

This is the preprint version of the contribution published as:

Khomami, N.T.S., Philippe, A., Abu Quba, A.A., Lechtenfeld, O.J., Guigner, J.-M., Heissler, S., Schaumann, G.E. (2020):

Validation of a field deployable reactor for *in situ* formation of NOM-engineered nanoparticle corona

Environ. Sci.-Nano 7 (2), 486 – 500

The publisher's version is available at:

<http://dx.doi.org/10.1039/c9en01090d>

Validation of a field deployable reactor for in-situ formation of NOM-engineered nanoparticles corona

* Corresponding author

Authors: Narjes Tayyebi Sabet Khomami ^a, Allan Philippe ^{a*}, Abd Alaziz Abu Quba ^a, Oliver J. Lechtenfeld ^{b,c}, Jean-Michel Guigner ^d, Stefan Heissler ^e, Gabriele E. Schaumann ^a

^a iES Landau, Institute for Environmental Sciences, Koblenz-Landau University, Fortstrasse 7, 76829 Landau, Germany. ^b UFZ - Helmholtz-Centre for Environmental Research, Department Analytical Chemistry, Research Group BioGeoOmics, 04318 Leipzig, Germany. ^c ProVIS – Centre for Chemical Microscopy, UFZ – Helmholtz-Centre for Environmental Research, 04318 Leipzig, Germany. ^d IMPMC, Sorbonne University, CNRS – UMR 7590, MNHN, Paris, France. ^e Institute of Functional Interfaces IFG, Karlsruhe Institute of Technology KIT, Hermann-von-Helmholtz-Platz 1, D-76344 Eggenstein-Leopoldshafen, Germany.

Abstract

Despite the numerous studies about the sorption of dissolved organic matter (DOM) onto nanoparticles, the extrapolation of laboratory-results to environmental conditions is currently impossible. Indeed, the complex dynamics of DOM under variable environmental conditions are not completely reproducible under control conditions. In this study, we propose a different approach by exploring a method for exposing nanoparticles to realistic environmental conditions in natural river water by using dialysis membranes as passive reactors. Inside this reactor, the complexity and the temporal variability of a large number of environmental parameters (DOM structure and composition, temperature, inorganic ions, pH, etc.) are reproduced, while colloidal and particulate interferences remain separated. To verify this assumption, we determined the concentration of the water components and nanoparticles (n-TiO₂, 20-50 nm) inside and outside the reactor before and after exposure to river water. In river water, more than 90% of the n-TiO₂ remained inside the reactor while DOM retained its molecular composition/characteristics after passing through the membrane (DOC, Fluorescence EEM, FT-ICR MS). For most elements and anions, the concentrations inside and outside the reactor did not differ indicating a good permeability for inorganic constituents (IC, ICP-OES); however, the concentrations of Al, Fe, Mn, and nitrate were lower. Membrane fouling, in terms of pore size distribution, was investigated using NMR relaxometry and AFM in fluid mode; no significant reduction in pore size was observed under the applied conditions during seven days of exposure. Finally, ATR-FTIR and CHNS analysis of n-TiO₂ before and after

31 exposure to the river water revealed that sorption of DOM occurred under field conditions. Therefore, we could
32 demonstrate the validity and the potential of this method.

33

34 **Keywords**

35 Passive reactor, dialysis membrane, n-TiO₂, natural organic matter, NMR relaxometry, AFM, FT-ICR MS

36 **Introduction**

37 For the last 15 years, engineered nanomaterials (ENMs) have attracted growing academic and industrial interests
38 with a wide range of applications in cosmetics, building materials, medicine, and energy storage.¹ Among these
39 materials, titanium dioxide nanoparticles (n-TiO₂) represent the second most important part of ENMs production
40 worldwide (550–5500 t/year) and is expected to increase in the near future.^{2–4} This high production as well as
41 diverse applications leads to inevitable emission of n-TiO₂ into the environment. These nanoparticles can enter
42 aquatic systems either directly or indirectly via wastewater treatment plants or landfills.^{5–7}

43 The fate and biological activity of n-TiO₂ in the aquatic systems depend not only on nanoparticle properties, but
44 also on the characteristics of the receiving water environment including dissolved organic matter (DOM),
45 multivalent cations and natural colloids.⁸ DOM, mainly containing humic substances, polysaccharides, and
46 proteins, represents one of the most dynamic fractions of organic matter in aquatic systems. Depending on the
47 biochemical conditions and concentration in waters, they typically range from 0.1 to 10 mg/L.⁹ Once n-TiO₂ are
48 released into natural systems, interactions of NOM with these nanoparticles will affect their fate, transport, and
49 risk assessments.¹⁰ There are a multitude of studies to understand NOM sorption on titanium dioxide
50 nanoparticles;^{10–17} nonetheless, most of them have been conducted in the laboratory under highly simplified
51 controlled conditions which do not consider, for instance, DOM dynamic structure dependency on water
52 parameters affect the sorption mechanism. Therefore, the results are difficult or even impossible to extrapolate to
53 natural conditions. Hence, there is still a lack of methods allowing a realistic exposure of nanoparticles to
54 temporal environmental conditions including NOM composition, temperature, background electrolyte
55 concentration, and pH for testing hypotheses developed from lab experiments.

56 Passive sampling is an environmental monitoring technique based on free flow of analyte molecules from the
57 sampled medium to a collecting medium as a result of a difference in chemical potentials.^{18–20} The device used
58 for passive sampling is usually membrane dialysis.²⁰ Dialysis is a simple process in which small solutes diffuse
59 from a high concentration solution to a low concentration solution across a semipermeable membrane. There are

60 several studies using dialysis membranes in passive sampling. Vroblecky *et al.* used regenerated cellulose
61 dialysis samplers to measure the volatile organic compounds in different wells.²¹ Vencalek *et al.* applied
62 cellulose ester dialysis bags to separate Cu nanoparticles from the dissolved Cu species in freshwater
63 mesocosms.²² Benes *et al.* determined the state of trace elements in natural waters using cellulose membrane.²³

64 In this study, we present the first steps of the evaluation of a realistic river water exposure method for n-TiO₂
65 inspired from the concept of passive sampling. n-TiO₂ nanoparticles were selected to test the method since they
66 do not dissolve in water and the sorption of DOM components on these nanoparticles is well studied.^{24,25} The
67 proposed method relies on membrane dialysis, i.e. the dialysis bag considered as a passive reactor retaining n-
68 TiO₂ nanoparticles inside while DOM can diffuse inside. Furthermore, the natural colloids cannot enter which
69 simplifies the extraction of the nanoparticle after exposure. In order to apply this method to environmental
70 waters, the membrane needs to meet several requirements:

- 71 • Retaining nanoparticles, permeable to non-colloidal water components (suitable molecular weight cut-
72 off of the membrane).
- 73 • Robustness towards environmental variation (pH, temperature, water flow, aquatic organisms).
- 74 • The permeability of the membrane should remain constant during the exposure. Fouling is the principal
75 mechanism affecting the permeability under environmental conditions.^{26,27}

76 In order to assess these issues, we exposed the dialysis bags (for improved readability, we will refer to “dialysis
77 bag” for denoting the passive reactor) in river water and determined the concentration of the main organic and
78 inorganic components inside and outside. Furthermore, we investigated the pore structure before and after
79 exposure using NMR relaxometry and AFM in fluid mode.

80 Finally, we carried out a field exposure of n-TiO₂ in a river and evaluated the sorption of DOM of the river water
81 onto n-TiO₂ by characterizing nanoparticles before and after river exposure using ATR-FTIR and CHNS
82 analyses. The results present the proof-of-concept of using dialysis bags and the validity of implementing this
83 method to study the interactions of NOM and engineered nanoparticles under real environmental conditions.

84

85 **Material and methods**

86 *Material*

87 Biotech Cellulose ester (CE) Membranes with three different molecular weight cut off (20, 100, and 300 kDa)
 88 were purchased from Repligen (Formerly Spectrum). The specifications provided by the supplier can be found in
 89 **Table 1**. Before usage, the membranes were soaked first in 10% (v/v) ethanol-water for 10 minutes, rinsed with
 90 distilled water (DW) and soaked in DW for removing glycerin and achieve maximum membrane permeability.²⁸
 91 The membranes were stored in DW until further usage. Pre-experiments with dialysis bags using clip type
 92 closure resulted in the loss of 50% of the deployed dialysis bags, damaged under the movement induced by the
 93 river flow (30-40 cm/s, OTT MF pro, Germany). Therefore, cylindrical dialysis bags with screw-on caps
 94 showing 100% resistance over one week were selected for this study (**Figure S1**). Aeroxide® n-TiO₂ P25
 95 powder was purchased from Degussa, Germany.

96

97 **Table 1** specifications of the dialysis bag

specifications	Membrane type	Physical Appearance	Packaging	pH limit	Temperature limit	Total Length	Membrane Diameter
	Float-A-Lyzer® Cellulose Ester (CE)	Opaque, Rigid	Dry with glycerine	2-9	4-37 °C	10 cm	10 mm

98

99 *HR-TEM (n-TiO₂)*

100 For nanoparticles characterization, 5 µL of 1 g/L n-TiO₂ suspension was placed on a TEM grid and dried at
 101 ambient conditions. Transmission Electron Microscopy (TEM) measurements were performed using a JEOL
 102 2100F (JEOL Ltd., Tokyo, Japan), field emission gun instrument operating at 200 kV equipped with a polar
 103 piece ultra-high resolution. Images were recorded on an UltraScan 4000 Gatan (Gatan Inc., Pleasanton, CA,
 104 United States) camera with a 4k × 4k pixels CCD.

105 *Sampling and characterization of the river water*

106 The experiments were conducted with water collected from the River Queich (latitude: 49.205510, longitude:
 107 8.088081) in Landau in der Pfalz, Germany in May-September 2018 (In case of a complementary experiment,
 108 the date is mentioned). For the sake of simplicity we will refer to “river water” for denoting the water sampled at
 109 this place. The characteristics of the river water were fairly stable over this period of time (**Table S1**).

