (f) coexisting ions on TC degradation by the  $Cu_2S@Co_3S_4/H_2O_2$  system. ( $[TC] = 20 \mu M$ ,  $[catalyst] = 0.08 \text{ g/L}$ ,  $[H_2O_2] = 5 \text{ mM}$ ).



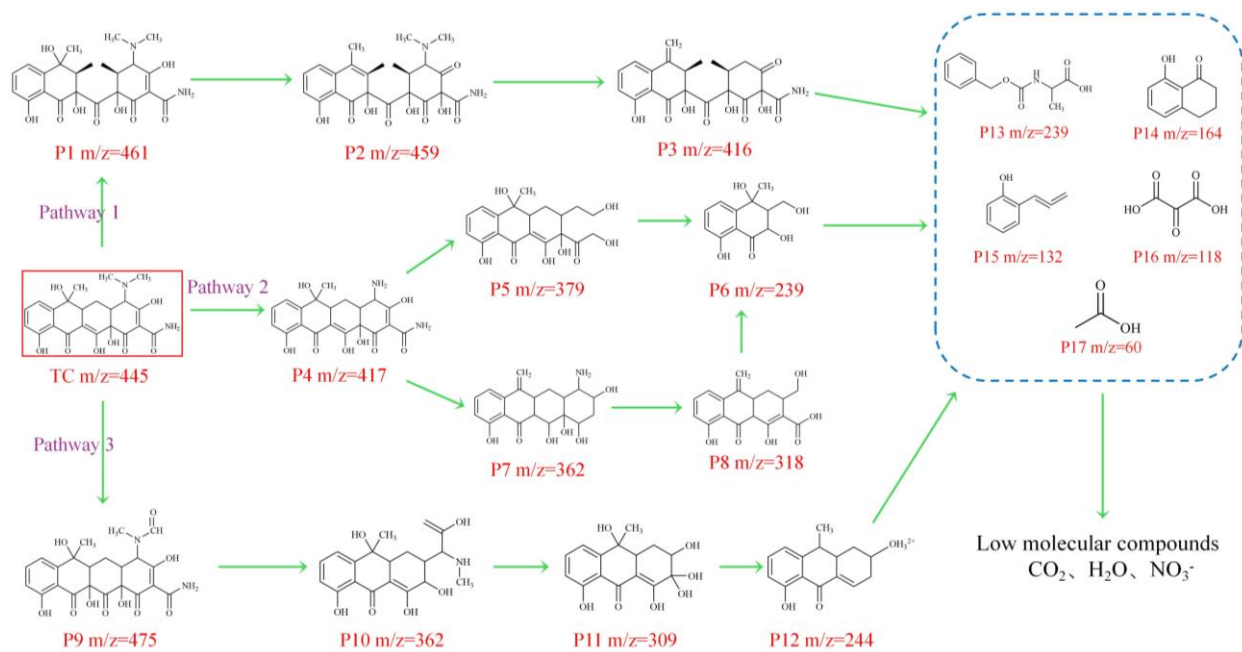
**Figure 4.** (a) Effect of different radical scavengers on the degradation of TC; EPR spectroscopy of (b) DMPO-•OH, (c) TEMP-<sup>1</sup>O<sub>2</sub> and (d) DMPO-•O<sub>2</sub><sup>-</sup>.



**Figure 5.** (a) Degradation effects on different radical trapping agents; (b) PMSO removal in Cu<sub>2</sub>S@Co<sub>3</sub>S<sub>4</sub>/H<sub>2</sub>O<sub>2</sub> system; (c) TC removal in Cu<sub>2</sub>S@Co<sub>3</sub>S<sub>4</sub>/H<sub>2</sub>O<sub>2</sub> system under different conditions. ([TC] = 20  $\mu M$ , [catalyst] = 0.08 g/L, [H<sub>2</sub>O<sub>2</sub>] = 5 mM); (d) The open circuit potential of different systems; The composite structure and differential charge density of (e) Co<sub>3</sub>S<sub>4</sub>-H<sub>2</sub>O<sub>2</sub> and (f) Cu<sub>2</sub>S@Co<sub>3</sub>S<sub>4</sub>-H<sub>2</sub>O<sub>2</sub> (The red and blue areas represent electron depletion and accumulation, respectively).



**Figure 6.** The XPS spectrum of  $\text{Cu}_2\text{S}@ \text{Co}_3\text{S}_4$  before and after reaction: (a) survey, (b) Cu 2p, (c) Co 2p, and (d) S 2p; (e) The proposed  $\text{H}_2\text{O}_2$  activation mechanism in  $\text{Cu}_2\text{S}@ \text{Co}_3\text{S}_4/\text{H}_2\text{O}_2$  system.

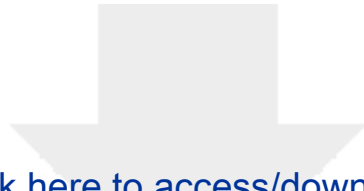


**Figure 7.** Possible degradation pathways of TC by the  $\text{Cu}_2\text{S}@Co_3\text{S}_4/\text{H}_2\text{O}_2$  system.

**Declaration of interests**

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

The authors declare the following financial interests/personal relationships which may be considered as potential competing interests:



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