110 Samples were collected in a polypropylene canister at 1 m from the river bank. The pH was measured on site
111 (SG2-FK SevenGo, Mettler Toledo, Schwerzenbach, Switzerland). The samples were transported immediately to
112 the nearly located laboratory, and were stored in the dark at 4 °C. Multi-parameter analyser (Consort C863,
113 Turnhout, Belgium) was used to measure electrical conductivity. Dissolved organic carbon (DOC) concentration
114 was determined after filtration with 0.45 µm PTFE filters (Altmann, Germany) using a TOC analyzer (multi N/C
115 2100, Analytik Jena AG, Jena, Germany). The concentrations of Al, Ba, Ca, Cu, Fe, K, Mg, Mn, Na, Sr, and Zn
116 the river water samples were measured using inductively coupled plasma optical emission spectroscopy (ICP-
117 OES, 720, Agilent Technologies, Santa Clara, USA). Digestion procedure for determination was done similar to
118 the literature with some modifications. ⁵ 10 mL of the river water was dried at 95 °C, cooled down at room
119 temperature before adding 2.5 mL of hydrogen peroxide (30 %, Rotipuran®, Carl Roth, Germany). After 10
120 min standing at room temperature, 5 mL of sulfuric acid (95 %, Rotipuran®, Carl Roth, Germany) was added
121 dropwise before being progressively heated until ebullition (225°C). After one hour at 225°C, the samples were
122 cooled down at room temperature and diluted into a 100 mL volumetric flask prior to ICP-OES analysis. All
123 samples were measured in triplicates. Ion chromatography (Professional IC 881 Metrohm) was used to analyze
124 anions. Dissolved oxygen was measured using PyroScience Optical Oxygen Sensor. The chemical and physical
125 information of the river summarized in the supporting materials **Tables S1-3**.

126 *Permeability of dialysis bags toward n-TiO₂*

127 To check the permeability of dialysis bags for the nanoparticles used in this study, a 300 mg/L suspension of n-
128 TiO₂ was prepared and sonicated (ultrasound bath) for 10 minutes. The dialysis bags were filled with 5 ml of n-
129 TiO₂ suspension, and placed in a 50 ml polypropylene centrifuge tube filled with 35 ml river water. The tubes
130 were shaken at 200 rpm using a horizontal shaker for a specified time. Samples were collected from outside of
131 the dialysis bags, prior to Ti-content determination using ICP-OES. The samples were digested following
132 Philippe et al. ⁵ The ICP-OES measurements were carried out for Ti at an emission wavelength of 334.941 nm.
133 All samples were measured in triplicates.

134 *Determination of the equilibrium time*

135 The dialysis bags were filled with 5 ml distilled water, and placed into a 50 ml polypropylene centrifuge tube
136 filled with 35 ml river water. The tubes were shaken at 200 rpm using a horizontal shaker at room temperature
137 (21 °C). After the specified time, samples were collected from inside and outside of the dialysis bags, filtered
138 using 0.45 µm PTFE (Altmann, Germany), and analyzed for TOC.

139 *NMR relaxometry*

140 The transverse relaxation time (T_2) in ^1H NMR relaxometry measures the decay of magnetization of proton spins
141 after excitation from their dephasing in time-dependent fluctuation of the magnetic field caused by adjacent
142 nuclei (T_2).²⁹ Thus, T_2 distribution can be related to the pore size distribution with lower T_2 corresponding to
143 water present in small pores while larger T_2 correspond to large pores as well as “free” bulk water. Cellulose
144 compounds (dialysis bag) depict recognizable bimodal T_2 distribution,³⁰ which was also observed for the
145 cellulose ester membrane of the dialysis bag and represent the hierarchical porous structure of the membrane.
146 For measuring the spin-spin relaxation time (T_2) of dialysis bags in different media (distilled water, river water
147 with and without $n\text{-TiO}_2$), the dialysis bags were completely emptied and measured immediately to avoid drying
148 of the membrane. All samples were measured in triplicates. A Bruker Minispec MQ, Version 2.2 (Bruker,
149 Karlsruhe, Germany) was used at a magnetic field strength of 0.176T (proton Larmor frequency of 7.5MHz);
150 applying 64 scans, with the recycled delay of 10 s. The gain was adjusted for each sample individually such that
151 70–80% signal intensity was achieved. Calculations and figures were done using Matlab R2014 a, and Origin
152 7.5.³¹

153 *AFM*

154 The dialysis bags were cut to approximately $2 * 1 \text{ cm}^2$ pieces. They were fixed on a steel-disc using instant glue,
155 and stored in distilled water, or river water until measurement. The atomic force microscopy (AFM, Dimension
156 Icon, Bruker Corporation, USA) analyses were conducted using tapping mode in water media, with New Sharp
157 Nitride Lever tips (SNL, Bruker, USA) with a radius of 2 nm (nominal value). Sample mounting for AFM fluid
158 experiments along with the probe calibration procedures were performed as recommended in the Bruker
159 protocols.^{32,33} To measure the pore size of the dialysis bag, images were captured from six random locations and
160 further processed for pore size estimation (ImageJ). The pores area was determined automatically after
161 black/white picture conversion and contrast adjustment. The obtained areas were used to determine a
162 hydrodynamic diameter for each pore (also known as pore thickness or opening diameter) defined as the
163 diameter of the largest circle inscribed in a pore following the equation (1):

164 (1)

165 where A (area) equals the total number of pixels enclosed by the pore boundary, and P (perimeter) is the number
166 of pixels on the boundary. The results of the six regions of interest were combined to have a set of representative
167 data. Analysis of the images and corresponding calculations were carried out using the program ImageJ v1.52a.
168 and Origin 7.5.

169 *Field exposure experiment*

170 To avoid the damage of dialysis bags by the stream flow of the river or the aquatic animals, each dialysis bag
171 was enclosed in a perforated polyethylene plastic canister (approximate perforation diameter: 0.3 mm). The
172 dialysis bags were filled by 5 ml distilled water (control), or a freshly prepared and sonicated (10 minutes in an
173 ultrasound bath) n-TiO₂ 300 mg/L suspension (three replicates), and placed in the canister (**Figure S2**). The
174 canisters were fixed to an anchor and immersed in the river about 1 m from the river bank. After a week, the
175 content of the dialysis bags was collected in a 15 mL polypropylene centrifuge tube and immediately transferred
176 to the laboratory for further analyses. It is worth mentioning, the realistic concentration of n-TiO₂ in surface
177 waters is low (e.g. 0.55-16 µg/L).³⁴ However, the majority of current analytical techniques used for sorption
178 studies are not capable of working with concentrations in µg/L range; therefore, the applied n-TiO₂ concentration
179 (300 mg/L) was way too higher than the realistic ones. Nonetheless, in the field experiment, there is a large
180 excess of available DOM for nanoparticles; hence, high concentration of n-TiO₂ (300 mg/L) inside the bags is
181 not changing the ratio of sorbate/sorbent significantly.

182

183 *Fluorescence spectroscopy*

184 The collected river water samples were centrifuged (Universal 320, Hettisch, Bäch, Switzerland) at 4500 rpm
185 (3283 g) for 30 min. Since the n-TiO₂ nanoparticles were visibly agglomerated, this speed was sufficient to
186 collect them at the bottom and the supernatant was transparent under this condition. The supernatant was taken
187 for further measurements. Fluorescence Excitation/emission matrix (EEM) of the samples were recorded on a
188 PerkinElmer LS 55 Fluorescence spectrometer in the emission (Em) range of 200-700 nm by varying the
189 excitation (Ex) wavelength from 250 to 450 nm in 20 nm increments with a scan rate of 1200 nm/ min.
190 Excitation and emission slits were both 10 nm. Since a linear calibration curves (fluorescence intensity versus
191 fluorophore concentrations, $R^2 = 0.9991$) was obtained after serial dilutions of the river water, we considered the
192 filter effects as negligible for this river sample. No corrections for scattering effects were applied to the data as
193 there were no observable overlapping of the fluorescence and scattering peaks. The EEM spectra were plotted
194 using Origin 7.5.

195 *CHNS*

196 For each measurement of river water, 250 ml of the river water was filtered with 0.45 μm PTFE filters
197 (Altmann, Germany), and freeze-dried (Christ, Osterode, Germany) for two continuous days at $-40\text{ }^{\circ}\text{C}$ and 0.12
198 mbar and two more days at $-60\text{ }^{\circ}\text{C}$ and 0.011 mbar. TiO_2 nanoparticles exposed to the river water were
199 centrifuged at 4500 rpm (3283 g) for 30 min. The supernatant was withdrawn carefully to the last drop and the
200 centrifugate was freeze dried as described above. For CHNS elemental analysis, 4-15 mg of samples were
201 weighed into tin boats (LabNeed GmbH, Nidderau, Germany) together with around 20 mg of WO_3 powder
202 (LabNeed GmbH, Nidderau, Germany), and measured using CHNS varioMicroCUBE (Elementar,
203 Langensfeld, Germany). Sulfanilamide (Elementar GmbH, Langensfeld, Germany) was used as a reference
204 sample. Computation of the Euclidian distances was carried out using the program R Studio (Version 1.0.143).

205 *ATR-FTIR*

206 The nanoparticle pellet collected after centrifugation and also the river water sample collected on the last day of
207 field experiment were freeze-dried as for CHNS. For ATR-FTIR measurements, a Bruker Tensor 27 IR
208 spectrometer (Bruker Optics, Ettlingen, Germany) with a Bruker Platinum ATR accessory, single reflectance
209 diamond crystal, 45° angle of incidence, was used. Some milligrams of the samples were applied directly on the
210 ATR-crystal. Spectra were measured against an air background. Each spectrum comprised 32 coadded scans
211 with a spectral resolution of 4 cm^{-1} in the $3600\text{--}370\text{ cm}^{-1}$ range. The absorption spectra were depicted using
212 Origin 7.5 software.

213 *FT-ICR-MS sample preparation and measurement*

214 River water samples (5 mL) were extracted via solid-phase extraction using an automated sample preparation
215 system (FreeStyle, LC Tech) on 50 mg styrene-divinyl-polymer type sorbents (Bond Elut PPL, Agilent
216 Technologies) to desalt the sample for subsequent DI-ESI-MS according to Raeke et al.³⁵. The SPE-DOM was
217 eluted with 1 mL methanol (Biosolv), diluted to 20 ppm and mixed 1:1 (v/v) with ultrapure water immediately
218 prior FT-ICR MS analysis. Carbon based extraction efficiency was approx. 50% (for river water). SRFA
219 measured in triplicate was used to check instrument variability and solvent and extraction blanks were prepared.

220 An FT-ICR mass spectrometer equipped with a dynamically harmonized analyzer cell (solariX XR, Bruker
221 Daltonics Inc., Billerica, MA) and a 12 T refrigerated actively shielded superconducting magnet (Bruker
222 Biospin, Wissembourg, France) instrument was used in ESI negative ionization mode (capillary voltage: 4.3
223 kV). Extracts were analyzed in random order with an autosampler (infusion rate: $10\text{ }\mu\text{L min}^{-1}$). For each
224 spectrum, 256 scans were co-added in the mass range 150–3000 m/z with 25 ms ion accumulation time and 4

225 MW time domain (resolution@400 m/z ca. 500 000). Mass spectra were internally linear calibrated with a list of
226 peaks (250-600 m/z, n > 143) commonly present in terrestrial DOM and the mass accuracy after calibration was
227 better than 0.13 ppm. Peaks were considered if the signal/noise (S/N) ratio was greater than four.

228 *FT-ICR-MS data evaluation*

229 Molecular formulas were assigned to peaks in the range 150-750 m/z allowing for elemental compositions C₁₋₆₀
230 ¹³C₀₋₁ H₁₋₁₂₂ O₁₋₄₀ N₀₋₂ S₀₋₁ ³⁴S₀₋₁ with an error range of ±0.5 ppm according to Lechtenfeld et al.³⁶ Briefly, the
231 following rules were applied: 0.3 ≤ H/C ≤ 2.5, 0 ≤ O/C ≤ 1.0, 0 ≤ N/C ≤ 1.5, 0 ≤ DBE ≤ 20 (double bond
232 equivalent, DBE = 1+1/2 (2C-H+N), Koch et al.³⁷), 8 ≤ DBE-O ≤ 8 (Herzprung et al.^{38,39}), and element
233 probability rules proposed by Kind and Fiehn⁴⁰. Isotope formulas were used for quality control but removed
234 from the final data set as they represent duplicate chemical information. All molecular formulas present in the
235 medium blank or instrument blank samples were excluded from the peak lists. 4668 - 5022 formulas were
236 assigned with no multiple assignments to 16568 - 17423 peaks above noise level). Molecular formulas and
237 compounds are used synonymously throughout the text, although no molecular structures are known.

238 Relative peak intensities were calculated based on the summed intensities of all assigned monoisotopic peaks in
239 each sample. Van Krevelen diagrams for river water samples inside and outside the dialysis bags were used to
240 depict differences in relative intensities (ΔRI) for each individual molecular formula according to Equation 2.⁴¹

241 (2)

242 where *sample* refers to the water inside the bag (with n-TiO₂) and *reference* is the water outside the bag (river
243 water). To test the effect of instrumental variability on the ΔRI values six SRFA samples (Suwannee River
244 Fulvic Acid) were measured on the same day. Relative standard deviations (RSD) were calculated from the
245 normalized intensities for each molecular formula. The 95 percentile of the RSD values were used as threshold
246 and any change in normalized peak intensity among different samples above this percent value is considered as
247 statistical significant difference (**Figure S3**). ΔRI values corresponding to the RSD threshold were calculated
248 (ΔRI < 0.43; ΔRI > 0.57). In the following, ΔRI values above 0.57 were considered to indicate that the
249 respective compound is enriched in the sample, and ΔRI values below 0.43 indicates the respective compound is
250 enriched in the reference.

251

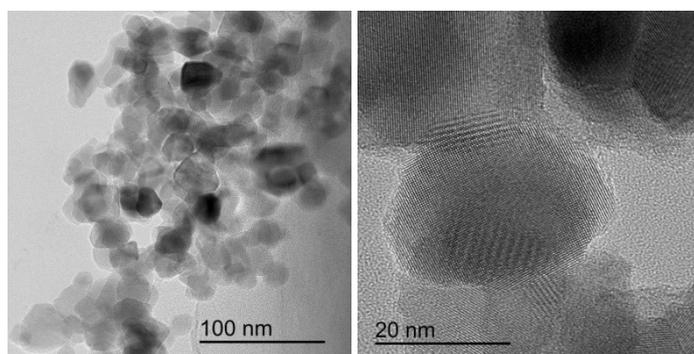
252 **Results and discussion**

253 *Permeability of the membrane*

254 The selection of an appropriate dialysis membrane is essential for exposing nanoparticles to DOM under field
255 conditions. In particular, the molecular weight cut-off (MWCO) should be high enough for the dissolved
256 components of natural water to diffuse freely through the membrane, to simulate the river composition to a good
257 extent inside the dialysis bag. On the other side, the membrane should not be permeable towards nanoparticles,
258 in this study represented by n-TiO₂.

259 **Figure 1** shows the HR-TEM image of pristine n-TiO₂ with diameters in the range of 20-50 nm. Hence, the
260 average pore size of the applied dialysis bag should be significantly lower than 20 nm to retain the nanoparticles.
261 Symmetrically, the natural colloids larger than the membrane pore size will not permeate through the membrane,
262 thus simplifying the analytical procedure for the subsequent surface analysis of the DOM-coated nanoparticles.

263



264

265 **Figure 1:** HR-TEM images of pristine n-TiO₂.

266

267 **Table 2** shows the retention rate of n-TiO₂ depending on the MWCO (20, 100, 300 kDa) after two and seven
268 days exposure. The initial Ti-content of river water was below the detection limit of the ICP-OES (**Table S2**).
269 The retention rates were all higher than 90% . High retention values are expected considering the smallest size of
270 n-TiO₂ (20-50 nm) compared to the pore size of the membranes (5-20 nm). Furthermore, n-TiO₂ nanoparticles
271 were agglomerating in the river water due to the almost neutral pH (close to the isoelectric point of P25)⁴² and
272 the presence of different ions.²⁴ Therefore, the non-permeability of the membrane to nanoparticles can be
273 improved when the nanoparticles are agglomerating in the natural water. Hence, the colloidal stability in natural
274 water has to be considered in the choice of the membrane cut-off in addition to the size of primary particles.

275

276 **Table 2:** retention rate in % of n-TiO₂ inside the dialysis bags after 2 and 7 days incubation in river water

Days	Retention rate in %		
	20 kDa (~ 5nm) ¹	100 kDa (~ 10nm) ¹	300 kDa (~ 20nm) ¹

2	92.9 (± 3.6) ²	93.8 (± 4.2) ²	92.4 (± 5.3) ²
7	92.8 (± 5.4) ²	92.8 (± 3.1) ²	90.6 (± 8.3) ²

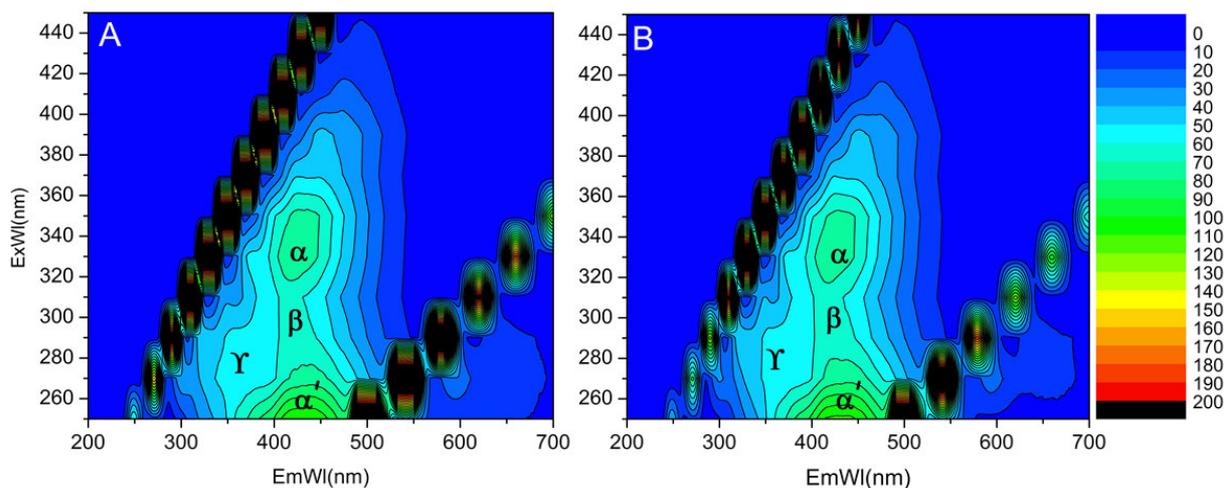
277 ¹ There is no direct correlation between pore dimension (nm), and the molecular size cut-off (kDa); however, the
 278 manufacturer provides some approximations. ²⁸

279 ² Standard deviation

280

281 Permeability of the membrane to dissolved organic matter (DOM) via free diffusion was evaluated using three-
 282 dimensional excitation-emission-matrix fluorescence spectroscopy (EEM). Four typical excitation/emission
 283 peaks have been observed in surface waters: ⁴³ α (Ex/Em \sim 340/420), α' (Ex/Em \sim 250/430), β (as a shoulder on
 284 the α peak Ex/Em \sim 300/420), and γ (Ex/Em \sim 280/350). Among them, α , and α' have been attributed to the
 285 carboxylic and phenolic groups, respectively, ¹⁶ β to weakly humified structures, simple phenols, coumarins and
 286 alkaloids, ⁴⁴ and γ to proteins. ⁴⁵ **Figure 2** depicts the EEM fluorescence map of the river water inside and
 287 outside of the dialysis bag (100 kDa) exposed to river water for 1 week. The similarity of the signals suggest that
 288 The DOM fluorophores are similar in terms of quantity and quality, therefore, the membrane is probably
 289 permeable to most part of DOM, including proteins (similar γ signals). These results suggest that a cut-off of
 290 100 kDa is large enough for DOM in natural water to permeate. Since we kept the possibility to apply the present
 291 method to particles smaller than 20 nm but larger than 10 nm such as some n-TiO₂ found in sunscreens ⁵ and
 292 avoid the presence of small natural colloids with the DOM-coated n-TiO₂, 100 kDa was selected for further
 293 optimization.

294



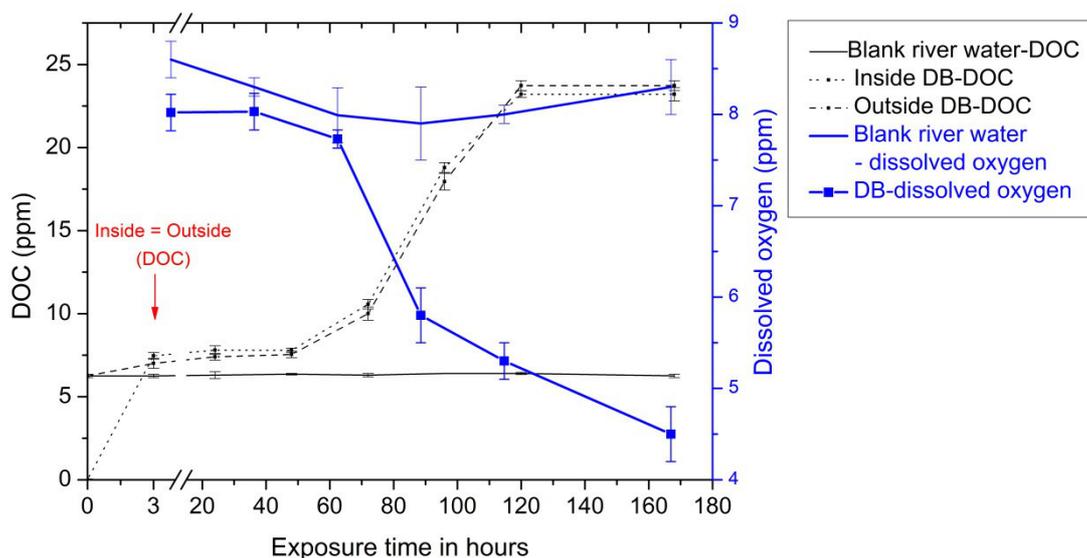
295

296 **Figure 2:** Fluorescence EEMs of A) inside and B) outside of the dialysis bag after one week of exposure to river
 297 water in the lab (the color scale depicts the intensity).

298

299 The exposure time of the dialysis bags to the river water is another important factor to optimize. On one hand,
300 this time should be long enough to reach the equilibrium of DOM between inside and outside of the dialysis bags
301 and to allow sufficient reaction time for nanoparticles; on the other hand, it should be short enough not to cause
302 the decomposition of the membrane (chemical- and bio-degradation) in the river water. The optimal exposure
303 time depends on the molecular cut-off and on the environmental conditions. **Figure 3** (left axis) shows the
304 dissolved organic carbon (DOC) of the river sample (DOC around 6.5 ppm) inside and outside of a dialysis bags
305 initially filled with distilled water over one week under laboratory conditions. The initial DOC inside the dialysis
306 bag was zero. Over time, the DOC inside dialysis bag increased due to free diffusion of DOM from river water
307 toward inside the dialysis bag. By three hours, the measured DOC inside and outside of the dialysis bag became
308 similar and remained stable indicating that the system reached equilibrium in less than 3 h and up to 48 h. The
309 difference between the DOC in the blank river water and with dialysis (about 13%) is probably due to organic
310 leaching of the membrane and the closures.⁴⁶ This problem is not of relevance under field conditions since the
311 volume of the water outside the bag is nearly infinite compared to the volume inside the membrane. Thus, the
312 organic leaching cannot accumulate significantly near the bag.

313



314

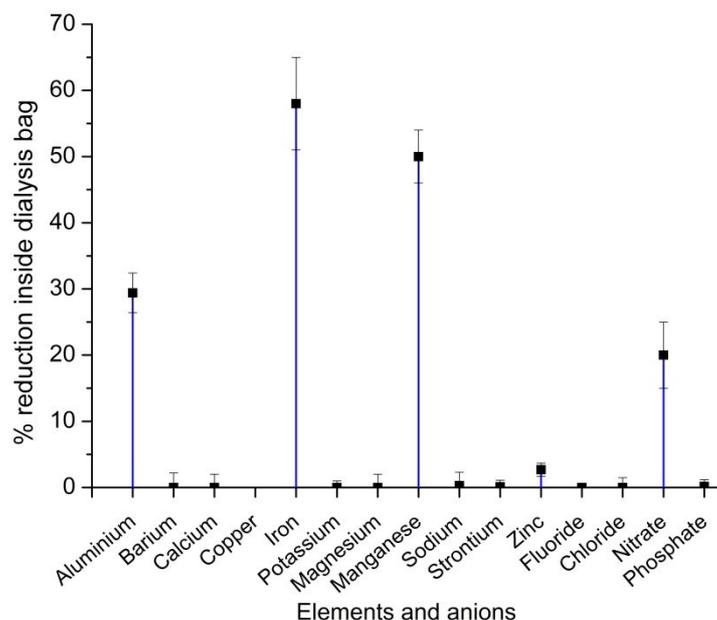
315 **Figure 3:** DOC (left axis), and dissolved oxygen (right axis) of the river water inside and outside dialysis bags
316 (DB) initially filled with distilled water and immersed in river water at room temperature (Error bars depict
317 standard deviation).

318 After 48h, there is a large increase in DOC concentration inside and outside the dialysis bag. This increase is
319 most probably due to microbial activity leading to membrane decomposition ⁴⁷ as suggested by the parallel
320 decrease in dissolved oxygen (**Figure 3, right axis**). ⁴⁸ Since the parallel increase in DOC, and decrease in
321 dissolved oxygen were not observed in the blank river water, the dialysis bag is most probably the actual
322 substrate for the microbial development under conditions causing the membrane to decompose over time. In
323 order to overcome this drawback for studies requiring exposure times longer than 48h, we suggest modifying
324 dialysis membranes to suppress microbial proliferation by using antibacterial agents in the membrane ⁴⁷ or
325 applying more robust membranes to microbial activity such as PVDF.

326 It has to be noted that, under different conditions (e.g. higher temperatures, high concentrations of nutrient, etc.),
327 the decomposition of the membrane can be significantly faster. Therefore, we recommend keeping the exposure
328 time as low as necessary for the equilibration of the DOC concentration inside the bag, while covering the
329 relevant variations of environmental factors (e.g. day and night conditions) to be studied.

330 In addition to DOC and nanoparticles, the ability of inorganic ions to diffuse through the membrane was tested
331 with river water under laboratory conditions after one week of exposure to river water. At room temperature, the
332 pH remains stable inside and outside of the dialysis bag (pH = 7.2). However, the conductivity reduced about
333 55% inside the bag. This can be due the discrimination of some ions during the permeation or to bacterial
334 growth. ⁴⁹ To identify the source of this discrepancy we determined the total concentration of a selection of the
335 most common elements in surface waters inside and outside the dialysis bag using ICP-OES. For most monitored
336 elements, the equilibrium could be reached resulting in similar concentrations inside and outside the dialysis
337 bags (**Figure 4**). Notable exceptions are Al, Fe, and Mn whose total concentrations inside the bag decreased
338 more compared to other elements (30-60%). This is probably due to their high valencies when present as ions
339 (Al: +3, Fe: +2 and +3, Mn: +2,+4, and +7), which increases the probability to interact with the cellulose ester
340 membrane. ⁵⁰ On the other hand, these elements have been often observed as particulate matter, colloidal or not,
341 in surface waters, ^{51,52} which would drastically reduce their ability to diffuse through the membrane.

342



343

344 **Figure 4:** The percentage of reduction of elements and anions by passing through the dialysis bags (compared to
 345 outside). Error bars depict standard deviation.

346 A complete equilibrium was reached for anion concentrations, as observed for the elements, except for nitrate
 347 with 20 % reduction (**Figure 4**). The highest reduction observed for nitrate can be due to the nitrate reduction
 348 caused by the microbial activity on the substrate of the dialysis bag after one week of exposure to river water.⁵³
 349 Therefore, the observed decrease in conductivity can be partly due to a lower amount of natural colloids carrying
 350 charges and to lower nitrate concentration related to microbial activity, whereas other factors involving microbial
 351 activity cannot be ruled out.

352

353 *Membrane fouling*

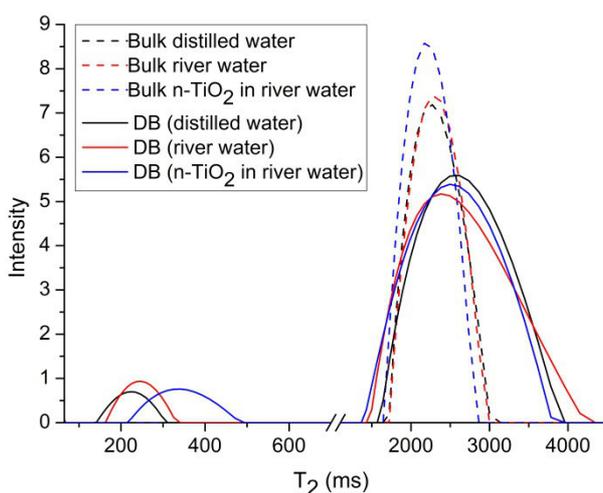
354 Membrane fouling occurs when biotic or abiotic materials obstruct pores, thus reducing the permeability of the
 355 membrane. Fouling in natural waters, with a complex mixture of particulate and dissolved components, is one of
 356 the important processes reducing the permeability of membranes by reducing the pore size of the membrane.⁵⁴
 357 Since drying of the membrane reduces drastically the pore size of dialysis membranes,⁵⁵ we determined the pore
 358 size of the membranes used for DOM exposure using NMR relaxometry and AFM under wet conditions.^{56,57}
 359 NMR relaxometry enables an in situ estimation of a pore size distribution averaged over the whole sample, while
 360 AFM enables imaging of the pore system at some selected spots at the surface of the membrane. Therefore, the
 361 combination of these two complementary methods is highly valuable for obtaining information of the pore size
 362 under wet conditions.

363 *Pore size distribution measured by NMR relaxometry*

364 To investigate the probable effect of water medium (e.g. cations) on spin-spin relaxation time (T_2), bulk water
365 media (distilled water, and river water with and without n-TiO₂) were firstly measured (**Figure 5 - dash lines**).
366 There was no significant difference (t-test, 95%) in terms of T_2 distribution modes among the bulk media;
367 therefore, the T_2 of water-filled pores was independent of the medium itself.

368 **Figure 5** (solid lines) depicts the T_2 measurements of water-filled pores of the dialysis bags in three different
369 water media (distilled water, river water with and without n-TiO₂). In contrast to bulk water samples, the T_2
370 distributions of dialysis membrane samples depict two distinguished T_2 peaks representing the hierarchical
371 structure in applied dialysis bags (cellulose ester).^{30,58} Since the characteristic pore size of the membrane (r) and
372 the T_2 of water-filled pores are proportional,³⁰ the larger T_2 (around 2000-3000 ms) indicates the slower
373 relaxation and a larger pores, and smaller T_2 (200-300 ms) indicates faster relaxation and smaller pores. In
374 addition, the larger T_2 distribution is the result of a mixed contribution between the water molecules absorbed on
375 the surface of the membrane and free state; both states merge into one peak in the NMR relaxation spectra.³⁰

376 Based on t-test, we did not observe any significant difference in the T_2 distributions of dialysis membranes in
377 different water media (distilled water, river water with and without n-TiO₂). This suggests that, under the applied
378 conditions, the overall pore size of the dialysis bags is not changing significantly. Therefore, the membrane
379 fouling that causes changing the pore size is negligible.

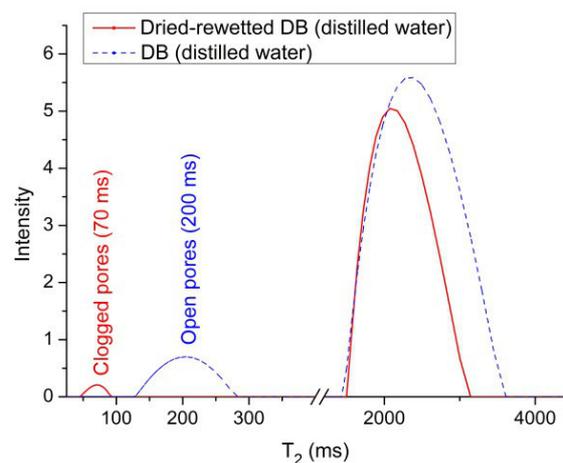


380

381 **Figure 5:** NMR relaxation spectra (T_2) of the ¹H spins of the bulk samples of distilled water, river water, and n-
382 TiO₂ in river (dash line), and the water-filled pores of dialysis bags (DB) incubated in the corresponding water
383 media for one week (solid line). Each sample was measured in triplicates and the T_2 distributions are averaged
384 over the corresponding replicates.

385

386 In order to verify that pore clogging can actually be detected using NMR relaxometry, measurements were
387 performed with membrane dried under ambient conditions. Since drying of dialysis membrane is known to
388 induce an irreversible collapse of the pores,²⁸ we expected the pore size to be drastically reduced after drying.
389 Since the presence of water molecules in the pores is required for characterizing the pore size using NMR
390 relaxometry, the dried membrane was rewetted for 24 hours prior to T_2 measurement. The first peak of the T_2
391 distribution corresponding to small pores of dried dialysis membranes after rewetting (**Figure 6-clogged pores**)
392 was significantly smaller (t-test, 95%) compared to non-dried membranes (**Figure 6-open pores**). Considering a
393 T_2 value for small pores around 70 ms as an extreme case for collapsed of the membrane structure, it can be
394 concluded that all dialysis membrane samples in water media (**Figure 4-solid line**) with T_2 values of 200-300 ms
395 did not experience extended fouling, which would have led to a significant reduction of pore size.



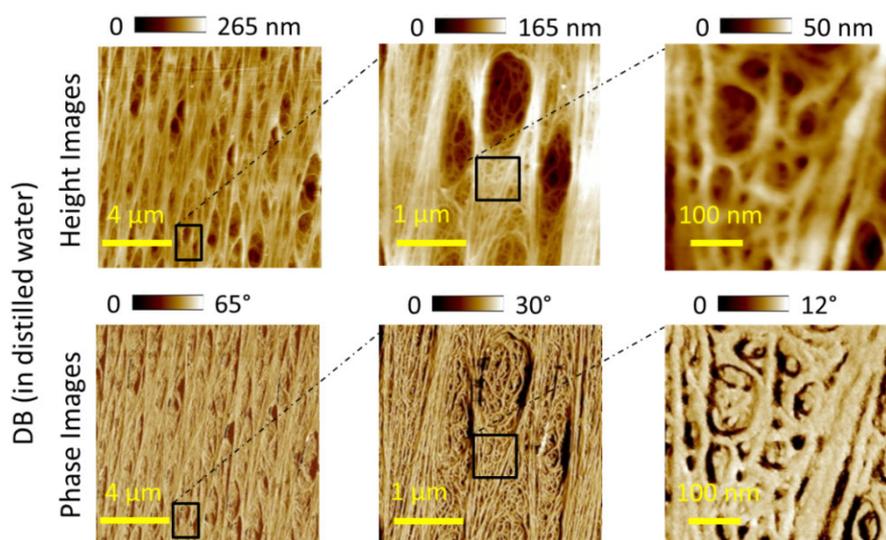
396

397 **Figure 6:** T_2 distribution comparison of dried-rewetted dialysis bags (clogged pores) and wet dialysis bag (open
398 pores) in distilled water.

399

400 *Pore size distribution measured by AFM*

401 **Figure 7** shows the AFM height and phase images of a dialysis membrane measured in distilled water. All the
402 measurements were carried out in the fluid mode for avoiding drying of the sample. Furthermore, this mode
403 enables using the same media as during the permeability experiments (river water with and without n-TiO₂), thus
404 providing a more realistic assessment of the membrane pore size.



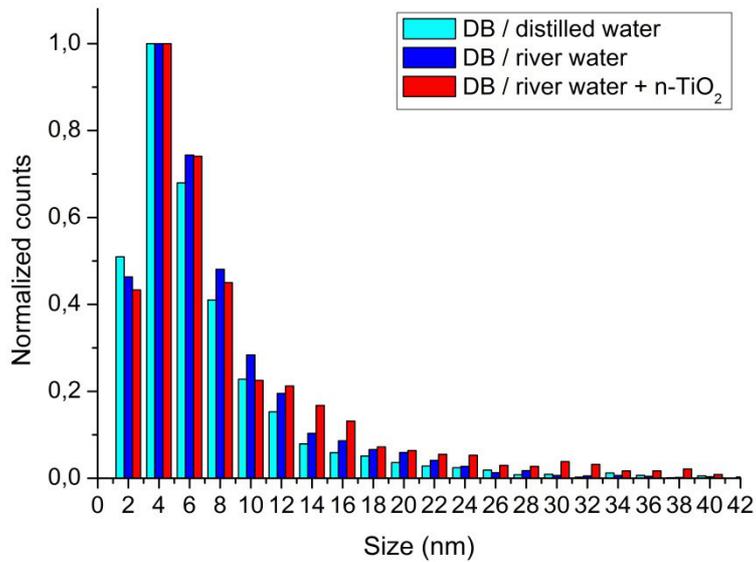
405

406 **Figure 7:** AFM height (top) and phase (bottom) images of the dialysis bag (DB) in distilled water measured in
 407 fluid mode.

408

409 The images exhibit the hierarchical porous structure of the dialysis bag. Three different areas are distinguishable
 410 in the images ranging from the nanometer to the micrometer scale: 1) a microporous structure with a
 411 polydisperse size distribution, 2) at higher magnification, a nanoporous network covering the whole sample
 412 including inside the micropores, and 3) a lamellar substructure. AFM images of dialysis bags in the river water
 413 (with and without n-TiO₂) depict an overall lower resolution compared to the samples measured in distilled water
 414 (**Figures S4-S5**) probably due to ionic screening charges in river water (Bruker.com).

415 The pore size distribution of dialysis bags in different media (**Figure 8**) shows a hydrodynamic diameter mode
 416 of 4 nm for all the samples. Besides, the observed differences between the pore sizes of the dialysis bags in
 417 different water media were not significant; in agreement with the results of NMR relaxometry. The
 418 determination of the average pore diameter of a three-dimensional porous structure based on two-dimensional
 419 images can only be an approximation based on several assumptions. Therefore, the absolute values of the pore
 420 size reported here should be taken as a first estimation and used for comparison purposes only.



421

422 **Figure 8:** Pore size distribution of dialysis bags (DB) in different water media determined using AFM in fluid
 423 mode (Six AFM regions of interest were used for each sample).

424

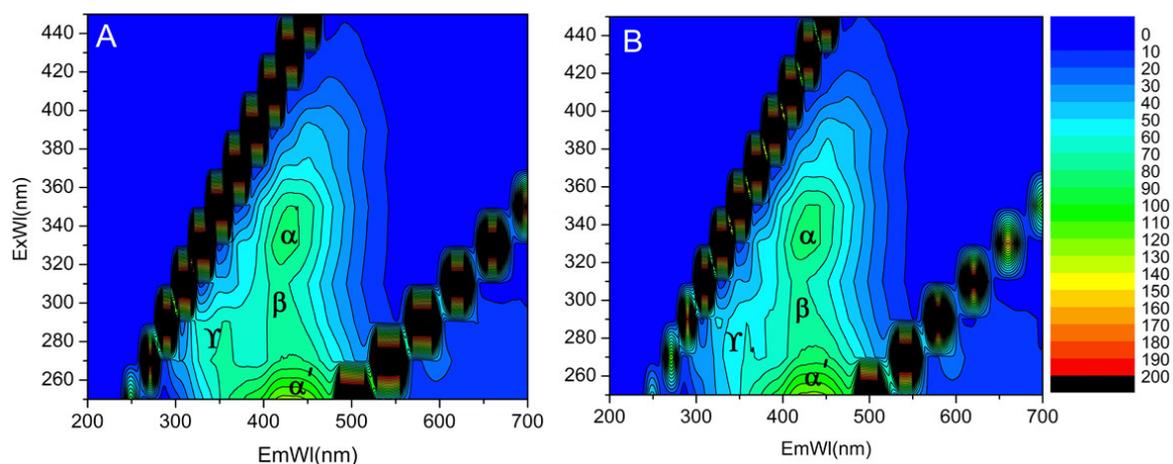
425 *Field experiment*

426 Based on the previous method development, cylindrical cellulose ester dialysis bags with MWCO of 100 kDa
 427 were chosen to carry out a proof of concept of investigating the interaction of n-TiO₂ with natural DOM under
 428 natural conditions. After one week of exposure in the river, the samples (inside the dialysis bag) were collected
 429 in polypropylene centrifuge tubes and transported immediately to the nearby located laboratory. The n-TiO₂ were
 430 then separated using centrifugation for characterizing the sorption of NOM onto n-TiO₂. In general, the
 431 composition and quantity of DOM in natural waters vary over time⁵⁹ and investigations on the sorption require
 432 monitoring these variations over the deployment period. However, the concentrations inside and outside the
 433 dialysis bag equilibrate in less than a few hours and the water composition was fairly stable over the time of this
 434 study (**table S1**). Hence, we assume that the compositions of water sampled outside and inside the dialysis bag
 435 are similar. To provide a reference for NOM (outside the dialysis bag), the river water was also collected in
 436 polypropylene centrifuge tubes on the last day of exposure.

437

438 *Permeability of the membrane under field experiment: Fluorescence EEMs*

439 **Figure 9** shows the Fluorescence EEMs of the river water (A), and the river water diffused into the dialysis bag
 440 (B). In both samples, the EEM plots show four spectral features of the natural waters relate to α , α' , β , and γ
 441 corresponding respectively to carboxylic, phenolic, alkaloids, and protein groups (see discussion above).



442

443 **Figure 9:** Fluorescence EEMs of the samples carried out in the field A) river water B) river water inside the
 444 dialysis bag (the color scale depicts the intensity a.u).

445

446 As it can be seen, α , α' , and β peaks of the river water are similar in inside and outside of the DB. It can suggest
 447 that the composition of DOM of the river water inside the DB is similar to the natural water to a good extent.

448 **Figure 6S** depicts the Fluorescence EEM of the supernatant of the river water inside DB in presence of n-TiO₂.

449 All the mentioned peaks in the river water (α , α' , β , and γ) are present with reduced intensities in this sample.

450 An indirect effect of the sorption of DOM onto n-TiO₂ could explain these differences. However, one should
 451 notice that the quantitative interpretation of fluorescence results for such complex mixtures is far from trivial and
 452 should be considered as a first approach in the frame of this proof of concept. Hence, the Fluorescence EEMs
 453 results can be investigated qualitatively not quantitatively. However, the results show the DOM permeates the
 454 membrane under field condition and the made observations are similar to the ones made in the lab. The
 455 biological activities induced by the membrane decomposition seem not to impair sensibly the permeability of the
 456 membrane and may, therefore, be of little importance under field conditions.

457 Since the results of fluorescence spectroscopy are just expressing the fluorophore groups in the river water, and
 458 the activity of lipids or polysaccharides, for instance, cannot be monitored, the water media were further
 459 investigated with FT-ICR-MS.

460

461 *Permeability of the membrane under field experiment: FT-ICR-MS*

462 Ultrahigh resolution Fourier-transform ion cyclotron resonance mass spectrometry (FT-ICR-MS) was used to
 463 gain detailed insight in the molecular composition of river water DOM inside and outside the dialysis bag.

464 3766 (58%) out of 6468 formulas were shared between all three river samples (outside the dialysis bag, and
 465 inside the dialysis bag with and without n-TiO₂), while 1181 (18%) and 1539 (24%) formulas occurred only in

466 one and two samples, respectively (**Figure S7**). As expected for terrestrial derived DOM, there was a large
467 dominance of CHO (53%) compounds over CHNO (35%) and CHOS (10%) (**Table S4**).

468 Some compounds were depleted ($\Delta RI < 0.43$) in the water outside vs inside the bag ($n = 554$) but show a
469 homogenous distribution in the van Krevelen (vK) space as expected for analytical noise (**Figure 10**). However,
470 based on intensity differences between river water inside the dialysis bags and river water outside the bag, there
471 emerges a clear pattern for compounds enriched inside the bag ($\Delta RI > 0.57$, $n = 591$). They represent compounds
472 which are highly aliphatic ($H/C = 1.622 \pm 0.178$), and cover a broad range of oxygenation ($O/C = 0.403 \pm$
473 0.108).

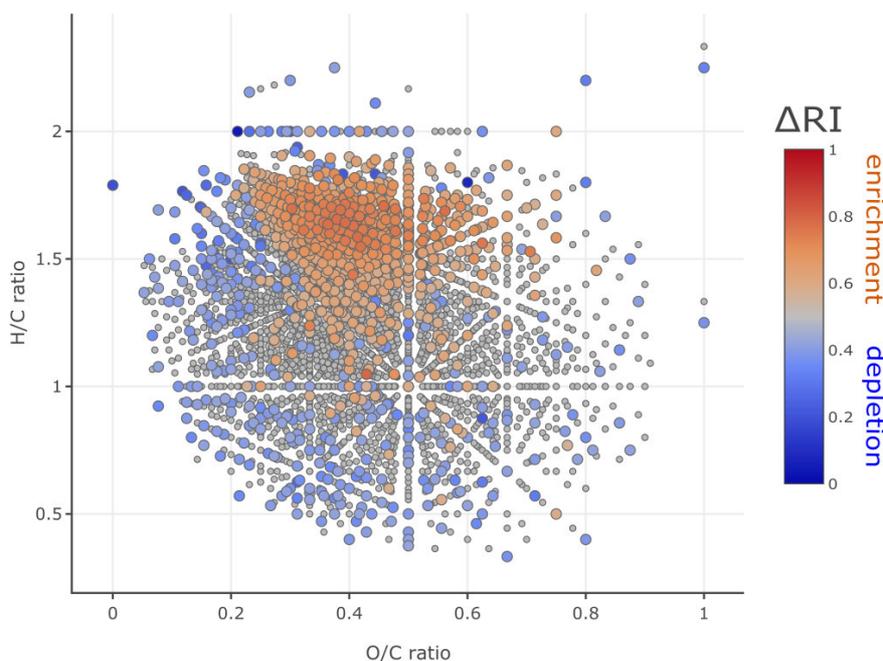
474 Cellulose acetate is biodegradable in presence of esterases which is produced by different classes of
475 microorganisms.⁶⁰ Upon biodegradation, cellulose acetate bears deacetylation and breaking down cellulose
476 backbone⁶¹ into smaller chains or glucose monomers, which are potential sources of energy for further microbial
477 activities. Hence, the observed pattern of enriched compounds inside the dialysis bag (compared to the river
478 water) may point to microbial induced degradation of the membrane. This is in agreement with the results of
479 DOC and dissolved O_2 (**Figure 3**) showing respiration within and DOC leaching from the bag in one week under
480 laboratory conditions.

481 Interestingly, compounds with similar chemical properties ($H/C = 1.539 \pm 0.368$, $O/C = 0.401 \pm 0.148$) were
482 depleted when n-TiO₂ was added to the bags compared to the bags without n-TiO₂ (**Figure S8**) i.e. the
483 enrichment observed in the river water inside the dialysis bag is not observed with n-TiO₂ present. While the
484 enriched compounds inside the bag are mostly CHO (73%), the depleted compounds with n-TiO₂ contain a
485 larger fraction of CHNO formulas (47%). In the field experiment, under the assumption of thermodynamic
486 equilibrium, any preferential sorption of DOM on the n-TiO₂ can be compensated by river water from outside the
487 dialysis bag. This assumption is acceptable considering the relatively short equilibration time measured in the
488 laboratory experiments (less than 3 h, **Figure 3**) and the stability of the river water chemical parameters over
489 months (**Table S1**). Therefore, the observed differences in DOM composition are probably not related only to
490 sorption, but to the effect of n-TiO₂ on biodegradation of the membrane. Indeed, Lazic et al. reported the
491 negative influence of n-TiO₂ on biodegradation of cellulose.⁶²

492 In order to explore this hypothesis, we determined the measured DOC and dissolved oxygen (DO) of the river
493 water inside the dialysis bag with and without n-TiO₂ over a week under laboratory conditions (**Figure S9**). In
494 both cases, DOC was increasing over a week; however, less increase was observed in presence of n-TiO₂. Since
495 the control samples of the river water with and without n-TiO₂ showed a similar DOC, sorption cannot be the
496 determinant factor of the decreased DOC production inside the bag in presence of nanoparticles. Furthermore,

497 DOC increasing occurred parallel to DO decreasing (**Figure S9**) with less reduction observed inside the dialysis
498 bag in presence of n-TiO₂ while the control samples of the river water with and without n-TiO₂ showed almost
499 the same DO. Therefore, we conclude that n-TiO₂ reduces the biodegradation of cellulose ester under laboratory
500 and field conditions.

501



502

503

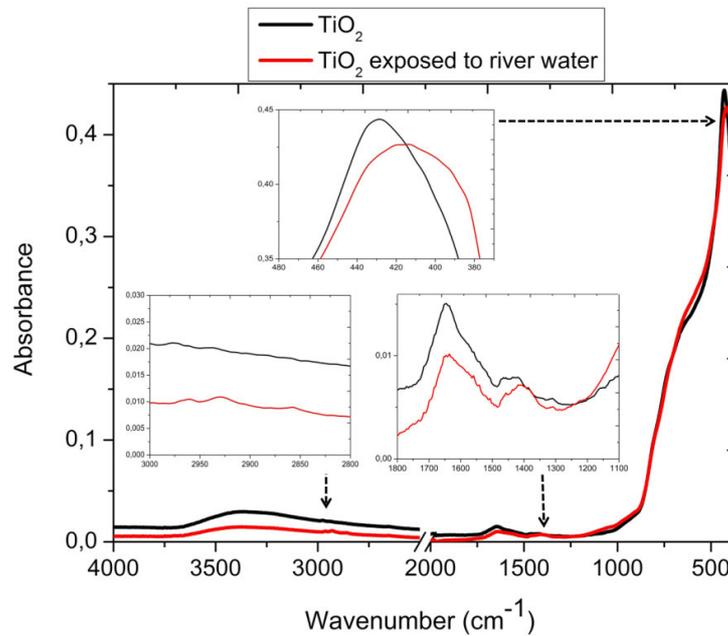
504 **Figure 10:** Van Krevelen diagram with intensity differences for river water inside the dialysis bags vs river
505 water. Δ RI values above 0.57 (red) were considered to indicate that the respective compound is enriched inside
506 the dialysis bags, and Δ RI values below 0.43 (blue) indicates the respective compound is depleted inside the
507 dialysis bag.

508

509 *Sorption of DOM onto n-TiO₂: ATR-FTIR*

510 The ATR-FTIR spectra of n-TiO₂, and n-TiO₂ exposed to the river water are shown in **Figure 11**. There are two
511 bands in both samples, the peak around 1640 cm⁻¹ is attributed to the bending vibration of the O-H bond of
512 chemisorbed water and the broad peak around 3350 cm⁻¹ corresponds to the surface adsorbed water and hydroxyl
513 groups. A prominent band occurring at 430cm⁻¹ due to Ti-O, and Ti-O-Ti stretching vibration modes is shifted to
514 lower frequency after exposing to river water; ⁶³ probably due to the interaction of Ti-O with the DOM of the
515 river water. The major functional groups in aquatic humic substances are carboxylic acid, hydroxyl, phenolic,
516 and carbonyl groups (1100-1700 cm⁻¹), ²⁶ which were seen in the river water sample (**Figure S10**). After

517 exposing n-TiO₂ to the river water, the band at 1400 cm⁻¹ (**Figure 11**) can be attributed to carboxylic acid groups
518 of the river water sorbed onto nanoparticles. The C-H stretching vibrations (CH₂) between 2950-2850 clearly
519 indicate organic matter on the river exposed sample. In addition, the agglomeration of the nanoparticles in the
520 river media could cause the observed band broadening.⁶⁴



521

522 **Figure 11:** ATR-FTIR spectra of n-TiO₂, and n-TiO₂ exposed to river water in field experiment.

523

524 Sorption of DOM onto n-TiO₂: CHNS

525 Elemental analysis in **Table 3** depicts that the carbon, nitrogen, hydrogen, and sulfur content of river water
526 (freeze-dried), n-TiO₂, and n-TiO₂ exposed to river water. The CHNS-contents in n-TiO₂ exposed to River water
527 were higher than in pristine n-TiO₂ probably indicating the sorption of DOM onto n-TiO₂. **Figure 12** depicts the
528 Euclidean distances allows comparing the elemental composition of the three treatments where “A” is assigned
529 to n-TiO₂, “B” to river water, and “C” to n-TiO₂ exposed to river water (A-B: 0.495 ± 0.25, A-C: 0.528 ± 0.24,
530 B-C: 0.0965 ± 0.18). Since the point corresponding to n-TiO₂ exposed to river water is closer to the river water
531 than to the pristine n-TiO₂ (**Figure 12**: B-C < A-C), we conclude that the organic matter adsorbed onto the
532 nanoparticles under field condition does not experience strong fractionation. This results in an NOM-coating
533 chemically close to river water DOM. Furthermore, comparing the absolute absorbance values of the elements
534 depicted that although there is a high difference between the amount of river water in two samples of “B” and
535 “C” (250 ml of freeze-died river water in “B” compared to few μL of residual river water on n-TiO₂ in “C”), the
536 absorbance is comparable. Hence, contribution of the residual river water to the CHNS-signal of the
537 nanoparticles in river water is negligible. Combining the hints provided by EEM fluorescence, ATR-FTIR, and

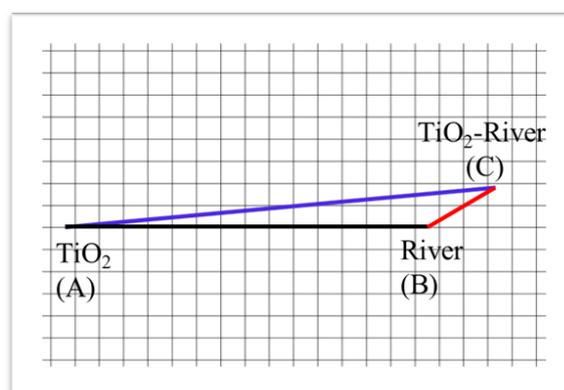
538 CHNS analyses, we can conclude that the sorption of DOM occurred under field condition and that the proposed
 539 concept is valid.

540 **Table 3** Elemental content (CHNS) in river water, n-TiO₂, and n-TiO₂ exposed to River water

Element content (wt %)	n-TiO ₂	n-TiO ₂ exposed to River water	River water
C	0.012	1.23	6.15
H	0.057	0.18	1.53
N	0.107	0.26	1.29
S	0.13	0.74	4.84

541

542



543

544 **Figure 12:** Euclidean distances calculated from the normalized C-, H-, N-, and S-contents (four dimensional
 545 space) of River water, n-TiO₂, and n-TiO₂ exposed to River water where A-B: 0.495±0.25, A-C: 0.528 ± 0.24, B-
 546 C: 0.0965±0.18.

547

548 *Conclusion*

549 In this work, we introduced dialysis membrane as a passive reactor to produce nanoparticles with natural
 550 coating. Such particles could be useful to study the fate and toxicity of nanoparticles under natural conditions.
 551 Since nanoparticles from 20 nm are successfully retained in the reactor and most of the DOM can permeate
 552 through the membrane and reach the nanoparticle surface, we conclude that the concept is valid. Furthermore,
 553 the sorption of DOM onto n-TiO₂ was evaluated by ATR-FTIR and CHNS elemental analysis of the
 554 nanoparticles before and after exposure to the river water which both depicted the occurrence of sorption under
 555 applied conditions. Further validation will include testing the performance of the reactor under various
 556 conditions and in differing surface waters. For exposure times longer than two days, the microbial activity due to
 557 the degradation of the membrane may interfere with the sorption processes. Optimizing the membrane properties

558 and sample preparation in order to minimize this effect can help in this respect. Finally, for future studies, more
559 advanced analytical methods are required to characterize NOM-engineered nanoparticles corona.

560 *Acknowledgments*

561 This research was funded by the German Research Foundation, research unit INTERNANO (FOR1536
562 “Mobility, aging and functioning of engineered inorganic nanoparticles at the aquatic–terrestrial interface”,
563 subprojects SCHA849/16). The authors would like to thank Wolfgang Fey, Karin Meyer, and Doris Burgard for
564 ICP-OES, DOC, and CHNS measurements, respectively. The authors also acknowledge Jan Kaesler for FT-ICR
565 MS measurements and are grateful for using the analytical facilities of the Centre for Chemical Microscopy
566 (ProVIS) at the Helmholtz Centre for Environmental Research, Leipzig which is supported by the European
567 Regional Development Funds (EFRE - Europe funds Saxony) and the Helmholtz Association.

568

569 *References*

- 570 1 N. C. Birben, C. S. Uyguner-Demirel, S. S. Kavurmaci, Y. Y. Gürkan, N. Turkten, Z. Cinar
571 and M. Bekbolet, Application of Fe-doped TiO₂ specimens for the solar photocatalytic
572 degradation of humic acid, *Catalysis Today*, 2017, **281**, 78–84.
- 574 2 F. Loosli, P. Le Coustumer and S. Stoll, Effect of electrolyte valency, alginate
575 concentration and pH on engineered TiO₂ nanoparticle stability in aqueous solution,
576 *Science of the Total Environment*, 2015, **535**, 28–34.
- 578 3 V. Adam, S. Loyaux-Lawniczak and G. Quaranta, Characterization of engineered TiO₂
579 nanomaterials in a life cycle and risk assessments perspective, *Environmental Science and*
580 *Pollution Research*, 2015, **22**, 11175–11192.
- 582 4 Y. S. Sahu, Nano Titanium Dioxide Market by Application (Paints & Coatings, Pigments,
583 Cosmetics, Plastics, Energy and others) - Global Opportunity Analysis and Industry
584 Forecast, 2014 - 2022, *Allied Market Research*, 2016, 119.
- 586 5 A. Philippe, J. Košík, A. Welle, J.-M. Guigner, O. Clemens and G. E. Schaumann,
587 Extraction and characterization methods for titanium dioxide nanoparticles from
588 commercialized sunscreens, *Environmental Science: Nano*, 2018, **5**, 191–202.
- 590 6 A. P. Gondikas, F. von der Kammer, R. B. Reed, S. Wagner, J. F. Ranville and T.
591 Hofmann, Release of TiO₂ nanoparticles from sunscreens into surface waters: a one-year
592 survey at the old Danube recreational Lake, *Environmental science & technology*, 2014,
593 **48**, 5415–5422.
- 595 7 M. Bundschuh, J. Filser, S. Lüderwald, M. S. McKee, G. Metreveli, G. E. Schaumann, R.
596 Schulz and S. Wagner, Nanoparticles in the environment: where do we come from, where
597 do we go to?, *Environmental Sciences Europe*, 2018, **30**, 6.
- 599 8 G. E. Schaumann, A. Philippe, M. Bundschuh, G. Metreveli, S. Klitzke, D. Rakcheev, A.
600 Grün, S. K. Kumahor, M. Kühn, T. Baumann and others, Understanding the fate and

- 601 biological effects of Ag-and TiO₂-nanoparticles in the environment: the quest for advanced
602 analytics and interdisciplinary concepts, *Science of the Total Environment*, 2015, **535**, 3–
603 19.
- 605 9 A. Philippe and G. E. Schaumann, Interactions of dissolved organic matter with natural and
606 engineered inorganic colloids: a review, *Environmental science & technology*, 2014, **48**,
607 8946–8962.
- 609 10 C. Zhang, J. Lohwacharin and S. Takizawa, Properties of residual titanium dioxide
610 nanoparticles after extended periods of mixing and settling in synthetic and natural waters,
611 *Scientific Reports*, 2017, **7**, 9943.
- 613 11 S. Valencia, J. M. Marín, G. Restrepo and F. H. Frimmel, Evaluation of natural organic
614 matter changes from Lake Hohloh by three-dimensional excitation-emission matrix
615 fluorescence spectroscopy during TiO₂/UV process, *Water research*, 2014, **51**, 124–133.
- 617 12 N. Sani-Kast, J. Labille, P. Ollivier, D. Slomberg, K. Hungerbühler and M. Scheringer, A
618 network perspective reveals decreasing material diversity in studies on nanoparticle
619 interactions with dissolved organic matter, *Proceedings of the National Academy of
620 Sciences*, 2017, 201608106.
- 622 13 C. Nickel, B. Hellack, A. Nogowski, F. Babick, M. Stintz, H. Maes, A. Schäffer and T.
623 Kuhlbusch, Mobility, fate and behavior of TiO₂ nanomaterials in different environmental
624 media, *Environmental Research of the Federal Ministry for the Environment*.
- 626 14 M. Luo, Y. Huang, M. Zhu, Y. Tang, T. Ren, J. Ren, H. Wang and F. Li, Properties of
627 different natural organic matter influence the adsorption and aggregation behavior of TiO₂
628 nanoparticles, *Journal of Saudi Chemical Society*.
- 630 15 M. Drosos, M. Ren and F. H. Frimmel, The effect of NOM to TiO₂: interactions and
631 photocatalytic behavior, *Applied Catalysis B: Environmental*, 2015, **165**, 328–334.
- 633 16 W. Chen, C. Qian, X.-Y. Liu and H.-Q. Yu, Two-dimensional correlation spectroscopic
634 analysis on the interaction between humic acids and TiO₂ nanoparticles, *Environmental
635 science & technology*, 2014, **48**, 11119–11126.
- 637 17 S. Shakiba, A. Hakimian, L. R. Barco and S. M. Louie, Dynamic Intermolecular
638 Interactions Control Adsorption from Mixtures of Natural Organic Matter and Protein onto
639 Titanium Dioxide Nanoparticles, *Environmental science & technology*, 2018, **52**, 14158–
640 14168.
- 642 18 J. Namieśnik, B. Zabiegała, A. Kot-Wasik, M. Partyka and A. Wasik, Passive sampling
643 and/or extraction techniques in environmental analysis: a review., *Anal Bioanal Chem*,
644 2005, **381**, 279–301.
- 646 19 A. Kot, B. Zabiegała and J. Namiesnik, Passive sampling for long-term monitoring of
647 organic pollutants in water, *TrAC Trends in Analytical Chemistry*, 2000, **19**, 446–459.
- 649 20 T. Górecki and J. Namieśnik, Passive sampling, *TrAC Trends in Analytical Chemistry*,
650 2002, **21**, 276–291.

- 652 21 D. A. Vroblesky, J. Manish, J. Morrell and J. Peterson, Evaluation of passive diffusion bag
653 samplers, dialysis samplers, and nylon-screen samplers in selected wells at Andersen Air
654 Force Base, Guam, March-April 2002, *US Geological Survey Water-Resources*
655 *Investigations Report*, 2003, 03–4157.
- 657 22 B. E. Vencalek, S. N. Laughton, E. Spielman-Sun, S. M. Rodrigues, J. M. Unrine, G. V.
658 Lowry and K. B. Gregory, In situ measurement of CuO and Cu (OH) 2 nanoparticle
659 dissolution rates in quiescent freshwater mesocosms, *Environmental Science &*
660 *Technology Letters*, 2016, **3**, 375–380.
- 662 23 P. Benes and E. Steinnes, In situ dialysis for the determination of the state of trace elements
663 in natural waters, *Water Research*, 1974, **8**, 947–953.
- 665 24 P. Wang, Aggregation of TiO₂ Nanoparticles in Aqueous Media: Effects of pH, Ferric Ion
666 and Humic Acid, *Int. J. Environ. Sci. Nat. Res*, 2017, **1**, 555575.
- 668 25 W. Wu, G. Shan, Q. Xiang, Y. Zhang, S. Yi and L. Zhu, Effects of humic acids with
669 different polarities on the photocatalytic activity of nano-TiO₂ at environment relevant
670 concentration, *Water research*, 2017, **122**, 78–85.
- 672 26 K. J. Howe, K. P. Ishida and M. M. Clark, Use of ATR/FTIR spectrometry to study fouling
673 of microfiltration membranes by natural waters, *Desalination*, 2002, **147**, 251–255.
- 675 27 S. Jeon, S. Rajabzadeh, R. Okamura, T. Ishigami, S. Hasegawa, N. Kato and H.
676 Matsuyama, The effect of membrane material and surface pore size on the fouling
677 properties of submerged membranes, *Water*, 2016, **8**, 602.
- 679 28 <https://www.repligen.com/dialysis-tubing-membranes>.
- 681 29 M. Meyer, C. Buchmann and G. Schaumann, Determination of quantitative pore-size
682 distribution of soils with ¹H NMR relaxometry, *European journal of soil science*, 2018, **69**,
683 393–406.
- 685 30 C. Zhang, P. Li, Y. Zhang, F. Lu, W. Li, H. Kang, J. Xiang, Y. Huang and R. Liu,
686 Hierarchical porous structures in cellulose: NMR relaxometry approach, *Polymer*, 2016,
687 **98**, 237–243.
- 689 31 J. V. Bayer, F. Jaeger and G. E. Schaumann, Proton nuclear magnetic resonance (NMR)
690 relaxometry in soil science applications, *The Open Magnetic Resonance Journal*, 2010, **3**,
691 15–26.
- 693 32 [http://www.nanophys.kth.se/nanophys/facilities/nfl/afm/fast-scan/bruker-](http://www.nanophys.kth.se/nanophys/facilities/nfl/afm/fast-scan/bruker-help/Content/Probe%20and%20Sample%20Guide/Samples/FS%20Fluid%20Sample%20Mounting.htm)
694 [help/Content/Probe%20and%20Sample%20Guide/Samples/FS%20Fluid%20Sample](http://www.nanophys.kth.se/nanophys/facilities/nfl/afm/fast-scan/bruker-help/Content/Probe%20and%20Sample%20Guide/Samples/FS%20Fluid%20Sample%20Mounting.htm)
695 [%20Mounting.htm](http://www.nanophys.kth.se/nanophys/facilities/nfl/afm/fast-scan/bruker-help/Content/Probe%20and%20Sample%20Guide/Samples/FS%20Fluid%20Sample%20Mounting.htm).
- 697 33 [http://www.nanophys.kth.se/nanophys/facilities/nfl/afm/fast-scan/bruker](http://www.nanophys.kth.se/nanophys/facilities/nfl/afm/fast-scan/bruker-help/Content/Fluid%20Imaging/FS%20Fluid%20Operation_Droplet.htm)
698 [help/Content/Fluid%20Imaging/FS%20Fluid%20Operation_Droplet.htm](http://www.nanophys.kth.se/nanophys/facilities/nfl/afm/fast-scan/bruker-help/Content/Fluid%20Imaging/FS%20Fluid%20Operation_Droplet.htm).
- 700 34 R. J. Peters, G. van Bommel, N. B. Milani, G. C. den Hertog, A. K. Undas, M. van der Lee
701 and H. Bouwmeester, Detection of nanoparticles in Dutch surface waters, *Science of the*
702 *Total Environment*, 2018, **621**, 210–218.

- 704 35 J. Raeke, O. J. Lechtenfeld, M. Wagner, P. Herzsprung and T. Reemtsma, Selectivity of
705 solid phase extraction of freshwater dissolved organic matter and its effect on ultrahigh
706 resolution mass spectra, *Environmental Science: Processes & Impacts*, 2016, **18**, 918–927.
- 708 36 O. J. Lechtenfeld, G. Kattner, R. Flerus, S. L. McCallister, P. Schmitt-Kopplin and B. P.
709 Koch, Molecular transformation and degradation of refractory dissolved organic matter in
710 the Atlantic and Southern Ocean, *Geochimica et Cosmochimica Acta*, 2014, **126**, 321–337.
- 712 37 B. Koch, G. Kattner, M. Witt and U. Passow, Molecular insights into the microbial
713 formation of marine dissolved organic matter: recalcitrant or labile?, *Biogeosciences*, 2014,
714 **11**, 4173–4190.
- 716 38 P. Herzsprung, N. Hertkorn, W. von Tümpling, M. Harir, K. Friese and P. Schmitt-
717 Kopplin, Understanding molecular formula assignment of Fourier transform ion cyclotron
718 resonance mass spectrometry data of natural organic matter from a chemical point of view,
719 *Analytical and bioanalytical chemistry*, 2014, **406**, 7977–7987.
- 721 39 P. Herzsprung, N. Hertkorn, W. von Tümpling, M. Harir, K. Friese and P. Schmitt-
722 Kopplin, Molecular formula assignment for dissolved organic matter (DOM) using high-
723 field FT-ICR-MS: chemical perspective and validation of sulphur-rich organic components
724 (CHOS) in pit lake samples, *Analytical and bioanalytical chemistry*, 2016, **408**, 2461–
725 2469.
- 727 40 T. Kind and O. Fiehn, Seven Golden Rules for heuristic filtering of molecular formulas
728 obtained by accurate mass spectrometry, *BMC bioinformatics*, 2007, **8**, 105.
- 730 41 J. Raeke, O. J. Lechtenfeld, J. Tittel, M. R. Oosterwoud, K. Bornmann and T. Reemtsma,
731 Linking the mobilization of dissolved organic matter in catchments and its removal in
732 drinking water treatment to its molecular characteristics, *Water research*, 2017, **113**, 149–
733 159.
- 735 42 M. Kosmulski, Isoelectric points and points of zero charge of metal (hydr) oxides: 50 years
736 after Parks' review, *Advances in colloid and interface science*, 2016, **238**, 1–61.
- 738 43 B. Matthews, A. Jones, N. Theodorou and A. Tudhope, Excitation-emission-matrix
739 fluorescence spectroscopy applied to humic acid bands in coral reefs, *Marine Chemistry*,
740 1996, **55**, 317–332.
- 742 44 P. Boguta and Z. Sokołowska, Interactions of Zn (II) ions with humic acids isolated from
743 various type of soils. Effect of pH, Zn concentrations and humic acids chemical properties,
744 *PLoS One*, 2016, **11**, e0153626.
- 746 45 M. Sierra, M. Giovanela, E. Parlanti and E. Soriano-Sierra, Fluorescence fingerprint of
747 fulvic and humic acids from varied origins as viewed by single-scan and
748 excitation/emission matrix techniques, *Chemosphere*, 2005, **58**, 715–733.
- 750 46 E. Khan and S. Subramania-Pillai, Effect of leaching from filters on laboratory analyses of
751 collective organic constituents, *Proceedings of the Water Environment Federation*, 2006,
752 **2006**, 901–918.
- 754 47 A. F. de Faria, A. C. M. de Moraes, P. F. Andrade, D. S. da Silva, M. do Carmo Gonçalves
755 and O. L. Alves, Cellulose acetate membrane embedded with graphene oxide-silver

- 756 nanocomposites and its ability to suppress microbial proliferation, *Cellulose*, 2017, **24**,
757 781–796.
- 759 48 <http://www.epa.gov/glindicators/water/oxygenb.html>, Dissolved Oxygen Depletion in Lake
760 Erie. In Great Lakes Monitoring.
- 762 49 K. Krishnamurti and S. Kate, Changes in electrical conductivity during bacterial growth,
763 *Nature*, 1951, **168**, 170.
- 765 50 K. Andarany, A. Sagir, A. Ahmad, S. Deni and W. Gunawan, in *IOP Conference Series:*
766 *Materials Science and Engineering*, 2017, vol. 237, p. 012042.
- 768 51 B. M. Tebo, J. R. Bargar, B. G. Clement, G. J. Dick, K. J. Murray, D. Parker, R. Verity and
769 S. M. Webb, Biogenic manganese oxides: properties and mechanisms of formation, *Annu.*
770 *Rev. Earth Planet. Sci.*, 2004, **32**, 287–328.
- 772 52 T. Rennert, Wet-chemical extractions to characterise pedogenic Al and Fe species—a critical
773 review, *Soil Research*, 2019, **57**, 1–16.
- 775 53 M. Tiso and A. N. Schechter, Nitrate reduction to nitrite, nitric oxide and ammonia by gut
776 bacteria under physiological conditions, *PloS one*, 2015, **10**, e0119712.
- 778 54 E. Fridjonsson, S. Vogt, J. S. Vrouwenvelder and M. Johns, Early non-destructive
779 biofouling detection in spiral wound RO membranes using a mobile earth's field NMR,
780 *Journal of Membrane Science*, 2015, **489**, 227–236.
- 782 55 Y. Qing, R. Sabo, Y. Wu, J. Zhu and Z. Cai, Self-assembled optically transparent cellulose
783 nanofibril films: effect of nanofibril morphology and drying procedure, *Cellulose*, 2015,
784 **22**, 1091–1102.
- 786 56 M. Hayama, K. Yamamoto, F. Kohori and K. Sakai, How polysulfone dialysis membranes
787 containing polyvinylpyrrolidone achieve excellent biocompatibility?, *Journal of membrane*
788 *science*, 2004, **234**, 41–49.
- 790 57 L. A. Neves, P. J. Sebastiao, I. M. Coelho and J. G. Crespo, Proton NMR relaxometry
791 study of nafion membranes modified with ionic liquid cations, *The Journal of Physical*
792 *Chemistry B*, 2011, **115**, 8713–8723.
- 794 58 S. Polarz, B. Smarsly and J. H. Schattka, Hierarchical porous carbon structures from
795 cellulose acetate fibers, *Chemistry of materials*, 2002, **14**, 2940–2945.
- 797 59 H. Van de Weerd, W. Van Riemsdijk and A. Leijnse, Modeling the dynamic
798 adsorption/desorption of a NOM mixture: Effects of physical and chemical heterogeneity,
799 *Environmental science & technology*, 1999, **33**, 1675–1681.
- 801 60 K. Sayali, P. Sadichha and S. Surekha, Microbial esterases: an overview, *International*
802 *Journal of Current Microbiology and Applied Sciences*, 2013, **2**, 135–146.
- 804 61 J. Puls, S. A. Wilson and D. Höltter, Degradation of Cellulose Acetate-Based Materials: A
805 Review, *Journal of Polymers and the Environment*, 2011, **19**, 152–165.

807 62 V. Lazic, M. Radoicic, Z. Saponjic, T. Radetic, V. Vodnik, S. Nikolic, S. Dimitrijevic and
808 M. Radetic, Negative influence of Ag and TiO₂ nanoparticles on biodegradation of cotton
809 fabrics, *Cellulose*, 2015, **22**, 1365–1378.

811 63 L. Saravanan, R. M. Kumar, A. Pandurangan and R. Jayavel, Synthesis and photophysical
812 studies of PVP capped Titania Nanostrips for photocatalytic applications, *Optoelectronics
813 and advanced materials-rapid communications*, 2010, **4**, 1676–1680.

815 64 K. S. Babu, A. R. Reddy, C. Sujatha, K. V. Reddy and A. Mallika, Synthesis and optical
816 characterization of porous ZnO, *Journal of Advanced Ceramics*, 2013, **2**, 260–265.

818